

Environmental Engineering
Databases
Wastewater, Chemical, Pharmaceutical, Electronics, Battery, and Oil
Industries
Case Studies and Solution to Wastewater Case Study
Professor Zikri Ahmed
Gateway Project
July, 1997

**GATEWAY EEC PROJECT No. CID - U - 05 - CU
FINAL REPORT**

August 15, 1997

**Project Title; " Shared Resources " Classroom Case Studies and Database Applications
In Environmental Engineering Education**

**Cooper Union Personnel; Dr. Zikri Ahmed , Faculty
Department of Chemical Engineering**

Project Description;

Scope;

Environment, as a specific curriculum ,must be an integral part of the engineering education process. Environmentally safe products require the application of environmentally sound design and the use of less hazard alternatives.

EPA provides guidelines for waste reduction. It does not provide pollution prevention technology. The environmental awareness and designer skills are the cornerstone for pollution prevention technology. Engineering students should learn the skills inorder to become environmentally conscious and to avoid costly training after graduation.

The lack of reliable, quantifiable information on environmental fate and health data is an impediment to effective class analysis and strategic design policy. Compilation of such information assists in locating potential trouble spots and provide ideas on how to reduce environmental risks and develop safe design.

One of the areas that is of most concern to our daily life and represents an interesting module is municipal wastewater. A prototype database system has been constructed from the information contained in the annual survey of municipal wastewater in The New York - New Jersey area. The database module developed spans hundreds of pollutants and can project wastewater emmissions in urban and suburban regions. It is therefore a useful guide to safe design. Database modules together with case studies that cover other areas such as;chemical, pharmaceutical,electronic , electrochemical and oil industries have also been developed.

Objectives;

The objectives of this project is to establish an information sharing database system that can be used by students and teachers to estimate comprehensive profiles of domestic and industrial pollution for regions and urban areas and to provide them with a reliable picture and better understanding of the concept of environmental engineering in more details. It can also provide them with the basic training required to enhance their abilities to implement alternative technology. It is also expected that these developed modules will serve as educational tools for integrating environmental factors into other courses.

Methodology and Goals ;

The database in the attached disk has been collected from different municipalities inorder to have complete coverage which allows sectoral comparison.It covers several areas of interest such as, municipal wastewater, battery and electronic industries, chemical and pharmaceutical industries and oil refineries.These database modules can answer

such questions as;

what types of waste are produced and processed by such industries?

what types of chemicals are used by these industries?

what are the typical influent and effluent stream concentrations?

what are the effluent standard concentrations established by EPA?

what are the threshold concentration limits that an average worker endures for these chemicals?

what are the toxic effects and safety considerations?

The broad databases developed here have been used to construct mini-type classroom projects which represent true case studies and have been used by different engineering majors. Some of these projects have been incorporated into ChE 340 (a junior-senior chemical engineering course that deals with industrial waste control and can be taken by all majors) and CE 441 (a civil engineering course that deals with pollution and water management open to civil and chemical engineering senior and graduate students).

The databases developed together with these case studies are available on the Internet .This creates an electronic environmental mini-library available to all institutions. This mini-library can be used for class applications and research. For example, in the case of municipal wastewater module, students and teachers can summon the data to check the variation of the effluent streams due to seasonal and abnormal changes, compare the different municipalities involved or use the data directly to design a treatment facility.

A detailed solution of one of these case studies (design of a new water treatment plant for a growing community) is presented and discussed .The detailed solution can be used as a guiding model to enhance student ability and approach to solution of engineering problems. This case can be used as a term project .Parts of this case study can also be assigned as mini projects or homework problems.

Assessment and Evaluations

These databases have been used and betasted at Cooper Union and The University of South Carolina. All points raised by evaluators in their assessment have been adressed. A copy of the assessment is attached .

Conclusion

Environmental regulations are currently implementd at great cost to society and industry. This is because the infrastructure needed for implementing these regulations has not been sufficiently developed. Industry can no longer react to these challenges with "end-of-pipe" solutions. The need to design for environment is a must. Integrating environmental considerations into existing design practices reflects a forward thinking approach to achieve a safe and sucessful design. Academia can play an important role in developing future generations of engineers who are trained in methodology of design for environment. Developing of such information and modules and making it available for engineering students is a step on the road to achieving this goal.

* <http://www.cooper.edu/~ahmed/intro.html>

or

 <http://www.cooper.edu/engineering/chemechem/Welcome.html> (faculty research projects)



June 30, 1996

CIVIL AND ENVIRONMENTAL ENGINEERING

Professor Zikri Ahmed
The Cooper Union
Albert Nerken School of Engineering
Cooper Square
New York, New York 10003-7183

Re: *Submission of the Gateway Beta Test*

Zikri
Dear Dr. Ahmed:

Enclosed is the Beta Test evaluation of the wastewater treatment module (D21) developed at the Cooper Union as part of the Gateway Environmental Engineering Project. A summary of the beta test results is provided on page 5 of the report.

If you require any future information, please call me at (803) 777-7403 or send me e-mail at mcanally@engr.engr.sc.edu. Thank you.

Sincerely,

A. Steve McAnally, Ph.D., P.E.
Associate Professor

Enclosures

GATEWAY PROJECT
Beta Test of Polytechnic University Modules D17 -D19
and The Cooper Union Module D21

Introduction

In January 1997 the co-PI received the course modules from Polytechnic University and the Cooper Union. Polytechnic University's modules included D17: Small Municipal Wastewater Treatment Plant Design, D18: Municipal + Industrial Wastewater Treatment, and D19: Large Wastewater Treatment Plant Design each of which is based on the use of *SuperPro Designer*[®] v. 1.0. The Cooper Union module included D21: Data Base Information for Municipal Wastewater, Chemical and Pharmaceutical Industries Wastewater, and Electronic Industries Wastewater. These case studies were introduced to the students of a junior/senior level water and wastewater treatment course (ECIV 551- *Elements of Water and Wastewater Treatment*) as a final project for the Spring 1997 semester. Evaluations were performed by the instructor (Co-PI) and the students of ECIV 551. Additionally, some feedback on The Cooper Union module was obtained from a couple of graduate students in ECIV 752 (Water and Wastewater Treatment II). This is a graduate level course dealing with the principles of biological process design.

Implementation

The overall evaluation process of the case study modules developed at Polytechnic University and The Cooper Union required a four-step procedure. The first step involved the introduction of the students to the use of the *SuperPro Designer*[®] v. 2.0 software by implementing several of the USC developed instructional modules. The USC modules provided preliminary training for the ECIV 551 students in utilizing the software to analyze various unit operations and treatment trains. This introductory step prepared the students for working the more comprehensive case study modules developed by Polytechnic University and The Cooper Union. ECIV 551 has both science and design components. The objectives of the course include the development of the students' understanding of the engineering principles governing the design of physical, chemical, and biological water/wastewater treatment unit operations, and the integration of the students understanding into municipal treatment systems design. An outline of this course is as follows:

1. Introduction
2. Water and wastewater treatment systems
 - Water quality standards
 - Regulations
3. Chemical principles and reactor kinetics
4. Physical treatment unit operations applied to water and wastewater treatment plant design
5. Chemical treatment processes applied to water treatment plant design

6. Introduction to wastewater treatment and wastewater characteristics
7. Secondary wastewater treatment processes
 - Suspended growth systems
 - Attached growth systems
 - Ponds and lagoons
8. Advanced wastewater treatment processes
9. Sludge treatment and disposal

By mid-semester (March 15, 1997) the students had been introduced to two of the USC instructional modules, D24: Clarifier/Thickener Instructional Module and D26: Aerobic Treatment Instructional Module. The third USC instructional module D27: Sludge Treatment Instructional Module was introduced later in the semester after the Polytechnic University and The Cooper Union case study modules were presented to the students. The USC modules are provided in Appendix 1.

The second step involved the development of a problem statement for the presentation of the Polytechnic University and The Cooper Union case study modules to the students. Because the ECIV 551 class had only six students, it was divided into three teams of two students each. Therefore, only three modules could be utilized as design problems, two from Polytechnic University and one from The Cooper Union. (Another module from The Cooper Union was introduced as a final project for a graduate student in the ECIV 752 course).

Each of the modules required preparation time by the instructor before they could be integrated into the course. Although the Polytechnic University case study modules provided example simulation reports that included the input and output data, the instructor needed to develop a more detailed scenario so the ECIV 551 students would be able to complete the final projects within the second half of the semester. The problem statements developed and presented by the USC instructor for Polytechnic University's Modules D18: Municipal + Industrial Wastewater Treatment and D19: Large Wastewater Treatment Plant Design are presented as Design Project #1 and Design Project #2, respectively, in Appendix 2. The Cooper Union provided data bases for typical influent and effluent parameter values representing several municipal and industrial facilities found in the New York/New Jersey area. The USC instructor developed a problem scenario for one of the data bases to be introduced to a student team. This problem statement is also provided in Appendix 2 as Design Project #3.

The third step involved the implementation of the Polytechnic University and The Cooper Union case study modules into the course. As an introduction to the various aspects of a design project, the instructor modified and presented an overview of the Polytechnic University module D17: Small Municipal Wastewater Treatment Plant Design. The modification required updating the module to *SuperPro Designer*[®] v. 2.0. The summary of the overview is presented in Appendix 3. The overview included the development of a problem scenario, and some specific information for the more difficult aspects of the simulations. Additionally, technical information on engineering economics (Peters and Timmerhaus, 1968) was provided to help explain the engineering economics report of the module. The overview was formally provided over 1.5 class

periods (approximately 2 hours of class time). Also, informal tutoring was available with a graduate teaching assistant throughout the semester.

The fourth step involved the formal evaluation of the Polytechnic and The Cooper Union case study modules.

Module Evaluation

The development of evaluation procedures for the case study modules was performed by the co-PI in conjunction with a local Gateway evaluator. The evaluation has two basic components: an instructor review and student evaluation. The instructor review involved a technical review of module documentation as well as an evaluation of the effectiveness and practicality of implementing the module. The students evaluated the quality and usefulness of the case study module application and the instructor's approach in implementing the modules.

Instructor Evaluation. The instructor evaluated the practicality and effectiveness of the case study modules by answering the following questions as he implemented each into the classroom instruction. A summary of the responses is provided following each question.

(1) *What is the degree of compatibility of the instructional module with the course objectives?* The theme of each module (Polytechnic University D17 to D19, and The Cooper Union D21) was very compatible with the objectives of the ECIV 551 course of instruction.

(2) *What degree of effort was required to evaluate the module during the initial "screening" review?* The degree of effort required for the initial screening review has been summarized by the amount of time required to read the instructions and perform the example problem simulations. The instructor (who is familiar with the computer software) screened the first module within a 4 - 6 hour period. This included reviewing the module background information and running the simulations with *SuperPro Designer*[®] v. 2.0. (Additional time was required to transfer the modules to from v. 1.0 to v. 2.0). However, instructors not familiar with the computer software will require a significantly greater period of time to perform the initial screening review.

The Cooper Union module (D21) was a slightly different situation. This module presented a data base and didn't provide a formal case study problem to be implemented. Because of this approach, the instructor spent additional time developing an appropriate case study problem for the class. The effort is described in more detail in Question #4.

(3) *How does the case study module format compare to the SuperPro Designer*[®] *User's Guide format for utility in this course?* The summary format of the Polytechnic University modules D17 to D19 provided a more clear and concise approach for using the computer program to produce wastewater treatment plant designs. 

This question does not apply to *The Cooper Union* module (D21).

(4) *What degree of effort was required to implement each case study module in the classroom instruction?* The *Polytechnic University* modules D17 to D19 are very useful in providing specific input/output data required for a particular problem scenario. However, the instructor must still generate the problem scenario to apply to the specific input/output data. It would be more useful to have an example problem scenario included with at least one of the modules so the instructor can quickly assess the module utility and easily implement it in the course.

The Cooper Union module (D21) contains thorough useful data sets for application to the ECIV 551 course. A couple of data sets (Pharmaceutical and Oil Refinery) would be more readily adaptable for design problems with a typical and range of example flowrates, or a typical and range of mass loading rates. Even so, the instructor must still generate the problem scenario to apply to the specific input/output data. It would be more useful to have an example problem scenario included with the module so the instructor can quickly assess the module utility and easily implement it in the course.

Student Evaluation. The ECIV 551 students completed two surveys at the end of the 1997 Spring Semester. A 9 item survey asked the students to evaluate the case study modules for use in classroom instruction. The second survey included 20 questions requesting the students to evaluate the instructor and the course. A summary of the student evaluations is provided in Appendix 4. (Note: the local Gateway evaluator is reviewing and summarizing the student evaluations of the instructor and course. These are not available at the time of this writing).

There were six students in the ECIV 551 class, all of which were civil engineering majors. Self-reports on the survey indicated that the students GPAs ranged from # to # with an average of 3.1 for the class. All of the students were familiar with AutoCad v. 12 and 13 software and with KYPipes software. Fifty percent of the students were familiar with WaterCad.

Students responded to seven evaluative questions about the case study modules. A summary of the responses to each of these questions is provided in Appendix 4. Overall, the students were very positive concerning the usefulness of the case study modules for this particular course of instruction. The students felt that the strongest advantage of the modules was that they were helpful in aiding the student visualize the practical design aspects of the course. Most of the students (67%) felt that the case study modules added to the quality of the course instruction and should be used as part of the course in the future.

The students did not strongly feel that the instructional modules were helpful in learning the fundamental concepts of the course. However, the majority (approximately 67%) of the students did indicate that the modules reinforced their learning of the fundamental concepts to a varying degree.



Summary of the Beta Test Results

The overall conclusions from the evaluations by the instructor and the students are that the case study modules (Polytechnic University D17 to D19 and The Cooper Union D21) definitely enhanced the presentation of the course material, and the modules should be used in future courses. The modules can be strengthened for a science/design type course, such as ECIV 551, by providing a more detailed example problem scenario for the instructor. Such an inclusion will allow a potential user (the instructor) to readily assess the utility of the module for his/her course, and easily implement the module with minimal preparation time.

**Design Project#3 Municipal Wastewater with metals and nutrients
(Copper Union Module D21)**

An influent from several industrial plants and towns located in the New York city are treated at a single waste treatment plant. The yearly average flow into the waste treatment plant is 270 mgd. The municipal waste contains sewage, metals, and nutrients with the following average influent characteristics:

SS (suspended solids) = 83 mg/l

Glucose = 83 mg/l (Biodegradable organics can be represented as glucose to simplify the problem)

Silver = 0.003 mg/l

Zinc = 0.056 mg/l

Copper = 0.044 mg/l

Mercury = 0.0002 mg/l

Nickel = 0.0043 mg/l

Lead = 0.0087 mg/l

Ammonia = 9.5 mg/l

Design a waste treatment plant to handle the influent flow that meets the NPDES standards set by the regulatory authorities for the discharge of the effluent into the Savannah River located in Augusta, Ga. Also, evaluate the design under average, peak, and low loading conditions.

The finish product should consist of a summary report (5 to 7 pages) to communicate the results of the study. The summary report should have the general format:

INTRODUCTION
BACKGROUND
DESIGN ANALYSIS
CONCLUSIONS
RECOMMENDATIONS
REFERENCES

Each design problem statement should included the following format:

1. List of assumptions and justifications
2. Sizes and number of unit operations and specifications of the oxygen delivery facilities
3. Print out of flow diagram of design
4. A stream report, economic report, and environmental report under average conditions included in an appendix
- 5 Other information you deem important and necessary.

NOTE : Any questions should be directed to Brian Bush(Bush@engr.sc.edu)

- Office Hours MWF 11:00 a.m.-12:15 a.m.
TH 3:00 p.m.-5:00 p.m.

**STUDENT EVALUATION
of
Case Study Module**

1. Instructor: _____ Date: _____ Major: _____ GPA: _____
2. List the number of the case study evaluated?
3. How did the case study help or hinder the learning process? (What were the advantages and disadvantages of using the case study)?
4. To what extent did the case study module help you learn the fundamental concepts in the course?
5. To what extent did the case study module help you visualize the practical design aspects of the course?
6. If you could get the software developer to change any aspect of the program, what would you suggest and why?
7. Did you consult with the user's manual at any time during the course? If yes, how helpful was the manual? If no, why not?

8. Would you recommend the usage of the case study module as part of future course instruction? Why?

9. If you could make any changes to the case study module, what would you suggest and why?

DEPARTMENT OF CIVIL AND ENVIRONMENTAL ENGINEERING
STUDENTS EVALUATION OF INSTRUCTION

Course _____ Instructor _____ Term Spring Year 1997

The instructor clearly stated the instructional objectives of the course.

- (1) inadequately (2) poorly (3) adequately (4) well (5) very well
-

The instructor clearly stated the method by which your final grade would be determined.

- (1) inadequately (2) poorly (3) adequately (4) well (5) very well
-

The instructor clearly explained any special requirements of attendance which differ from the attendance policy of the University.

- (1) no special requirements stated (2) no (3) yes
-

The instructor graded and returned the student's written work (e.g., examinations and papers) in a timely manner.

- (1) inadequately (2) poorly (3) adequately (4) well (5) very well
-

The instructor met the class regularly and at the scheduled times.

- (1) inadequately (2) poorly (3) adequately (4) well (5) very well
-

The instructor scheduled a reasonable number of office hours per week.

- (1) no hours scheduled (2) no (3) yes
-

Please indicate your satisfaction with the availability of the instructor outside the classroom by choosing one response from the scale below. (In selecting your rating, consider the instructor's availability via established office hours, appointments, and other opportunities for face-to-face interaction as well as via telephone, e-mail, fax, and other means)

- (1) very dissatisfied (2) dissatisfied (3) satisfied (4) very satisfied
-

During the semester, how often did you seek assistance or attempt to seek assistance from the instructor outside of class?

- (1) never (2) less than once a month (3) about once a month (4) several times a month (5) weekly
-

What is your classification?

- (1) freshman (2) sophomore (3) junior (4) senior (5) graduate
-

What is your cumulative G.P.A. ?

- (1) first semester (2) 2.00-2.49 (3) 2.50-2.99 (4) 3.00-3.49 (5) 3.50-4.00
-

What grade do you anticipate in the course ?

- (1) F (2) D or D+ (3) C or C+ (4) B or B+ (5) A
-

Why are you taking this course ?

- (1) elective in my major (2) elective outside my major (3) degree requirement
-

How beneficial were the textbook and other aids utilized in the course?

(1) inadequate (2) barely adequate (3) fair (4) good (5) excellent

6. To what extent does the instructor exhibit command of the subject matter?

(1) inadequate (2) barely adequate (3) fair (4) good (5) excellent

5. How beneficial were the instructor's responses to student questions?

(1) inadequate (2) barely adequate (3) fair (4) good (5) excellent

4. Based on the instructor's presentation; he/she was prepared for the class:

(1) not applicable (2) rarely (3) sometimes (4) usually (5) almost always

7. To what extent did the examinations reflect the course objectives and the material emphasized in class?

(1) very poorly (2) poorly (3) fair (4) good (5) excellent

3. In your opinion is the instructor concerned about the students as individuals?

(1) no opinion (2) unconcerned (3) concerned

2. The overall effectiveness of the Instructor in this course is:

(1) terrible (2) poor (3) fair (4) good (5) excellent

1. The overall quality of the course is:

(1) terrible (2) poor (3) fair (4) good (5) excellent

In the space below write your comments which will help the instructor improve his/her effectiveness as a teacher. Include any strengths or weaknesses which are not adequately revealed by the questionnaire. In addition, your reasons for any particularly high or low ratings will be useful.

**Case Study
Student Evaluation from 551**

Question #1: List the number of students involved in each case study?

Number of students: 6 undergraduates students Ave. GPA: 3.1

Question #2: List the number of the case study evaluated?

- Case study #1 was given as an example
- Case study # 2 and 3 were given as problems
- Copper Union database

Question #3: How did the case study help or hinder the learning process? (What were the advantages and of using the case study)?

Advantages:

- Helped with application of class material
- It explained a lot of little details of a waste treatment plant design and operation.

Question #4: To what extent did the case study module help you learn the fundamental concepts in the course.

- Above average
- Good
- Not very good

Question #5: To what extent did the case study module help you visualize the practical design aspects of course.

- Excellent
- Pretty good

Question #6: If you could get the software developer to change any aspect of the program, what would you suggest and why?

- Provide more real examples of their software
- Increase the number of unit operation allow in one simulation
- Make the software more user friendly
- The problem is to sensitive because it kicks you out for entering the wrong numbers.
- Increase the number of unit operations that can be combined in one simulation.
- Add more options for operations that can be combined in one simulation
- Check divide by zero error because it terminates the program if the user neglects to input a flow.
- Check influent component percentage because if you change your flowrates or even enter the stream and don't change anything, the programs says the mass percentages don't add up to 100 percent. However, the mass percentages add up to 100 percent.
- Make the [OK] button the default selection on the simulation data sheet for unit operation and not the

reaction button.

- Have a dialog box pop up when doing the iterations which allows the user to pause calculation and check the status of lines or cancel calculation.

Question #7: Did you consult with the user's manual at anytime during the course? If yes, how helpful was the manual? If no, why not?

Yes Responses:

- It was moderately helpful
- It was pretty good

No Responses:

- Because of it's simplicity

Question #8: Would you recommend the usage of the case study modules as part of the future course instruction? Why?

Yes Responses:

- It helps the student practice and apply concepts.
- Yes, but need to expand the complexity

No Responses:

- Need to expand it's completeness.
- Superpro Version 2 has too many bugs

Question #9: If you could make any changes to the case study module, what would you suggest and why?

- Expand the scope of the case study

•

Graduate Student Evaluation
Brian M. Bush

Question #3: How did the case study help or hinder the learning process? (What were the advantages and of using the case study)?

Advantages:

- It tied the course material with real application work.
- Gave examples of results of unit operation under different conditions.
- It demonstrated different types of design for waste treatment plants.
Case #2 - showed an illustration of industrial treatment.
Case #3 - Showed a full scale plant design of waste treatment plant.
- Showed how engineering knowledge is applied using computer software.
- Displayed the big picture of a waste treatment plant.
- Show impacts on environmental properties under different loading conditions.

Disadvantages:

- Superpro Ver. 2.0 software is not easy to use and master
- Students depended to much on the software to answer the case study problem
- Not detailed enough to be presented in the 551 class because the class is not a design class
A) Lacked background information to explain the difference in the case study modules

Question #4: To what extent did the instructional module help you learn the fundamental concepts in this course?

- Tie the individual unit operation into a big picture
- Extended the learning process because of the quickness of the program

Question #5: To what extent did the case study module help you visualize the practical design aspects of the course?

- It provided a technical view on how different unit operations are tied together.

Question #6: If you could get the software developer to change any aspect of the program, what would you suggest and why?

- A) Make the program less sensitive to input data such that the inputs do not cause the program to terminate it's operation.
· For example, if no input flows are not entered, it would terminate the program
- B) Put a undo button in the program
- C) Add a liquid exiting stream from the anaerobic digester
· Such a designer could recycle the stream
- D) Increase the number of unit operations on the simulation

- Could not add nitrification and denitification such that I could perform different load values such that one could use one simulation.
- E) Address in the manual that some of the database components are incomplete which will effect the environmental properties in the simulation.
- In the database provided by in the program, the ammonia environmental properties have all zero values
- F) Make the air flotation unit calculate the area of the length, width, and amount of air used in the unit operation.
- G) Add a simulation run window so that you could cancel the simulation run or show any important errors
- H) Add an error check routine to display any missing information on the flowsheet
- I) Make the program recognize that streams beside the influent is a input stream because this makes the mass balance off by the amount entered in the streams that are entering the simulation. For example, the amount of water entered in the belt press for washing is not counted as a input and the mass balance is off by a number plus the input stream of the belt filter press.

Question #7: Did you consult with the user's manual at anytime during the course? If yes, how helpful was the manual? If no, why not?

- No, because the manual does not show or define how to effectively run a simulation.

Question #8: Would you recommend the usage of the case study module as part of future course instruction? Why?

- Yes because the module was beneficial to class understanding of the class material

Question #9: If you could make any changes to the case study module, what would you suggest and why?

Polytech

- A) Need more input as why the input was provided
 - Why the Case Study #2 lacked a sludge handling process
 - Why case study 2 used the influent as income in the economics section
 - What the overall goals of each case study
 - Why the polymer was removed out of case study 2 and 3.
- B) Address reactions provided with the case studies
 - Why all the case studies coupled the synthesis and oxidation equation
- C) Give more detail on a background of the case study
 - What region are the case study modules basis

- D) Give more information on how to present the case study
- E) Give more information on why certain values were entered in the economic section
 - Why each stream was used as income
- F) Give a focus on the case study such a sample NPDES permit.
 - What was case study number 2 overall goal for treating the industrial waste
 - What was the requirements for case study 3 since it used polymers to increase the efficiency of the secondary clarifier.

Cooper Union

- A) Provide more operating data so a good representation of average, peak, and minimum flows can be determined
- B) Provide some limits from the NPDES permit.
 - Since the flows were so large, the NPDES requirements would give a regional treatment requirements
- C) Give more detail on a background of the case study
- D) Provide a sample design of one of the databases

Municipal Wastewater Treatment Facilities

Case 1.

The population increase in the state of Easy Living has brought about growing demands for the establishment of new cities in the state. The cities would be constructed on land owned by the state. The state would sell the land to the developers. However, it is the responsibility of the state to supply these new communities with water, energy, schools, and recreation areas. The state is also responsible for building municipal wastewater treatment facilities for these new cities. A typical city would have the potential for approximately 100,000 to 200,000 residents over the next 30 years. These new cities will also attract industries such as food processing, metal and light chemicals. Typical wastewater influent streams would resemble those of an urban city. Design a suitable wastewater treatment facility for one of these cities.

This project requires a teamwork solution.

Case 2.

Design a wastewater treatment facility that can handle 20 MGD. Sources of wastewater are commercial, household and pretreated industrial waste. The following table gives stream influent characteristics:

Component	Concentration (mg/l)
BOD	18
Suspended Solids	180
Biomass	26
Debris	70
Copper	0.3
Lead	0.1
Organic Compounds	3.0
Oil and Grease	1.0
Water	999,600

The treatment process should involve among others; screening, sedimentation, clarification, thickening, digestions, and filtration. You can use your own unit operations and unit processes scheme or any

wastewater treatment software such as SuperPro Designer. The effluent stream is discharged into a nearby river.

Case 3.

The population increase in the state of Easy Living has brought about growing demands for a new supply of potable water, especially in the area of Freedom City (a residential community). It is anticipated that the city will have a population potential for approximately 50,000 new residents over the next 50 years. 1,000 visitors per day are also expected when the new shopping mall is completed within the next two years. The existing treatment facilities are limited and allow no future expansion. The purpose of any treatment plant is to provide water that is chemically and bacteriologically safe for human consumption and domestic use. A surface water reservoir is located 8 miles north of Freedom City and is assumed to contain enough water supply at all times. Preliminary studies by the Pussy Cat water company indicate that the average use of water per capita is 300 gallons per day. This includes residential interior, business, schools, recreation and fire fighting use. It also indicates a peaking factor equal to 2. The company also studied the quality of the reservoir water. Analysis of a typical sample of the surface reservoir water gave the following information:

1. amount of dissolved oxygen = 5 mg/L
2. turbidity = 8 NTU
3. suspended solids = 30 mg/L
4. BOD₅ = 8 mg/L
5. dissolved inorganic salts (mostly calcium) = 300 mg/L
6. 2000 fecal coliform per 100 mL
7. some debris and fish
8. no radioactive contaminants

The city has designated a space located 4 miles south of the reservoir as a site for the construction of a new water treatment plant. It has an elevation 400 ft lower than the reservoir. This elevation is also 200 ft higher than the ground surface of the city.

Design a suitable water treatment plant that solves the water shortage problem and meets the EPA standards. The following design criteria apply:

1. Minimum detention time in a sedimentation tank is 4 hours
2. Maximum overflow rate in a sedimentation tank is $30 \text{ m}^3/\text{m}^2$ a day.
3. Efficiency for sedimentation tank no less than 85%
4. Filtrate rate in a treatment filter is $3 \text{ L}/\text{m}^2$ per second
5. Pumping station efficiency is no less than 80%
6. Flocculation average detention time no less than 30 minutes



Justify and design parameters used and give references for any assumed values.

Pharmaceutical Wastewater Treatment Systems

Case 1.

Curepharma is engaged in the production of soft gelatin capsules (vitamins and dietary supplements). These products consist of gelatin shells and medicine or vitamin fill materials. In order to produce softgels, the gelatin and medicines or vitamins must be processed.

The gelatin is melted down to a liquid, then cast into a sticky ribbon like form of specific dimensions. This ribbon is then lubricated with oil so it can be drawn through the mechanical components of the encapsulation machine without sticking to the machine parts. The fill material must be liquid and must have an edible oil base since a water base liquid would destroy the gelatin ribbon. Rotary dies cut capsule shapes from the ribbons while a pump simultaneously fills the capsule shell as it is being formed. This process consumes 20,000 pounds of processed gelatin per day and 3,000 gallons of food grade oil per day.

Because the products are manufactured for human consumption, the cleanliness of equipment is very important. To remove the oils and vitamin and medicine powders from tanks, trays, pumps, and other manufacturing equipment, manual and automatic washing processes utilize strong detergents which emulsify the oils and powders.

The wastewater resulting from the procedures discussed above is rich in oils and high in pH and heavy with sediments in the form of mineral and vitamin powders. While all the oils and soaps used are non-toxic and FDA approved, the company's wastewater permit requires an effluent which meets the EPA levels of oil and grease and acceptable pH values. Design a treatment system which can handle a 10,000 gallon per day of wastewater produced by Curepharma.

Case 2.

A wastewater system of a vitamin gel capsule manufacturing company collects wastewater from the following areas:

- 1 - Formulation
The pot wash sink

- 2 - Wash Room
 - a- Capsule Tray washing machine
 - b- Formulation Tank washing pit
 - c- Formulation Tank Wash Room sink
- 3 - Maintenance Shop
 - a- Parts washing sink
 - b- Pump washing pit
- 4 - Porter station
 - a- Mop Washing pit

The company uses food oils and non-toxic petroleum products to facilitate the encapsulation process. The wastewater resulting from the manufacturing process is high in oils and grease (5,000 - 15,000 ppm) and heavy sediments (mineral and vitamin powders). Its pH ranges from 9 to 12 and its BOD is between 2,000 and 5,000 mg/lit.

Design a treatment facility capable of producing an effluent that meets EPA standards and regulations. The company generates approximately 20,000 gallons wastewater per day.

Case 3.

The growth of the pharmaceutical industry has been steady over the past years. Their products are classified according to the SIC system as a) medicinal, chemical, and botanical products, b) pharmaceutical preparations, c) in vitro and invivo diagnostic substances, and d) biological products, except diagnostic substances (US EPA). The pharmaceutical industry utilizes batch type reactions to manufacture its products. Cleanliness is an important factor since the products are eventually consumed by humans. Typical pharmaceutical products include vitamin supplements, aspirin, saline solution, and shampoos.

Depending upon the specific product, the raw materials, processes employed, generated wastes for the industry vary. The industry can be divided into the following sections:

1. research and development
2. chemical synthesis
3. natural product extraction
4. fermentation
5. formulation

The fifth segment will be analyzed, specifically a soft gel capsule production.

Soft Gel Capsule Production



The formulation process involves the production of gels, capsules, creams and ointments. In the production of soft gels, the capsules are prepared by melting gelatin into rotary die plates. To avoid sticking to the rotary plates and other mechanical components, oil is used to lubricate the equipment. A capsule is formed when the rotary plates are brought together combining the two halves of the capsule shell. Afterwards, the fill material, a non-aqueous solution, is injected into the empty shell capsules, thus producing a soft gelatin capsule. The finished product can be a vitamin supplement or an over the counter medicine.

Process Waste Description

The wastes generated by the soft gel capsules production results from the cleaning and sterilization of equipment, chemical spills, rejected products, and lubricants. The equipments must be thoroughly cleaned since the capsules are for human consumption. The oil and medicine powder residues from the machines are mechanically and hand cleaned. Strong detergents are utilized to emulsify the oils and powders. A typical waste stream composition includes oil, grease, and hydrocarbons. Therefore, the industrial pretreatment facility for soft gel capsule production must handle oils and sediments. In addition, the water is basic with a pH range os 9-12.

For a plant with the following Influent Stream Characteristics;

Component	Flow Rate, kg/hr	Concentration, gm/lit
Oil and Grease	150	93.8
Petroleum Hydrocarbons	340	212.5
TSS	10	6.3
Water	1100	687.5

Design a treatment facility that will produce and effluent within the range of POTW's regulations. The treated effluent is ultimately discharged into sewers.

Electronics and Electrochemical Industrial Waste Treatment Facilities

Case 1.

The Printed Circuit Board: Electroplating

Since its development, printed circuit board has virtually replaced hand wiring as a means of connecting electronic circuitry in military and commercial applications. A printed circuit board consists of a circuit pattern placed on a nonconductive base. These patterns are made with conductive metals such as nickel, copper and aluminum. Depending on its use, the design and complexity of the printed circuit board varies.

The wastes generated in the production of printed circuit (PC) boards range from solid wastes such as failed PC boards to hazardous wastes such as nitric acids. The principal sources of wastes are; cleaning and surface preparation operations, catalyst application and electrolyze plating operations, pattern printing and masking operations, electroplating and etching operations

The materials used for each operation dictate the characteristics of the wastewater resulting from such operation. It includes spent solvents, airborne particles, acids and metals.

In a typical electroplating process, the influent waste stream consists of the following:

Component	Flow Rate (kg/hr)
copper	14.5
nickel	12.2
lead	10.4
cyanide	6.2
water	500

Design a treatment facility capable of treating 4000 gallons per day of liquid waste. The effluent stream is to be discharged into a public sewer system. Common unit operations used in such treatment facilities might include among others; ion exchange, granular media filtration and neutralization.

Case 2.

Pollution Prevention or Reduction at the Source; Computer Impact Printers:

Printbands are parts of many component parts used in the manufacturing of impact printers. Printbands are stainless steel belts chemically machined via a photolithographic process in which stainless steel panels are treated with etching solution of ferric chloride and hydrochloric acid (IBM).



The dissolved steel spent etchant (ferrous chloride) solution contains also chromium and traces of

molybdenum. The treatment of the waste etch solution involves neutralization of the hydrochloric acid and precipitation of metals. The presence of chromium deposits in the sludge makes it hazardous and results in an expensive disposal cost.

Expansion of the computer industry in the last 15 years requires large investment in on-site sludge handling and off-site disposal treatment. To handle the voluminous waste etch solution alternative technologies which 1) ensure continuous supply of ferric chloride, 2) encourage conservation practices, and 3) reduce waste and minimize treatment costs are needed.

Suggest, discuss and design at least two alternative strategies that will address this problem.

Case 3.

Treatment Plant from and Electrochemical Industry

Wastewater treatment system design requires two phases, (1) the identification of the chemical compounds in the waste, the sources of these compounds in the industrial process, the toxic effects of these chemicals, the concentration levels of these chemicals and the technologies capable of reducing the concentrations of these contaminants to an acceptable non-toxic levels, (2) the selecting, combining and arranging of the unit treatment operations and processes that will achieve the treatment objectives.

The design or simulation of a chemical plant or a wastewater treatment facility becomes more realistic with the use of actual site data. Whether it involves utilizing the quantitative aspects of the influent or effluent stream concentrations or basically just obtaining a listing of the chemicals used, the student has a better chance of practically solving or simulating the facility. In turn, the sizes of the unit operations and costs of the plant will not be ridiculously meaningless.

The wastes generated by an electrochemical industry have to be treated first before discharging it into the sewers. The main source of pollution comes from two general chemical categories: 1) heavy metals and 2) organics. The typical influent wastes' characteristics include chromium, copper, benzene, and toluene. The concentration values for these and other chemicals can be obtained from the electrochemical folder in the enviro.wb2 database. The effluent stream from this database readily meets the stringent EPA guidelines. Design a feasible, cost-effective treatment facility that can reduce the influent stream characteristics to the desired effluent stream values. Note that the flow rates are not given. Look for the typical flow rates used in this industry and state any assumptions made.

Battery Industries

Case 1.

The waste generated by battery industries contains chemicals that are not only toxic but also resistant to degradation. Thus, they represent serious health, safety and environmental problems. Manufacturing processes involve casting, chemical reactions, pasting and curing, container and tank formation of batteries, quality control work,... Waste that could result from such processes include among others; acids, alkalies, heavy metals, oil and greases, metallic dust, and spent and washing water.

reducing pollution at the source through new technologies or minimizing toxic waste is an objective of these industries. Companies are looking for ways to replace some of the raw materials used. They are also investigating more efficient methods that can recycle some of the compounds found in the waste.

Until new technologies are found, industry is required to treat its waste before discharging into sewers or downstream reservoirs. For such an existing battery manufacturing company, design a treatment plant capable of treating 1000 gallons of liquid waste per day.

Case 2.

Pollution reduction and prevention in industry became an important objective and a priority for both the Environmental Protection Agency and the manufacturing companies.

Materials used in battery industries (lead, chromium, zinc, mercury, arsenic, cadmium) are high sources of toxicity. Battery-related pollution is found in raw materials, manufacturing processes, use and disposal.

The "Forever Working" Battery Company is under construction. The company is a small to medium organization. Preliminary and pilot plant studies indicate that the generated influent waste stream will be around 500 gallons per day and includes the following;

Parameters (mg/lit)

Chemical Oxygen Demand (COD) 1200 - 1300

Total Suspended Solids 60 - 70

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Heavy Metals (mg/lit)

Copper 1 - 1.5

Lead 30 - 36

Nickel 0.5 - 0.7

Silver 0.01

Zinc 3 - 5

Chromium 1 - 1.2

Cadmium 0.1

Arsenic 0.2 - 0.4

—

Other Substances (mg/lit)

Oil and Greases 8 - 10

Cyanide 0.04 - 0.06

You have been asked to lead a team responsible for assuring that the "Forever Working" Company meets and sustains the regulations of all federal and state environmental agencies. Develop a treatment plan that will accomplish this task.

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SOLUTION TO CASE STUDY #3: Municipal Wastewater Treatment Facilities

Problem Statement for Case 3.

The population increase in the state of Easy Living has brought about growing demands for a new supply of potable water, especially in the area of Freedom City (a residential community). It is anticipated that the city will have a population potential for approximately 50,000 new residents over the next 50 years. 1,000 visitors per day are also expected when the new shopping mall is completed within the next two years. The existing treatment facilities are limited and allow no future expansion. The purpose of any treatment plant is to provide water that is chemically and bacteriologically safe for human consumption and domestic use. A surface water reservoir is located 8 miles north of Freedom City and is assumed to contain enough water supply at all times. Preliminary studies by the Pussy Cat water company indicate that the average use of water per capita is 300 gallons per day. This includes residential interior, business, schools, recreation and fire fighting use. It also indicates a peaking factor equal to 2. The company also studied the quality of the reservoir water. Analysis of a typical sample of the surface reservoir water gave the following information:

1. amount of dissolved oxygen = 5 mg/L
2. turbidity = 8 NTU
3. suspended solids = 30 mg/L
4. BOD₅ = 8 mg/L
5. dissolved inorganic salts (mostly calcium) = 300 mg/L
6. 2000 fecal coliform per 100 mL
7. some debris and fish
8. no radioactive contaminants

The city has designated a space located 4 miles south of the reservoir as a site for the construction of a new water treatment plant. It has an elevation 400 ft lower than the reservoir. This elevation is also 200 ft higher than the ground surface of the city.

Design a suitable water treatment plant that solves the water shortage problem and meets the EPA standards. The following design criteria apply:

1. Minimum detention time in a sedimentation tank is 4 hours
2. Maximum overflow rate in a sedimentation tank is $30 \text{ m}^3/\text{m}^2$ a day.
3. Efficiency for sedimentation tank no less than 85%
4. Filtrate rate in a treatment filter is $3 \text{ L}/\text{m}^2$ per second
5. Pumping station efficiency is no less than 80%
6. Flocculation average detention time no less than 30 minutes



Justify and design parameters used and give references for any assumed values.

Introduction

Water treatment plants are designed to achieve two basic goals: "speed up the natural purification process that occur in streams, rivers and lakes and reduce toxic containinants that might otherwise interfere with the natural process."

In the design of a water treatment facility for the city of Freedom, environmental percussions must be adressed. The areas of most concern are the air, water and local ecology surrounding the plant. The following should be considered:

(1) Air

any gases or vapors resulting from the treatment be non-toxic,
any chemicals used in the treatment are properly stored and processed,
emergency backup system for contamination is installed.

(2) Water

water returning to the environment is non-toxic,
waste products are treated before discharging,
efficient distribution system,
prevention design for flood or overflow.

(3) Ecology

safety of fish and marine life,
preservation of non-aquatic animal wildlife,
maintenance of existing wildlife habitat,
reforestation of local vegetation,
environmental landscaping.

The building facilities will include besides the treatment sections, an administration section, a laboratory and workshop section, water storage facility and several parking lots. The site area should allow further expansion. The design should be flexible to permit any control adjustments required to compensate for any changes in the composition and behavior of the influent and its contents. Finally a proper on-site safety program that includes regular training in safety and emergency procedures should be established.

The major stages of the treatment process are:

- 1. Intake and Screening**
- 2. Coagulation and Flocculation**
- 3. Sedimintation**
- 4. Filtration**

5. Disinfection

The Design Process

Intake and Screening

Because of the geography of the reservoir location, the treatment site and city elevation, the screening operation will take place along-side the water reservoir. The design will rely on the natural water pressure of the reservoir to force the water through the screening section. Placing the screening operation in close proximity to the reservoir allows quick and safe return of the retained fish and other aquatic life to their natural habitat. Effective screening should remove approximately 10% of the suspended solids and all the debris.

Daily amount of water used by residents	= 50,000 x 300	= 15,000,000 gallons
Daily amount of water used by visitors	= 1000 x 300 x 2/24	= 25,000 gallons
Maintenance, spillage and evaporation		= 5,000 gallons/day
Average daily consumption		= 15,030,000 gallon
Peak flow	= 2 x 15,030,000	= 30,060,000 gallons/day (347.92 gallons/sec)

To avoid potential intake of surface debris and bottom sludge, the intake pipe entrance is located at 30 ft. below the surface. The pipe opening is covered with a grating composed of metal bars spaced 2 inches apart to prevent the influx of extremely large debris.

Inlet velocity should not exceed 3 ft/sec to prevent debris from being forced through the screens.

$$v = 3 \text{ ft/sec}$$

$$Q = 347.92 \times 8.33 / 62.4 = 46.5 \text{ ft}^3/\text{sec}$$

$$A = Q / v = 15.5 \text{ ft}^2 = 3.14 D^2 / 4$$

$$D = \text{diameter of pipe} = 3.44 \text{ ft}$$

take $D = 4.5 \text{ ft}$. Use concrete as material of the pipe due to its durability and low cost.

As recommended, head loss due to each screen should not exceed 0.3 ft.



Now, the equation of Bernoulli will be used to calculate the location of the screening facility. Taking the inlet velocity as zero (very large reservoir) and assuming atmospheric pressure and using Darcy-Weisbach expression for head loss, the equation reduces to:

$$30 = v^2 / 2g + H_b + 0.0006 L * v^2$$

where

H_b = height of screen above intake level

L = the length of the pipe.

Solving the above equation iteratively gives a slight drop in elevation from reservoir surface. Taking into account the natural grade in the vicinity of the reservoir, location of screening would be 30.5 ft from water edge.

Two wedgewire rotary screens will be used, one with 1/2 inch mesh to remove large debris and aquatic life, the second with 1/8 inch mesh to remove suspended particulate matter. Based on recommended value of screen capacity of 10 to 30 gal / ft²-min, screen dimensions are 5 ft diameter and 10 ft long each.

Waste accumulates on the screening surface is scraped using a rubber flange and sprayer system. Debris is collected in a waste tank of dimensions 9 x 6 x 6 ft. Aquatic life will be returned to the reservoir. Periodic cleaning of tank is required. The filtered water enters a catch basin tank, from which it proceeds to the second screen. The basin tank has dimensions of 8 x 15 x 12 ft assuming 30 sec lag.

A backup screening system should be available and should be easily mounted in case of any rotary screening failure. Screening is housed on floor of dimensions 50 x 30 ft.

After screening, water is transported in concrete piping system of 4.5 ft diameter to the treatment facility using decreasing gradual elevation mechanism.

Coagulation and Flocculation

This operation is carried out to form larger particles to facilitate their settling and reduce turbidity. Chemicals such as metallic salts (coagulants) are added to water at the inlet section of the flocculator to help agglomerate the particles. Mixing takes place in this section to bring more collision between particles, so flocs can be formed. The flocs then move to the detention section where wooden paddles regulate the motion of these particles. Chemical dosages can be determined experimentally or by searching existing data. In our case a mixture of Alum, cationic polymer and caustic soda is used. The dosage is as follows:

Alum	2.4 to 3.0 mg/L
Cationic polymer	0.5 to 2.0 mg/L
Caustic soda	2.0 to 4.0 mg/L

These data were obtained from a typical treatment facility.



Storage and piping for chemicals are made of polyethylene to resist corrosion. Hydraulic jump is chosen for mixing because it requires minimum maintenance. Coagulant should be added at the point of maximum turbulence.

Mixing Time = 3 minutes

Detection Time $t = V/Q$

Assuming $t = 50$ min,

$$V = 50 * 60 * 46.5 = 139,528 \text{ ft}^3$$

Use four flocculation tanks each of volume $139,528/4 = 34,882 \text{ ft}^3$

Water leaves screening system and enters the mixing section with a velocity = 3 ft/sec. Assuming head loss of 2 ft through the hydraulic jump mixing section, water enters the settling section with velocity = 1 ft/sec.

Velocity of paddle = 2 ft/sec = v_p

$$\begin{aligned} P &= \text{Power} = C A_p (\text{Density}) v_p^3 / 2 \\ &= 1.8 (0.2) (\text{Cross-sectional area of tank}) (62.4) (2^3) / 2 \\ &= 37.908 L^2 * \text{Watt} \end{aligned}$$

Let

$$\begin{aligned} G * t &= 105 = (50 * 60) G \\ G &= 33.33 \text{ sec}^{-1} \\ G^2 &= P / (V * \text{viscosity}) = 37.908 L^2 / (34882 * 0.00066) \end{aligned}$$

Therefore,

$$\begin{aligned} L &= 25.97 \text{ ft} \\ V &= L^2 W = 34,882 \text{ ft}^3 = \text{tank volume} \\ W &= 51.72 \text{ ft} \end{aligned}$$

The tank dimensions are $25.97 * 25.97 * 51.72$

$$\begin{aligned} \text{Total } A_p &= 0.2 * L^2 \\ &= 134.88 \text{ ft}^2 \end{aligned}$$

Using 20 paddles with one ft. spacing,

Area of paddle = $134.88/20 = 6.74 \text{ ft}^2$
with dimensions $3.54 * 1.9$ for the paddle.

Assume velocity of inflow to settling section = 1 ft/sec

Using steel pipes to inlet and exit from tank:

$$Q = 46.5$$

Using 4 pipes,

$$Q = 46.5 / 4 = 11.625 \text{ ft}^3$$

$$3.14 * r^2 * v = 11.625 = 3.14 * r^2 * 1$$

$$r = 1.92 \text{ and } d = 3.84 \text{ ft.}$$

Tanks are made of concrete and lined with polyethylene because of its chemical resistance.

Sedimentation

Suspended solids originally large and those formed by flocculation are given enough time to settle by gravity. Sedimentation is responsible for the removal of the majority of the suspended solids (over 80%). The technique used here is that of a horizontal flow sedimentation. Quiescent conditions should be established in the sedimentation tank through slow and smooth flow of water. A large detention time is required, i.e. a long and narrow tank is used. Sedimentation tanks have four zones: (1) inlet zone where very little settling is observed and the flow should be evenly distributed throughout the tank, (2) settling zone where particles start to settle as a result of quiescent conditions, (3) sludge storage zone where most of the settling takes place. The sludge at the bottom should be removed periodically to allow for more settling and prevent particles from moving back upward and disturb the flow, and (4) outlet zone where partially clear water exits the tank and moves to the filtration step.

To facilitate the design, four particle sizes ranging from 0.004 inch to 0.2 inch, all with the same density of 66 lb/ft³ and each size contributes the same amount to the total suspended solid concentration. An automated sludge removal will be constructed as part of the tank. This is a conveyor type chain pulling transverse blades which sweep the sludge toward a sump.

Total suspended solids concentration = 30 mg/L

$$= 46.5 * 28.316 * 0.03 = 39.50 \text{ g/sec}$$

$$= 0.087 \text{ lb/sec}$$



Assuming the smallest particles as 0.004 inch or 0.1 mm, particles with diameter s larger than 0.1 mm will be removed completely.

Using Stokes Equation for the smallest particles,

$$\begin{aligned} v_{\text{small}} &= (\text{density}_s - \text{density}) * g * d^2 / (18 * \text{viscosity}) \\ &= (66 - 62.4) (32.17) (0.00033)^2 / 18 * 0.0007 \\ &= 0.00102 \text{ ft/sec.} \end{aligned}$$

Assuming 50% of these particles is removed,

$$\begin{aligned} v_{\text{average}} &= 0.00102 / 0.5 = 0.00204 \text{ ft/sec} \\ d_{\text{average}} &= [(18 * \text{viscosity} * v_{\text{average}}) / (g * (\text{density}_s - \text{density}))]^{0.5} \\ &= 0.00047 \text{ ft} \\ \text{Re} &= (0.00047 * 0.00204 * 62.4) / 0.0007 = 0.085 < 0.3 \\ q_o &= 30 \text{ m}^3 / (\text{m}^2 * \text{day}) = 0.0011574 \text{ ft}^3 / (\text{ft}^2 * \text{sec}) \end{aligned}$$

Using 4 hours sedimentation time,

$$\begin{aligned} V &= \text{volume} = Q * t = 46.5 * 4 * 3600 = 669,600 \text{ ft}^3 \\ H_{\text{max}} &= \text{height} = v * t = 0.00204 * 4 * 3600 = 29.38 \text{ ft} \\ A &= 46.5 / q_o = 46.5 / 0.0011574 = 40,184 \text{ ft}^2 \\ H &= 669,600 / 40,184 = 16.66 \text{ ft} < 29.38 \text{ ft} \end{aligned}$$

Two tanks will be used , each of volume = 669,600 / 2 = 335,000 ft³ approximately.

$$\begin{aligned} A &= 335,000 / 16.66 = 20,100 \text{ ft}^2 \\ q_o &= 46.5 / (2 * 20,100) = 0.0011567 \text{ ft}^3/\text{ft}^2 \end{aligned}$$

Assuming 300 ft length,

$$\begin{aligned} w &= 20,100 / 300 = 67 \text{ ft} \\ \text{Stream exit velocity} &= 300 / (4 * 3600) = 0.0208 \text{ ft/sec} \end{aligned}$$

Water exits the sedimentation tank and continues on to filtration.

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Filtration

The remaining suspended solids (10 to 15 %) are removed by filtration. The resulting effluent is clear and colorless.

Filtration rate is constant at 3 lit / sq.m-sec and the head loss should not exceed 9.8 ft. Eight filter, each with filtration capacity of 4. million gallons per day are used. Because of the high filtration rate, the rapid sand filtration process is used. A layer of anthracite occupies the upper part of filter, sand and anthracite are chosen because of their particle size, porosity and specific gravity. The particles that escapes the large and light anthracite layer will be trapped in the fine sand layer. An 8 inches gravel layer is placed between the sand layer and the underdrain system to prevent sand from slipping into the underdrain system. The design is based on the peak conditions to ensure smooth operation at any time. The underdrain system consists of central manifold with laterals, 7 inches diameter steel pipes on each side containing a number of orifices (radius = 0.25 inches). A back washing system is to be used to remove any clogging and prevent any dramatic increase in the headloss or shearing stress on the cake. A recommended rate of washing is 15 to 20. gpm / sq.ft. The backwash valve has to be opened slowly to avoid upsetting the filter layers. The differences between the specific gravities of the layers materials allow the filter media to expand and fall without intermixing. The low specific gravity suspended particles are disposed through a system of troughs. A control system is used to control the constant flow rate operation.

number of units = $30.06 / 4 = 7.5$ units

use 8 units each of capacity = 4 million gallons per day

3 lit / sq.m -sec = 4.43 gallons / sq. ft-sec

filtration area per unit = $4 \text{ million} / 24 * 60 * 4.43 = 630$. sq.ft

with dimensions of 42 x 15 ft

total headloss = sum of headlosses over the three layers

$\Delta P = \left\{ \frac{L}{g} \left(\text{fluid density} * v^2 (1-\text{porosity}) / d * \text{porosity}^3 * 150 * (1-\text{porosity}) / \text{Re} + 1.75 \right) \right\}$

Assuming L = 2 ft for anthracite and 1 ft. for sand

$\Delta P_{\text{sand}} = 1.8$

$\Delta P_{\text{anthracite}} = 4.72$

$\Delta P_{\text{gravel}} = 1.22$

total pressure head loss = 7.73 ft

where

sp gravity sand = 2.65, d = 0.002 ft.

sp gravity anthracite = 1.45, d = 0.005 ft.

sp gravity gravel = 4.5, d = 0.003 ft.

superficial velocity v = 0.5 ft/sec.

Area of orifice / area of filter bed = 0.0001 - 0.2

$$N (3.14) (0.02 \text{ ft})^2 / 630 = 0.0216$$

N = number of orifices = 10,000

Area of laterals / area of orifices = 2:4:1

$$\text{take ratio} = 3.14:1 = n (3.14) (3.5/12)^2 / 10,000 (3.14) (.022)$$

Number of laterals n = 160

Area of manifold / area of laterals = 1.5 - 3:1

$$a / 160 (3.14) (3.5/12)^2 = 3$$

a = 128 ft² with dimensions 40 * 3.2 ft

use space between orifices same as space between laterals. Each lateral has about 63 orifices. Tanks above the troughs are used for supplying the backwashing water. The filtrate now goes to the disinfection unit.

Disinfection

Disinfection is done using chlorine. Chlorine is effective in killing harmful organisms. It also controls odor.

Chlorine is stored in cylinders, each of one ton capacity in a climate control room with sufficient ventilation and away from the sun.

Chlorination facility is housed in a separate building. Safety procedures must be used in storage transporting and processing chlorine. Piping should be PVC schedule 80 to resist corrosion. It is released as a solution into the water through diffusers constructed on the pipes carrying the gas solution along the bottom third of the basin.

Chlorine monitors and feed control system are installed to ensure 1.0 mg residual chlorine. A plug flow is preferred to help retain the water in the basin for the required detention time. Contact time between the gas and the water depends on the residual concentration of the chlorine, temperature, and pH of the water.

Recommended dosage for 1.0 mg/L chlorine residual is 6 mg/L

Rate of Chlorine supply / day

$$= 6 (30.06) (10)^6 (3.76) / (454 * 1000)$$

$$= 1500 \text{ lbs/day}$$

using a 2 inch diameter injection pipe

$$A = 3.14 (1) / 144 = 0.0218 \text{ ft}^2$$

at a rate 75 gpm or 0.167 ft³/sec

$$\text{velocity of chlorine solution} = 0.167/0.0218 = 7.66 \text{ ft/sec}$$

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Assuming a pH = 7 and average temperature of 35 F for winter,
to achieve 2 coliform / 100 mL

$$N_t/N_o = 2 / 1000 = (1 + 0.23 t)^{-3}$$

$$t = 39.13$$

For a residual of 1. mg/L

$$\text{Contact time} = 39.13 / 1 = 39.13 \text{ minutes}$$

Use detention time of 60 minutes.

For summer with average temperature of water=60F, use detention time 30 minutes.

Volume of detention basin:

$$V = 46.5 (60) (60) = 167,400 \text{ ft}^3$$

Use two 100,000 ft³ basins with L/W > 20

Dimensions of basin are

$$h = 16 \text{ ft}$$

$$W = 15 \text{ ft}$$

$$L = 416 \text{ ft}$$

velocity of water traveling the basin

$$v = 46.5 / (16 * 15) = 0.193 \text{ ft/sec}$$

Baffles are used to regulate the flow along the basin. Four baffles, 16 x 15 x 1/3 ft for each basin.

The disinfected water now goes to the distribution system.

BERGEN COUNTY UTILITIES AUTHORITY (NJ)													
MONTHLY AVERAGE VALUES													
PARAMETERS	APR 94	MAY 94	JUNE 94	JULY 94	AUG 94	SEPT 94	OCT 94	NOV 94	DEC 94	JAN 95	FEB 95	MAR 95	YEARLY AVERAGE
BCUA FLOW (MGD)	95.817	83.453	75.682	73.655	73.455	63.92	62.094	64.496	72.356	74.274	69.073	70.816	73.258
BOD 5-DAY (INFLUENT)	170	181	203	171	165	179	195	152	155	178	189	178	176
BOD 5-DAY (EFFLUENT)	26	17	26	17	18	20	18	17	17	19	16	19	19
TSS (INFLUENT)	194	234	262	228	208	226	275	227	211	222	237	219	229
TSS (EFFLUENT)	25	17	16	14	14	18	15	21	19	18	16	17	18
AMMONIA-NITROGEN (influent), mg/L	18.8	21.1	21.8	22.5	19.6	24.7	24.3	24.8	25.4	24.3	26.1	25.1	23.2
AMMONIA-NITROGEN (effluent), mg/L	16.1	18.1	19.2	15.7	16.3	18.6	18.3	20.5	20.3	19.4	20.9	20.6	18.7
CYANIDE (effluent), mg/L	0.06	0.04	0.11	0.06	0.05	0.05	0.06	0.04	0.04	0.07	0.07	0.04	0.06
PHOSPHATE (effluent), mg/L	2.69	3.46	4.29	2.72	3.85	4.81	5.07	5.4	5.86	3.71	3.28	3.18	4.03
SQAR DATA (mg/kg)													
METALS													
arsenic	6.8	0.33	0.34	0.22	1.25	1.1	0.55	0.94	0.35	0.4	4.65	7.3	
beryllium	0.36 U	0.28	0.2	1.43	1.8	1.6	0.8	1.45	1.15	0.6	0.01 U	0.01 U	
cadmium	22.1	12.7	15.3	7.37	7	6.6	4.3	6	1.25	2.2	4.05	3.35	
chromium	223	292.6	330.5	261.9	518	490.8	354.2	454.5	66.7	223.2	33.9	141.7	
copper	513	651	694.8	793.9	742.8	562	495.3	529.5	126.5	526.2	449.4	203.6	
iron	33250	31498	38123	43028	40859	39987	44467	43232	135	25870	1842	6660	
lead	109.5	143.3	138.1	136.1	145.5	128.3	92.6	107.8	3.5	88.5	22	48.6	
mercury	0.98	0.35	0.32	0.93	0.56	0.41	0.93	0.19	0.18	0.45	0.01 U	0.17	
molybdenum	7.2 U	3.55	3.24	3.02	4	4.3	3.02	2.95	0.01 U	1.4	0.5	0.01 U	
nickel	118	206.1	271.5	258	319.6	314.3	243.3	405.2	24	208.8	95	77.8	
selenium	4.35	0.41	0.5	0.78	0.71	0.58	0.69	0.25	0.01 U	0.15	21.45	3.8	
silver	74.6	71.5	72.1	38.8	19.6	20	2.9	4.8	5.2	37.5	8.5	17.3	
zinc	662	69.8	111.8	1023.1	767.6	725.8	1047.5	853.9	91.1	700.8	459.4	232	
SELECTED CHEMICALS													
total nitrogen	6725	49909	66319	49425	45953	42131	35660	38900	13079	48580	59021	15605	
NH3 nitrogen	6000	13921	20215	11161	2181	1987	1338	1386	5255	22387	19683	4373	
nitrate nitrogen	28.4	56	52.4	50.9	46.9	45.5	51.3	64.6	13.7	45.4	20.1	14.9	
oil & grease	2690	41149	33669	26313	6901	17601	20728	20375	8536	58470	33213	3112	
phenols	89.7	21.2	40.8	22	57.9	57.3	47.9	43.5	287.9	370.9	618.9	1.7	
phosphorus	4700	15100	12694	14204	11694	15055	10257	15165	8754	11872	10480	7271	
calcium	22850	10518	13339	11019	11275	10925	11905	14130	2795	11658	22516	389684	
magnesium	3095	2721	2679	2933	2831	2461	3710	2815	1008	5330	4917	7783	
potassium	1570	1118	994	1266	923	813	684	844	337	1627	549	976	
cyanide	0.9 U	9	11.85	3.61	22.6	20.3	15.05	10.35	0.5	14.75	41	7.35	
fluoride	7.1	97.2	89.8	75.1	107.8	109.9	138.5	92.6	7.8	26.9	44.7	24.4	
chloride	8070	6441	5279	5807	7214	7207	9362	7050	5538	4310	2128	1917	
petroleum hydrocarbons	1390	10652	8129	8609	8860	8484	9352	9480	4593	14262	15227	2857	

BERGEN COUNTY UTILITIES AUTHORITY (NJ)													
MONTHLY AVERAGE VALUES													
PARAMETERS	APR 94	MAY 94	JUNE 94	JULY 94	AUG 94	SEPT 94	OCT 94	NOV 94	DEC 94	JAN 95	FEB 95	MAR 95	YEARLY AVERAGE
METAL CONCENTRATION (mg/L)													
INFLUENT													
arsenic	0.00103	0.00164	0.00198	0.00267	0.0015	0.00165	0.00183	0.001	0.001	0.00153	0.001	0.0014	0.0015
cadmium	0.0045	0.0044	0.0043	0.0053	0.0042	0.004	0.004	0.006	0.004	0.004	0.004	0.0042	0.0044
chromium (total)	0.059	0.018	0.021	0.049	0.034	0.03	0.03	0.082	0.088	0.011	0.031	0.049	0.0418
copper	0.078	0.141	0.068	0.114	0.14	0.16	0.105	0.09	0.073	0.07	0.086	0.076	0.1001
lead	0.042	0.042	0.042	0.057	0.042	0.044	0.062	0.046	0.044	0.049	0.042	0.042	0.0462
mercury	0.00048	0.00044	0.0005	0.0002	0.00043	0.0002	0.00063	0.00036	0.00033	0.00035	0.0003	0.00022	0.0004
nickel	0.052	0.043	0.015	0.029	0.018	0.03	0.03	0.025	0.038	0.033	0.023	0.018	0.0295
silver	0.012	0.017	0.017	0.073	0.018	0.017	0.019	0.017	0.018	0.012	0.015	0.013	0.0207
zinc	0.085	0.117	0.113	0.115	0.9	0.144	0.141	0.125	0.143	0.103	0.128	0.125	0.1866
EFFLUENT (mg/L)													
arsenic	7E-05	0.00125	0.00068	0.001	0.00073	0.00093	0.00108	0.001	0.001	0.00085	0.001	0.001	0.0009
cadmium	0.004	0.004	0.004	0.004	0.004	0.004	0.0035	0.0268	0.004	0.004	0.004	0.004	0.0059
chromium (total)	0.005	0.014	0.005	0.016	0.006	0.014	0.013	0.027	0.025	0.006	0.006	0.022	0.0133
copper	0.032	0.068	0.038	0.022	0.02	0.041	0.017	0.028	0.02	0.013	0.009	0.013	0.0268
lead	0.051	0.042	0.037	0.042	0.042	0.042	0.028	0.042	0.042	0.042	0.042	0.042	0.0412
mercury	0.00023	0.0002	0.0002	0.0002	0.0002	0.0002	0.00023	0.0002	0.00029	0.00016	0.00015	0.0002	0.0002
nickel	0.013	0.03	0.011	0.015	0.012	0.019	0.023	0.008	0.014	0.026	0.015	0.01	0.0163
silver	0.01	0.009	0.007	0.019	0.007	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.0102
zinc	0.05	0.061	0.054	0.054	0.035	0.073	0.053	0.05	0.048	0.048	0.051	0.064	0.0534
VOLATILE ORGANICS													
INFLUENT (mg/L)													
1,2-dichloroethene, trans	0.00397	0.0016	0.00363	0.00269	0.00266	0.00183	0.00254	0.0016	0.0033	0.0033	0.00253	0.00376	0.0028
chloroform	0.00562	0.00598	0.00573	0.00827	0.00651	0.00709	0.0312	0.00333	0.00507	0.00392	0.00487	0.00287	0.0075
1,1,1-trichloroethane	0.00242	0.00975	0.00129	0.00078	0.0023	0.00149	0.00389	0.00096	0.00139	0.00238	0.00101	0.00679	0.0029
bromodichloromethane	0.00086	0.00086	0.00101	0.00045	0.00086	0.00043	0.0007	0.00086	0.00043	0.00052	0.00021	0.00191	0.0008
tetrachloroethene	0.0124	0.00607	0.0168	0.00428	0.004	0.00459	0.0121	0.00424	0.00438	0.00728	0.00487	0.0144	0.0080
toluene	0.033	0.0163	0.00623	0.00855	0.00842	0.00771	0.0156	0.00659	0.0109	0.0128	0.0151	0.0148	0.0130
m-xylene	0.0152	0.00279	0.00663	0.00497	0.00318	0.00605	0.0122	0.00352	0.00026	0.0047	0.0022	0.00315	0.0054
o,p-xylenes	0.015	0.00262	0.00883	0.00644	0.00776	0.00659	0.0164	0.00936	0.00136	0.00427	0.00076	0.00432	0.0070
EFFLUENT (mg/L)													
1,2-dichloroethene, trans	0.0023	0.0008	0.00143	0.00042	0.00076	0.0008	0.0008	0.0008	0.00177	0.00142	0.0008	0.00064	0.0011
chloroform	0.00807	0.00526	0.00615	0.00735	0.00405	0.0083	0.00365	0.00282	0.00528	0.00665	0.00547	0.00316	0.0055
1,1,1-trichloroethane	0.00113	0.00471	0.00113	0.00113	0.00031	0.00034	0.00113	0.00113	0.00045	0.00098	0.00113	0.00033	0.0012
bromodichloromethane	0.00263	0.00115	0.00102	0.00261	0.00083	0.0016	0.00123	0.00096	0.00156	0.00113	0.00052	0.001	0.0014
tetrachloroethene	0.00199	0.00097	0.00326	0.00099	0.00059	0.00065	0.00097	0.00095	0.00097	0.00405	0.00097	0.00465	0.0018
toluene	0.00144	0.00063	0.0021	0.00262	0.00079	0.00087	0.00063	0.00063	0.00197	0.00379	0.00063	0.00111	0.0014

BERGEN COUNTY UTILITIES AUTHORITY (NJ)													
MONTHLY AVERAGE VALUES													
PARAMETERS	APR 94	MAY 94	JUNE 94	JULY 94	AUG 94	SEPT 94	OCT 94	NOV 94	DEC 94	JAN 95	FEB 95	MAR 95	YEARLY AVERAGE
ADDITIONAL COMPOUNDS													
INFLUENT (ug/l)													
acetone	4690	1039	1543	269	3735	2447	636	1288	418	16225	3672	4572	3378
2-chlorotoluene	206	17.5	137	19.5	109	225	49.7	14.4	113	53.9	22.1	39.3	83.87
4-chlorotoluene	12.2	1.7	14.5	1.81	21.9	31.8	6.83	1.7 U	14.6	7.21	1.95	5.33	9.99
BASE NEUTRALS													
INFLUENT (ug/l)													
bis-2-ethyl hexyl phthalate	17.42	26.58	21.8	13.88	125.2	8.35	21.22	23.56	7.42	33.79	21.88	33.09	29.516
butyl benzyl phthalate	2.35	0.74	4.5	3.84	3.46	4.66	2.42	1.24	0.54	2.67	0.98	15.54	3.578
dibutyl phthalate	5.43	4.12	10.26	5.02	3.86	6.6	3.1	1.71	2.85	12.28	3.86	6.11	5.433
diethyl phthalate	3.9	0.83	5.86	5.3	0.82	3.96	5.56	1.94	1.35	2.34	1.88	5.78	3.293
di-n-octyl-phthalate	2.84	1.8	2.12	0.52	6.71	2.27	0.55	1.68	0.25	5.08	6.65	3.81	2.857
naphthalene	3.56	1.09	0.49	0.44	0.26	1.39	0.4	0.64	31.91	1.01	0.75	1	3.578
EFFLUENT (ug/l)													
bis-2-ethyl hexyl phthalate	108.12	10.8	17.18	7.38	11.6	21.26	11.45	2.41	6	3.35	4.27	3.23	17.254
butyl benzyl phthalate	0.7	0.19	1.27	1.15	1.28	1.15	1.15	0.68	0.1	1.15	0.12	0.3	0.770
dibutyl phthalate	6.5	2.46	2.83	1.18	2.95	2.2	0.9	1.45	0.73	1.45	0.35	0.82	1.985
diethyl phthalate	1.99	0.58	0.83	0.43	0.99	0.85	1.28	0.3	0.77	1.48	1.02	0.59	0.926
di-n-octyl-phthalate	4.96	1.15	0.86	0.44	0.87	1.16	1.8	1.14	4.3	1.16	1.2	0.25	1.591
naphthalene	1.72	0.19	0.42	0.41	0.42	0.59	0.12	0.4	1.25	0.49	0.17	0.32	0.542
ACID FRACTION (ug/l)													
phenol (influent)	6.57	8.09	8.1	4.82	10.02	8.7	13.98	6.15	4.83	6.05	2.75	8.24	7.358
phenol (effluent)	1.19	1.61	3.98	3.88	0.78	4.27	1.83	0.41	0.87	0.3	0.85	1.03	1.750
NOTE													
"U" INDICATES COMPOUND ANALYZED BUT NOT DETECTED													
"B" INDICATES COMPOUND FOUND IN ASSOCIATED BLANK													
"J" INDICATES COMPOUND CONCENTRATION FOUND BELOW MDL													
"E" INDICATES COMPOUND CONCENTRATION EXCEEDS CALIBRATION LIMIT													
"ND" INDICATES NO DATA AVAILABLE FOR THIS PARAMETER													

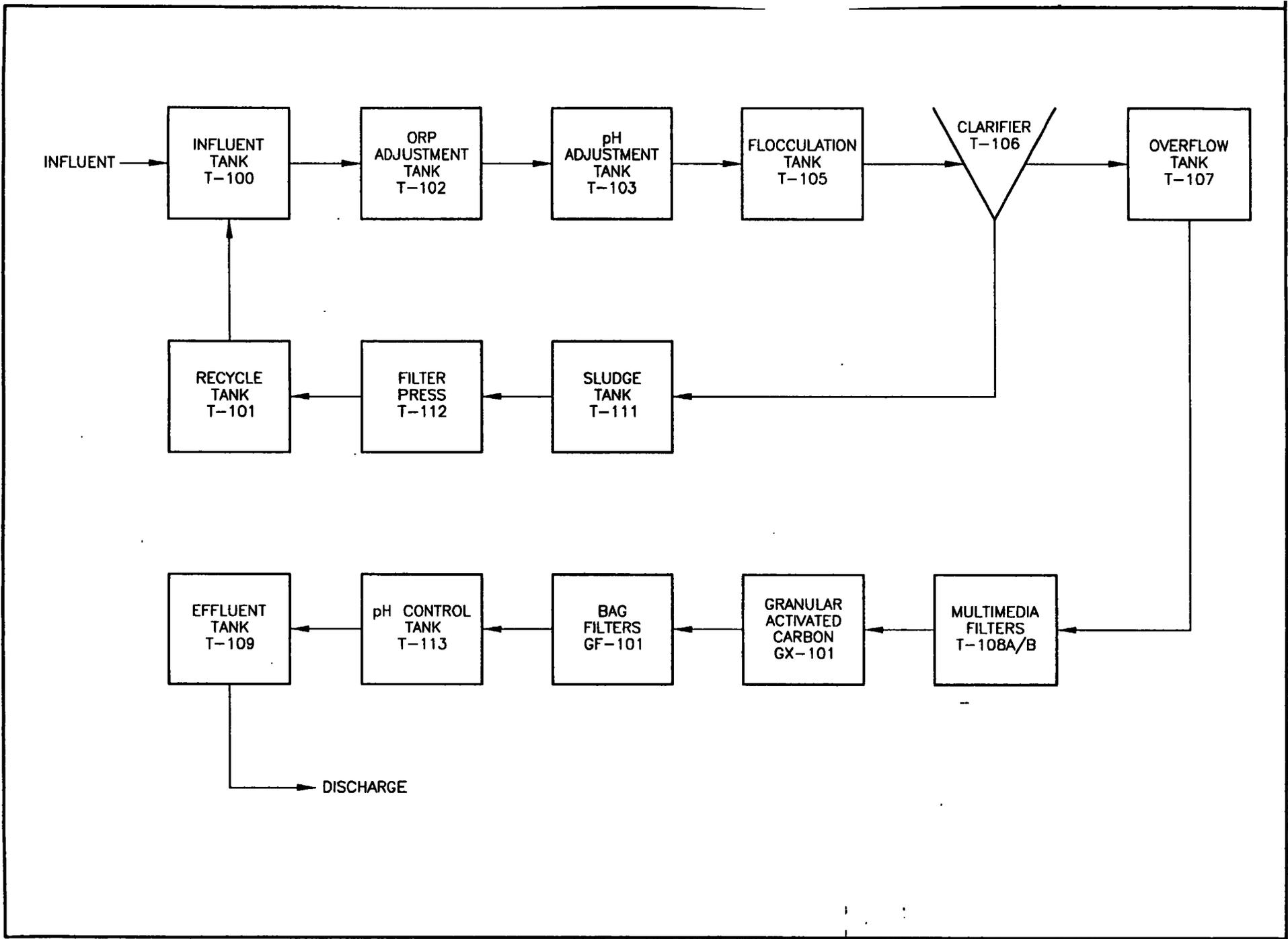
INFLUENT WASTEWATER STREAM OF A TYPICAL ELECTROCHEMICAL INDUSTRY

	<i>Cr</i>	<i>Cu</i>	<i>As</i>	<i>Benzene</i>	<i>Ethyl Benzene</i>	<i>Toluene</i>	<i>Xylene</i>	<i>TPH</i>
	<i>ug/l</i>	<i>ug/l</i>	<i>ug/l</i>	<i>ug/l</i>	<i>ug/l</i>	<i>ug/l</i>	<i>ug/l</i>	<i>ug/l</i>
Oct 3	1580	<4	<2	95	1.2	53	47	440
Oct 5	1600	<4	4.9	120	2	75	57	550
Oct 10	1610	<4	4.1	110	1.2	74	55	520
Oct 12	1680	<4	<2	120	1.3	74	60	540
Oct 17	1700	<4	<2	150	1.7	100	74	690
Oct 19	1710	<4	<2	99	1.2	69	50	470
Oct 24	1760	<4	3.4	170	2.8	120	84	820
Oct 26	1770	<4	<2	160	2.1	120	84	810
Oct 30	1810	<4	<2	190	6.3	140	96	1000
Nov 2	1930	<4	2.2	160	2.4	110	78	730
Nov 7	1880	<4	<2	200	3.5	150	88	920
Nov 9	1800	<4	2	200	2.7	150	95	980
Nov 14	1850	<4	<2	200	2.1	140	89	950
Nov 16	1790	<4	3.5	190	2.2	140	90	1000
Nov 20	1870	<4	<2	200	2.5	130	78	890
Nov 21	1840	<4	<2	240	4.8	186	107	1100
Nov 28	2090	<4	2.7	220	4.3	160	94	930
Nov 30	2070	<4	<2	190	3.6	130	82	1200
Dec 5	2040	<4	<2	190	2.8	130	91	790
Dec 7	2040	<4	<2	200	4.1	140	90	1200
Dec 12	2120	<4	4.9	250	4.8	150	97	1200
Dec 14	2170	<4	3	240	4.3	150	100	1200
Dec 19	2630	<4	2.5	200	2.6	110	96	930
Dec 20	2230	<4	<2	210	3.2	130	100	1100
Dec 26	2470	<4	2.2	110	1.4	60	60	540
Dec 27	2270	<4	2.5	180	3.2	110	86	850

EFFLUENT WASTEWATER STREAM OF A TYPICAL ELECTROCHEMICAL INDUSTRY

	<i>Cr</i>	<i>Cu</i>	<i>As</i>	<i>Cr +6</i>	<i>Benzene</i>	<i>Ethyl Benzene</i>	<i>Toluene</i>	<i>Xylene</i>	<i>TPH</i>
	<i>ug/l</i>	<i>ug/l</i>	<i>ug/l</i>	<i>ug/l</i>	<i>ug/l</i>	<i>ug/l</i>	<i>ug/l</i>	<i>ug/l</i>	<i>ug/l</i>
Oct 3	10.9	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Oct 5	11.3	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Oct 10	6	<4	4.6	<20	<0.2	<0.2	<0.1	<0.3	<4
Oct 12	5.5	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Oct 17	5	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Oct 19	6.2	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Oct 24	9.3	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Oct 26	9.7	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Oct 30	17.2	<4	<2	<20	<0.2	<0.2	0.1	<0.3	<4
Nov 2	20.9	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Nov 7	8	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Nov 9	8.1	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Nov 14	10.3	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Nov 16	19	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Nov 20	8.2	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Nov 21	6.8	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Nov 28	10.8	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Nov 30	23.8	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Dec 5	12.3	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Dec 7	13.9	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Dec 12	13.4	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Dec 14	10.3	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Dec 19	22	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Dec 20	11.4	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Dec 26	<3	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4
Dec 27	4.4	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4

TPH: Total Petroleum Hydrocarbons



ELECTROCHEMICAL TREATMENT SYSTEM

T-102 ORP ADJUSTMENT TANK-- INTRODUCTION OF FERROUS ION SOLUTION USING AN EXCESS OF STOICHIOMETRIC 3.2 POUNDS OF IRON PER ONE POUND CHROMIUM. Cr6 REDUCED TO Cr3. $3\text{Fe}(\text{OH})_2 + \text{CrO}_4^{2-} + 4\text{H}_2\text{O} \rightarrow 3\text{Fe}(\text{OH})_3 + \text{Cr}(\text{OH})_3 + 2\text{OH}^-$ SULFURIC ACID USED TO REDUCE PH TO 3 TO PROMOTE REDOX REACTION.

T-103 PH ADJUSTMENT TANK-- PH ADJUSTED TO 8.5 USING SODIUM HYDROXIDE TO PROMOTE PRECIPITATION OF METALLIC HYDROXIDES.

T-105 FLOCCULATION TANK-- POLYELECTROLYTE IS ADDED TO PROMOTE COAGULATION AND FLOCCULATION OF METALLIC HYDROXIDE PRECIPITATES.

T-106 CLARIFIER-- INCLINED PLATE CLARIFIER TO INHANCE SOLID SEPARATION.

T-107 OVERFLOW TANK-- CLARIFIED WATER.

T-108 A/B MULTIMEDIA FILTERS-- SUSPENDED SOLIDS REMOVAL.

GRANULAR ACTIVATED CARBON-- REMOVE BETX / METAL POLISHING.

BAG FILTERS-- FURTHER REDUCE SUSPENDED SOLIDS.

PH CONTROL TANK-- PH ADJUSTMENT TO A DISCHARGE RANGE 6 TO 8.5

Oct 95		INFLUENT (T100)							EFFLUENT (T109)							CARBON MID-BED							
Const. Units	Cr ug/l	Cu ug/l	As ug/l	B ug/l	E ug/l	T ug/l	X ug/l	TPH-g ug/l	Cr ug/l	Cu ug/l	As ug/l	Cr+6 ug/l	B ug/l	E ug/l	T ug/l	X ug/l	TPH-g ug/l	B ug/l	E ug/l	T ug/l	X ug/l	TPH-g ug/l	
Date	Day																						
1	S																						
2	M																						
3	T	1580	<4	<2	95	1.2	53	47	440	10.9	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
4	W																						
5	TH	1600	<4	4.9	120	2.0	75	57	550	11.3	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
6	F																						
7	S																						
8	S																						
9	M																						
10	T	1610	<4	4.1	110	1.2	74	55	520	6.0	<4	4.6	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
11	W																						
12	TH	1680	<4	<2	120	1.3	74	60	540	5.5	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
13	F																						
14	S																						
15	S																						
16	M																						
17	T	1700	<4	<2	150	1.7	100	74	690	5.0	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
18	W																						
19	TH	1710	<4	<2	99	1.2	69	50	470	6.2	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
20	F																						
21	S																						
22	S																						
23	M																						
24	T	1760	<4	3.4	170	2.8	120	84	820	9.3	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
25	W																						
26	TH	1770	<4	<2	160	2.1	120	84	810	9.7	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
27	F																						
28	S																						
29	S																						
30	M	1810	<4	<2	190	6.3	140	96	1000	17.2	<4	<2	<20	<0.2	<0.2	0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
31	T																						
Median Limit		1700	<4	<2	120	1.7	75	60	550	9.3 20	<4 100	<2 10	<20	<0.2 <DL	<0.2 <DL	<0.1 <DL	<0.3 <DL	<4 <DL	<0.2	<0.2	<0.1	<0.3	<4
Maximum Limit		1810	<4	4.9	190	6.3	140	96	1000	17.2 50	<4 200	4.6 50	<20	<0.2 <DL	<0.2 <DL	0.1 <DL	<0.3 <DL	<4 <DL	<0.2	<0.2	<0.1	<0.3	<4
MDL ug/l		3	4	2	0.2	0.2	0.1	0.3	4.0	3	4	2	20	0.2	0.2	0.1	0.3	4.0	0.2	0.2	0.1	0.3	4.0
PQL ug/l		20	20	40	0.5	0.5	0.5	0.5	20	20	20	40	20	0.5	0.5	0.5	0.5	20	0.5	0.5	0.5	0.5	20

Nov 85		INFLUENT (T100)								EFFLUENT (T109)								CARBON MID-BED					
Const. Units	Cr ug/l	Cu ug/l	As ug/l	B ug/l	E ug/l	T ug/l	X ug/l	TPH-g ug/l	Cr ug/l	Cu ug/l	As ug/l	CFB ug/l	B ug/l	E ug/l	T ug/l	X ug/l	TPH-g ug/l	B ug/l	E ug/l	T ug/l	X ug/l	TPH-g ug/l	
Date	Day																						
1	W																						
2	Th	1830	<4	2.2	160	2.4	110	78	730	20.9	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
3	F																						
4	S																						
5	Su																						
6	M																						
7	T	1880	<4	<2	200	3.5	150	88	920	8	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
8	W	1800	<4	2.0	200	2.7	150	95	980	8.1	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
9	Th																						
10	F																						
11	S																						
12	Su																						
13	M																						
14	T	1850	<4	<2	200	2.1	140	89	950	10.3	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
15	W																						
16	Th	1780	<4	3.5	190	2.2	140	90	1000	19	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
17	F																						
18	S																						
19	Su																						
20	M	1870	<4	<2	200	2.5	130	78	890	8.2	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
21	T	1940	<4	<2	240	4.8	188	107	1100	6.8	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
22	W																						
23	Th																						
24	F																						
25	S																						
26	Su																						
27	M																						
28	T	2090	<4	2.7	220	4.3	160	94	930	10.8	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
29	W																						
30	Th	2070	<4	<2	190	3.6	130	82	1200.0	23.8	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
Median Limit		1880	<4	<2	200	2.7	140	89	950	10.3 20	<4 100	<2 10	<20	<0.2 <DL	<0.2 <DL	<0.1 <DL	<0.3 <DL	<4 <DL	<0.2	<0.2	<0.1	<0.3	<4
Maximum Limit		2090	<4	3.5	240	4.8	188	107	1200	23.8 50	<4 200	<2 50	<20	<0.2 <DL	<0.2 <DL	<0.1 <DL	<0.3 <DL	<4 <DL	<0.2	<0.2	<0.1	<0.3	<4
MDL ug/l		3	4	2	0.2	0.2	0.1	0.3	4	3	4	2	20	0.2	0.2	0.1	0.3	4	0.2	0.2	0.1	0.3	4
PQL ug/l		20	20	40	0.5	0.5	0.5	0.5	20	20	20	40	20	0.5	0.5	0.5	0.5	20	0.5	0.5	0.5	0.5	20

Dec 95		INFLUENT (T100)							EFFLUENT (T109)							CARBON MID-BED							
Const. Units	Cr ug/l	Cu ug/l	As ug/l	B ug/l	E ug/l	T ug/l	X ug/l	TPH-g ug/l	Cr ug/l	Cu ug/l	As ug/l	Cr+8 ug/l	B ug/l	E ug/l	T ug/l	X ug/l	TPH-g ug/l	B ug/l	E ug/l	T ug/l	X ug/l	TPH-g ug/l	
Date	Day																						
1	F																						
2	S																						
3	Su																						
4	M																						
5	T	2040	<4	<2	190	2.8	130	91	790.0				<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4	
6	W	2040	<4	<2	200	4.1	140	90	1200.0	12.3	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
7	Th	2040	<4	<2	200	4.1	140	90	1200.0	13.9	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
8	F																						
9	S																						
10	Su																						
11	M																						
12	T	2120	<4	4.9	250	4.8	150	97	1200	13.4	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
13	W	2170	<4	3.0	240	4.3	150	100	1200	10.3	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
14	Th	2170	<4	3.0	240	4.3	150	100	1200	10.3	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
15	F																						
16	S																						
17	Su																						
18	M																						
19	T	2630	<4	2.5	200	2.6	110	96	930	22.0	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
20	W	2230	<4	<2	210	3.2	130	100	1100	11.4	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
21	Th	2230	<4	<2	210	3.2	130	100	1100	11.4	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
22	F																						
23	S																						
24	Su																						
25	M																						
26	T	2470	<4	2.2	110	1.4	60	60	540	<3	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
27	W	2270	<4	2.5	180	3.2	110	86	850	4.4	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
28	Th																						
29	F																						
30	S																						
31	Su																						
Median Limit		2200	<4	2.3	200	3.2	130	93.5	1015	11.85	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
										20	100	10		<DL	<DL	<DL	<DL	<DL					
Maximum Limit		2630	<4	4.9	250	4.8	150	100	1200	22	<4	<2	<20	<0.2	<0.2	<0.1	<0.3	<4	<0.2	<0.2	<0.1	<0.3	<4
										50	200	50		<DL	<DL	<DL	<DL	<DL					
MDL ug/l		3	4	2	0.2	0.2	0.1	0.3	4	3	4	2	20	0.2	0.2	0.1	0.3	4	0.2	0.2	0.1	0.3	4
PQL ug/l		20	20	40	0.5	0.5	0.5	0.5	20	20	20	40	20	0.5	0.5	0.5	0.5	20	0.5	0.5	0.5	0.5	20

EFFLUENT STREAM OF A PHARMACEUTICAL INDUSTRY

Date	O & G mg/L	PHC mg/L	TSS mg/L	BOD5 mg/L
Jan 19, 94	64	33	N/A	N/A
Feb 10, 94	25	19	N/A	N/A
Mar 4, 94	30	15	N/A	N/A
Apr 14, 94	82	61	N/A	N/A
May 6, 94	96	79	110	2020
May 19, 94	N/A	N/A	N/A	N/A
Jun 16, 94	509	377	N/A	N/A
Jun 23, 94	87	65	N/A	N/A
July 14, 94	57	28	N/A	N/A
Aug 5, 94	211	168	N/A	N/A
Aug 26, 94	21.2	10.7	N/A	N/A
Sept 2, 94	6.2	0.9	N/A	N/A
Sept 9, 94	250	160	N/A	N/A
Sept 16, 94	108	26	N/A	N/A
Sept 23, 94	134	129	N/A	N/A
Sept 30, 94	60	38	N/A	N/A
Oct 7, 94	143	138	N/A	N/A
Oct 14, 94	18	15	N/A	N/A
Oct 21, 94	111	89	N/A	N/A
Oct 28, 94	22	6.9	N/A	N/A
Nov 4, 94	20	11	110	2235
Nov 11, 94	336	301	N/A	N/A
Nov 18, 94	5.8	4	N/A	N/A
Nov 22, 94	58	56	N/A	N/A
Nov 29, 94	30	30	N/A	N/A
Dec 2, 94	22	18	N/A	N/A
Dec 9, 94	9.4	5.4	N/A	N/A
Dec 16, 94	5.2	2.7	N/A	N/A
Dec 22, 94	317	156	N/A	N/A
Dec 30, 94	34	34	N/A	N/A
Jan 6, 95	5.9	5.8	N/A	N/A
Jan 13, 95	28	19	N/A	N/A
Jan 20, 95	180	110	N/A	N/A
Jan 27, 95	90	61	N/A	N/A
Feb 3, 95	128	105	N/A	N/A
Feb 10, 95	24	21	N/A	N/A
Feb 17, 95	135	57	N/A	N/A
Feb 24, 95	5.3	4.2	N/A	N/A
Mar 3, 95	32	23	N/A	N/A
Mar 10, 95	13	5.5	N/A	N/A
Mar 17, 95	10	6.6	N/A	N/A
Mar 24, 95	142	116	N/A	N/A
Mar 31, 95	28	5.6	N/A	N/A
Apr 7, 95	16	11	N/A	N/A
Apr 14, 95	53	33	N/A	N/A
Apr 21, 95	258	182	N/A	N/A
Apr 28, 95	91	77	N/A	N/A
May 5, 95	22	7.2	N/A	N/A
May 12, 95	110	78	N/A	N/A
May 19, 95	38	26	94	4842
May 26, 95	407	340	N/A	N/A

EFFLUENT STREAM OF A PHARMACEUTICAL INDUSTRY

Date	O & G	PHC	TSS	BOD5
	<i>mg/L</i>	<i>mg/L</i>	<i>mg/L</i>	<i>mg/L</i>
Jun 2, 95	27	6.2	N/A	N/A
Jun 9, 95	376	334	N/A	N/A
Jun 16, 95	104	36	N/A	N/A
Jun 23, 95	5.6	3.4	N/A	N/A
Jun 30, 95	13	7.8	N/A	N/A
Jul 7, 95	8.1	0.9	N/A	N/A
Jul 14, 95	4	1.6	N/A	N/A
Jul 21, 95	15	11	N/A	N/A
Jul 28, 95	145	139.8	N/A	N/A
Aug 4, 95	45	22	N/A	N/A
Aug 11, 95	368	308	N/A	N/A
Aug 18, 95	9.8	5.4	N/A	N/A
Aug 25, 95	26	3.8	N/A	N/A
Sept 1, 95	17	4.6	N/A	N/A
Sept 8, 95	2.6	1.8	N/A	N/A
Sept 15, 95	6	3	N/A	N/A
Sept 22, 95	72	59	N/A	N/A
Sept 29, 95	35	21	N/A	N/A
Oct 6, 95	188	146	N/A	N/A
Oct 13, 95	85	63	N/A	N/A
Oct 20, 95	22	5.6	N/A	N/A
Oct 27, 95	66	34	N/A	N/A
Nov 3, 95	31	21	N/A	N/A
Nov 10, 95	75	30	65	1500
Nov 17, 95	8	4	N/A	N/A
Nov 22, 95	25	15	N/A	N/A
Dec 1, 95	18	8.2	N/A	N/A
Dec 8, 95	27	14	N/A	N/A
Dec 15, 95	3.4	1.4	N/A	N/A
Dec 21, 95	131	53	N/A	N/A
Dec 29, 95	27	7.2	N/A	N/A
Jan 5, 96	1.8	0.8	N/A	N/A
Jan 12, 96	19	9.3	N/A	N/A
Jan 19, 96	17	8.4	N/A	N/A
Jan 26, 96	1	0.4	N/A	N/A

O & G: Total Oil and Grease
PHC: Petroleum Hydrocarbons
TSS: Total Suspended Solids

BATTERY INDUSTRY

Influent Stream

PARAMETERS (mg/L)	Time Period A
Chemical Oxygen Demand (COD)	1240
Total Suspended Solids (TSS)	62
HEAVY METALS (mg/L)	
Copper, Cu	1.3
Lead, Pb	32.0
Nickel, Ni	0.63
Silver, Ag	< 0.01
Zinc, Zn	4.0
Chromium (total), Cr	1.1
Cadmium, Cd	0.1
Arsenic, As	<0.3
OTHER SUBSTANCES (mg/L)	
Oil & Grease	< 10
Cyanide (total), CN	< 0.05
Dissolved Sulfides	< 0.02

Time Period A
Time Period B
Time Period C

Jul-Sep 1995
Apr-Jun 1996
Jan-Mar 1996

Effluent Stream

PARAMETERS (mg/L)	Time Period B	Time Period C
Flow Rate (GPD)	444	1260
Chemical Oxygen Demand (COD)	161	8.8
Total Suspended Solids (TSS)	25	5
HEAVY METALS (mg/L)		
Copper, Cu	0.1	< 0.01
Lead, Pb	0.15	< 0.05
Nickel, Ni	0.24	0.07
Silver, Ag	< 0.01	0.01
Zinc, Zn	0.15	0.07
Chromium (total), Cr	< 0.01	< 0.01
Cadmium, Cd	< 0.01	< 0.01
Arsenic, As	< 0.3	< 0.3
Mercury, Hg	< 0.005	< 0.005
OTHER SUBSTANCES (mg/L)		
Oil & Grease	< 10	< 10
Cyanide (total), CN	< 0.05	< 0.05
Dissolved Sulfides	0.07	0.03

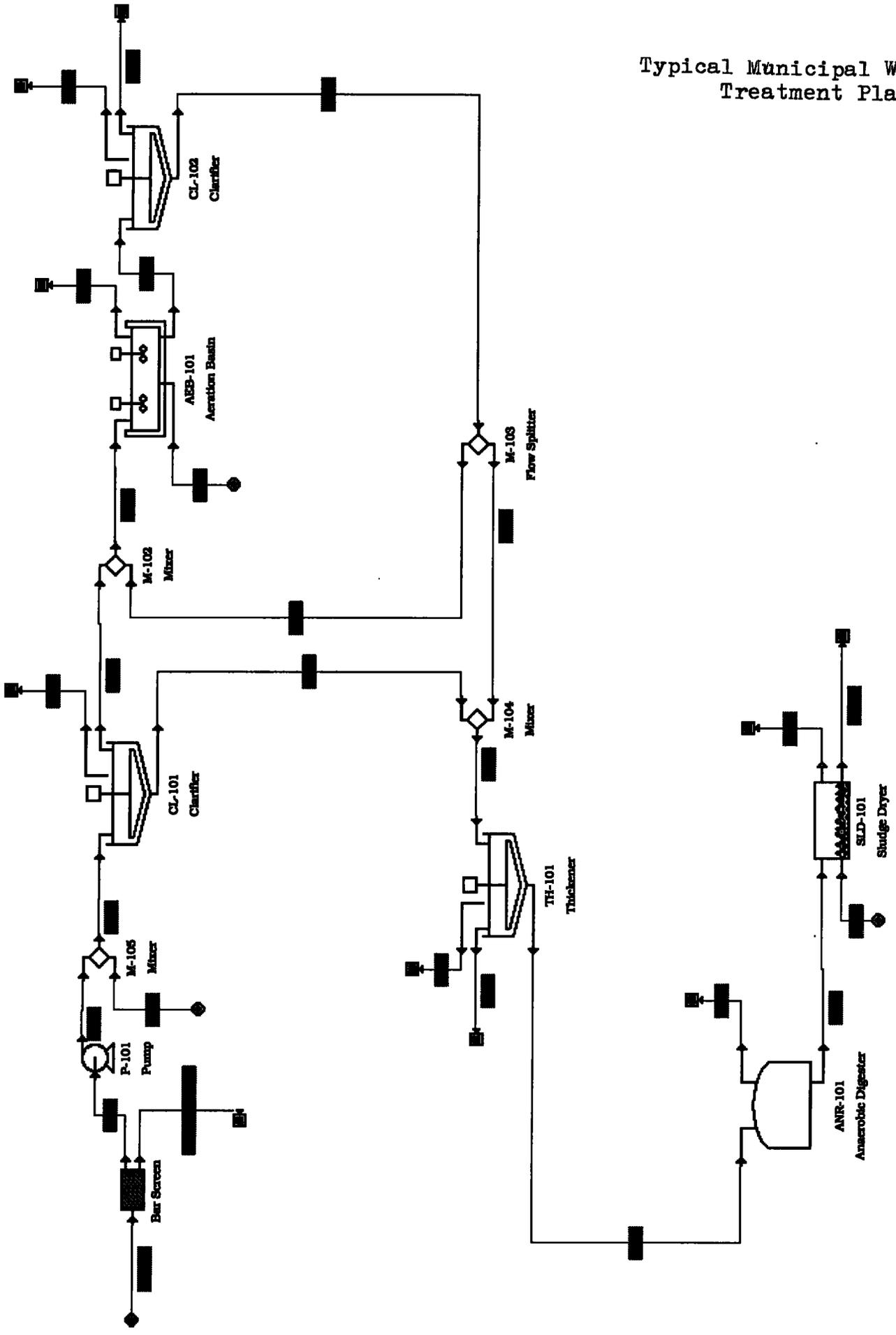
PARAMETERS	EXPOSURE LIMITS			HEALTH HAZARDS		TARGET ORGANS	SPECIFIC FLASH GRAVITY POINT (F)	
	NIOSH (mg/m3)	OSHA (mg/m3)	IDLH (mg/m3)	route	symptoms			
VOLATILE ORGANICS								
<i>1,2-dichloroethene, trans</i>	790	790	3950	In/Ig/Co	irritable eyes, respiratory system, CNS, depression	eyes, respiratory system, CNS	1.27	36-39
<i>chloroform</i>	9.78	240	2445	In/Ab/Ig/Co	irritable eyes, skin; dizziness, mental dullness, nausea, confusion, fatigue; anesthesia; headache; enlarged liver, carcinogenic	liver, kidneys, heart, eyes, skin, CNS; in animals, liver & kidney cancers	1.48	NA
<i>1,1,1-trichloroethane</i>	350 ppm	350 ppm/15 m		In/Ig/Co	irritating to the eyes, skin, mucous membranes, and upper respiratory tract; prolonged exposure can cause narcotic effect and dermatitis	skin, eyes, respiratory system; liver, kidneys	1.338	NA
<i>bromodichloromethane</i>				In/Ab/Co	causes eye and skin irritation; material is irritating to mucous membranes and upper respiratory tract; prolonged exposure can cause nausea, dizziness, headache, and narcotic effect; carcinogen	eye, skin, respiratory system	1.98	NA
<i>tetrachloroethene</i>	*minimum	689	1033.5	In/Ab/Ig/Co	irritable eyes, nose, throat; nausea; flush face, neck; vertigo, dizziness, incoordination, headache, somnolence; skin erythema (skin redness)	eyes, skin, respiratory system, liver kidneys, CNS; in animals: liver tumors	1.62	NA
<i>toluene</i>	375	750	1875	In/Ab/Ig/Co	irritable eyes, nose; fatigue, weakness, confusion, euphoria, dizziness, headache; dilated pupils, lacrimation, nervousness, muscle fatigue, insomnia; paresthesia; dermatitis; liver, kidney damage	eyes, skin, respiratory system, CNS, kidneys, liver	0.87	40
<i>m-xylene</i>	435	435	3915	In/Ab/Ig/Co	irritable eyes, skin, nose, throat; dizziness, excitement, drowsiness, incoordination, staggering gait, corneal vacuolization; anorexia, nausea, vomiting; abdominal pain, dermatitis	CNS, GI tract, blood, liver, kidneys	0.86	82
<i>o,p-xylenes</i>	435/435	435/435	3915/3915	In/Ab/Ig/Co	irritable eyes, skin, nose, throat; dizziness, excitement, drowsiness, incoordination, staggering gait, corneal vacuolization; anorexia, nausea, vomiting; abdominal pain, dermatitis	CNS, GI tract, blood, liver, kidneys	0.88/0.86	90/81

HEAVY METALS	EXPOSURE LIMITS			H E A L T H route	H A Z A R D S symptoms	TARGET ORGANS	SPECIFIC GRAVITY	FLASH POINT (F)
	NIOSH (mg/m3)	OSHA (mg/m3)	IDLH (mg/m3)					
<i>Cu, copper</i>	1	1	100	In/Ig/Co	irritable eyes, nose, pharynx; nasal perforation, metallic taste, dermatitis; in animals, lung, liver, kidney damage, anemia	eyes, skin, liver, kidneys, respiratory system, Wilson's disease	8.94	NA
<i>Cr, chromium</i>	0.5	1	250	In/Ig/Co	irritating eyes, skin; lung fibrosis (histologic)	eyes, skin, respiratory system	7.14	NA
<i>Ni, nickel</i>	0.015	1	10	In/Ig/Co	sensitization, dermatitis, allergic asthma, pneumitis, carcinogenic	nasal cavities, lungs, skin, lung & nasal cancers	8.9	NA
<i>Zn, zinc</i>				In/Ig	ingestion causes coughing, dyspnea, and sweating; a human skin irritant; inhalation may cause chills, throat dryness, cough, weakness, generalized aches, sweet taste, fever, nausea, vomiting	skin; causes "brass chills"	7.14	
<i>Pb, lead</i>	0.1	0.05	100	In/Ig/Co	weakness, lassitude, insomnia, facial pallor, pale eyes, anorexia, low-wgt, malnutrition, constipation, abdominal pain, colic, anemia, gingival lead line, tremor, paralysis of wrist, ankles; encephalopathy, kidney disease, irritable eyes, hypotension	eyes, GI tract, CNS, kidneys, blood, gingival tissue	11.34	NA
<i>Cd, cadmium</i>		0.005	9	In/Ig	pulmonary edema, dyspnea, cough, chest tightness, substernal pain, headache, chills, muscular aches, nausea, vomiting, diarrhea, anosmia, emphysema, proteinuria, mild anemia, carcinogenic	respiratory system, kidneys, prostate, blood, prostate & lung cancers	8.65	62
<i>Hg, mercury</i>	0.1 C	0.1 C	10	In/Ab/Ig/Co	irritable eyes, skin; coughing, chest pain, dyspnea, bronchitis, pneumitis, tremor, insomnia, irritability, headache, fatigue, weakness, stomatitis, salivation, GI disturbance, anorexia, low-wgt, proteinuria	eyes, skin, respiratory system, CNS, kidneys	13.6	NA
<i>As, arsenic</i>	0.002 SEL	0.01	5	In/Ab/Co/Ig	ulceration of nasal septum, respiratory irritation, peripheral neuropathy, hyperpigmentation of skin, dermatitis, gastrointestinal (GI) disturbances, carcinogenic	liver, kidneys, skin, lungs, lymphatic system, lung & lymphatic cancers	5.73	NA
<i>Be, beryllium</i>	0.0005	0.002	4	In/Co	berylliosis, anorexia, low-wgt, weakness, chest pain, coughing, clubbing of fingers, cyanosis, pulmonary insufficiency; irritable eyes; dermatitis, carcinogenic	eyes, skin, respiratory system, lung cancer	1.85	NA
<i>Ag, silver</i>	0.01	0.01	10	In/Ig/Co	blue-gray eyes, nasal septum, throat, skin; irritability, ulceration of skin, GI disturbances	nasal septum, skin, eyes	10.49	NA

PARAMETERS	EXPOSURE LIMITS			HEALTH HAZARDS		TARGET ORGAN	SPECIFIC GRAVITY	FLASH POINT (F)
	NIOSH (mg/m3)	OSHA (mg/m3)	IDLH (mg/m3)	route	symptoms			
ADDITIONAL COMPOUNDS								
<i>acetone</i>	590	2400	6050	In/Ig/Co	irritable eyes, nose, throat; headache, dizziness, CNS, depression; dermatitis	eyes, skin, respiratory system, CNS	0.79	0
<i>2-chlorotoluene</i>	250	none	N.D.	In/Ab/Ig/Co	irritable eyes, skin, mucous membrane; dermatitis; drowsiness, incoordination, anesthesia.; cough; liver, kidney injury	eyes, skin, respiratory system, CNS, liver, kidneys	1.08	96
<i>4-chlorotoluene</i>				In/Ig/Co	can be irritating to the eyes, skin, mucous membrane, and upper respiratory tract	eyes, skin, respiratory system	1.07	121
BASE NEUTRALS								
<i>bis-2-ethyl hexyl phthalate</i>	5	5	5000	In/Ig/Co	Irritable eyes, mucous membrane; in animals: liver damage; teratogenic effects; carcinogenic	eyes, respiratory system, CNS, liver, reproductive system, GI tract; in animals: liver, tumors	0.99	420 (oc)
<i>butyl benzyl phthalate</i>				In/Ig/Co	irritating to skin, eyes, mucous membranes, and upper respiratory tract	skin, eyes, respiratory system	1.106	230
<i>dibutyl phthalate</i>	5	5	4000	In/Ig/Co	irritable eyes, upper respiratory system, stomach	eyes, respiratory system, gastrointestinal (GI) tract	1.05	315
<i>diethyl phthalate</i>	5	none	N.D.	In/Ig/Co	irritable eyes, skin, nose, throat; headache, dizziness, nausea; lacrimation; possible polyneur, vestibular dysfunction; pain, numberness, weakness, spasms in arms & legs; in animals: reproductive effects	eyes, skin, respiratory system, CNS, peripheral nervous system, reproductive system	1.12	322 (oc)
<i>di-n-octyl-phthalate</i>	5	5	5000	In/Ig/Co	irritable eyes, mucous membrane; in animals: liver damage; teratogenic effects; carcinogenic	eyes, respiratory system, CNS, liver, reproductive system, GI tract; in animals: liver, tumors	0.99	420 (oc)
<i>naphthalene</i>	50	50	1332.5	In/Ab/Ig/Co	irritable eyes; headache, confusion, excitement, malaise; nausea, vomiting, abdominal pain; irritable bladder; profuse sweat; jaundice; hematuria, hemoglobinuria, renal shutdowns, dermatitis; optical neuritis, corneal damage	eyes, skin, blood, liver, kidneys, CNS	1.15	174
<i>phenol</i>	19	19	977.5	In/Ab/Ig/Co	irritable eyes, nose, throat; anorexia, low weight; weakness, muscular ache, pain; dark urine; cyanosis; liver, kidney damage; skin burns; dermatitis; ochronosis; tremor, convulsion, twitch	eyes, skin, respiratory system, liver, kidneys	1.06	175

	EXPOSURE LIMITS			H E A L T H route	H A Z A R D S symptoms	TARGET ORGANS	SPECIFIC GRAVITY	FLASH POINT (F)
	NIOSH (mg/m3)	OSHA (mg/m3)	IDLH (mg/m3)					
<i>Cu, copper</i>	1	1	100	In/Ig/Co	irritable eyes, nose, pharynx; nasal perforation, metallic taste, dermatitis; in animals, lung, liver, kidney damage, anemia	eyes, skin, liver, kidneys, respiratory system, Wilson's disease	8.94	NA
<i>Cr, chromium</i>	0.5	1	250	In/Ig/Co	irritating eyes, skin; lung fibrosis (histologic)	eyes, skin, respiratory system	7.14	NA
<i>As, arsenic</i>	0.002 SEL	0.01	5	In/Ab/Co/Ig	ulceration of nasal septum, respiratory irritation, peripheral neuropathy, hyperpigmentation of skin, dermatitis, gastrointestinal (GI) disturbances, carcinogenic	liver, kidneys, skin, lungs, lymphatic system, lung & lymphatic cancers	5.73	NA
<i>Benzene</i>	0.325	0.325	1625	In/Ab/Co/Ig	irritable eyes, skin, nose, respiratory system; giddiness; headache, nausea, staggered gait; fatigue, anorexia, lassitude; dermatitis; bone marrow depression, carcinogenic	eyes, skin, blood, CNS, respiratory system, bone marrow, leukemia	0.88	12
<i>Ethyl Benzene</i>	435	435	3528	In/Ig/Co	irritable eyes, skin, mucous membrane; headache; dermatitis; narcosis, coma	eyes, skin, respiratory system, CNS	0.87	55
<i>Toluene</i>	375	750	1875	In/Ab/Ig/Co	irritable eyes, nose; fatigue, weakness, confusion, euphoria, dizziness, headache; dilated pupils, lacrimation, nervousness, muscle fatigue, insomnia; paresthesia; dermatitis; liver, kidney damage	eyes, skin, respiratory system, CNS, kidneys, liver	0.87	40
<i>m-Xylene</i>	435	435	3915	In/Ab/Ig/Co	irritable eyes, skin, nose, throat; dizziness, excitement, drowsiness, incoordination, staggering gait, corneal vacuolization; anorexia, nausea, vomiting; abdominal pain, dermatitis	CNS, GI tract, blood, liver, kidneys	0.86	82
<i>o,p-Xylenes</i>	435/435	435/435	3915/3915	In/Ab/Ig/Co	irritable eyes, skin, nose, throat; dizziness, excitement, drowsiness, incoordination, staggering gait, corneal vacuolization; anorexia, nausea, vomiting; abdominal pain, dermatitis	CNS, GI tract, blood, liver, kidneys	0.88/0.86	90/81

Typical Municipal Wastewater Treatment Plant



STREAM REPORT

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STREAM NAME      Debris Remo      S-103      Influent      S-107      S-112
SOURCE           Bar Screen      Bar Screen      INPUT      CL-101      M-102
DESTINATION      OUTPUT          P-101      Bar Screen      M-102      AEB-101
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STREAM PROPERTIES

ACTIVITY	U/ml	0.0	0.0	0.0	0.0	0.0
TEMP	°C	20.0	20.0	20.0	20.0	20.0
PRES	bar	1.0	1.0	1.0	1.0	1.0
DENSITY	g/l	1075.2	1000.0	1000.0	1000.0	999.9

COMPONENT FLOWRATES (kg/h averaged)

Air	0.0000	0.0000	0.0000	0.0000	0.0000
Biomass	0.0000	107.5000	107.5000	80.6250	143.3832
BOD	0.0000	692.0000	692.0000	484.4000	913.4470
Carb. Dioxide	0.0000	0.0000	0.0000	0.0000	0.1162
Copper	0.0000	1.0000	1.0000	0.6000	1.0435
Dead Biomass	0.0000	0.0000	0.0000	0.0000	4.1010
Debris	285.0000	15.0000	300.0000	0.0000	0.0000
Lead	0.0000	0.5000	0.5000	0.3000	0.5217
Mercury	0.0000	0.1000	0.1000	0.0600	0.1043
Methane	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0000	0.0000	0.1162
Oxygen	0.0000	0.0000	0.0000	0.0000	0.2324
Suspended Solid	85.4000	768.6000	854.0000	384.3000	746.0750
Water	0.00004739223.00004739223.00004723993.82204972625.0758				

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==
TOTAL (kg/h)      370.40004740807.70004741178.10004724944.10704974434.2165
TOTAL (m3/h)      0.3445      4740.7998      4741.1443      4724.9394      4974.7635
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STREAM NAME      S-111      S-114      S-115      S-116      S-105
SOURCE           AEB-101      CL-102      CL-102      M-103      CL-101
DESTINATION      CL-102      OUTPUT      M-103      M-102      M-104
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STREAM PROPERTIES

ACTIVITY	U/ml	0.0	0.0	0.0	0.0	0.0
TEMP	°C	20.0	20.0	20.0	20.0	20.0
PRES	bar	1.0	1.0	1.0	1.0	1.0
DENSITY	g/l	999.9	1000.0	998.7	998.7	1000.2

COMPONENT FLOWRATES (kg/h averaged)

Air	0.0000	0.0000	0.0000	0.0000	0.0000
-----	--------	--------	--------	--------	--------

Biomass	139.4627	13.9463	125.5164	62.7582	26.8750
BOD	912.8659	54.7720	858.0939	429.0470	207.6000
Carb. Dioxide	0.2324	0.0000	0.2324	0.1162	0.0000
Copper	1.0435	0.1565	0.8870	0.4435	0.4000
Dead Biomass	8.2849	0.0828	8.2021	4.1010	0.0000
Debris	0.0000	0.0000	0.0000	0.0000	15.0000
Lead	0.5217	0.0783	0.4435	0.2217	0.2000
Mercury	0.1043	0.0157	0.0887	0.0443	0.0400
Methane	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.2324	0.0000	0.2324	0.1162	0.0000
Oxygen	0.4649	0.0000	0.4649	0.2324	0.0000
Suspended Solid	745.9279	22.3778	723.5500	361.7750	384.3000
Water	4972625.07584475362.5682	497262.5076	248631.2538	15229.1780	

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==
TOTAL (kg/h)      4974434.21654475453.9976 498980.2189 249490.1094 15863.5930
TOTAL (m3/h)      4975.1013  4475.4531  499.6482  249.8241  15.8604
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==
STREAM NAME      S-117      S-101      S-104      S-106      S-120
SOURCE           M-103      M-104      P-101      M-105      TH-101
DESTINATION      M-104      TH-101      M-105      CL-101      ANR-101
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STREAM PROPERTIES

ACTIVITY	U/ml	0.0	0.0	0.0	0.0	0.0
TEMP	°C	20.0	20.0	20.0	20.0	20.0
PRES	bar	1.0	1.0	6.7	1.0	1.0
DENSITY	g/l	998.7	998.8	1000.0	1000.0	999.0

COMPONENT FLOWRATES (kg/h averaged)

Air	0.0000	0.0000	0.0000	0.0000	0.0000
Biomass	62.7582	89.6332	107.5000	107.5000	85.1516
BOD	429.0470	636.6470	692.0000	692.0000	604.8146
Carb. Dioxide	0.1162	0.1162	0.0000	0.0000	0.0122
Copper	0.4435	0.8435	1.0000	1.0000	0.8435
Dead Biomass	4.1010	4.1010	0.0000	0.0000	4.1010
Debris	0.0000	15.0000	15.0000	15.0000	15.0000
Lead	0.2217	0.4217	0.5000	0.5000	0.4217
Mercury	0.0443	0.0843	0.1000	0.1000	0.0843
Methane	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.1162	0.1162	0.0000	0.0000	0.0122
Oxygen	0.2324	0.2324	0.0000	0.0000	0.0244
Suspended Solid	361.7750	746.0750	768.6000	768.6000	746.0750
Water	248631.2538	263860.43184739223.0000	4739223.0000	4739223.0000	27644.5526

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==
TOTAL (kg/h)      249490.1094 265353.70244740807.70004740807.7000 29101.0931
TOTAL (m3/h)      249.8241  265.6845  4740.7998  4740.7998  29.1298
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STREAM NAME           S-122           S-121           S-123           Sludge           S-125
SOURCE                ANR-101        ANR-101        INPUT           SLD-101        SLD-101
DESTINATION           OUTPUT         SLD-101        SLD-101        OUTPUT         OUTPUT
=====
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STREAM PROPERTIES

ACTIVITY	U/ml	0.0	0.0	0.0	0.0	0.0
TEMP	°C	30.0	30.0	25.0	60.0	115.0
PRES	bar	1.0	1.0	1.0	1.0	1.0
DENSITY	g/l	1.4	186.9	1.2	115.5	0.9

COMPONENT FLOWRATES (kg/h averaged)

Air	0.0000	0.0000	213022.5139	0.0000	213022.5139
Biomass	0.0000	40.9366	0.0000	40.9366	0.0000
BOD	0.0000	397.7820	0.0000	397.7820	0.0000
Carb. Dioxide	37.6932	37.6932	0.0000	37.6932	0.0000
Copper	0.0000	0.8435	0.0000	0.8435	0.0000
Dead Biomass	0.0000	8.5225	0.0000	8.5225	0.0000
Debris	0.0000	15.0000	0.0000	15.0000	0.0000
Lead	0.0000	0.4217	0.0000	0.4217	0.0000
Mercury	0.0000	0.0843	0.0000	0.0843	0.0000
Methane	7.5374	67.8369	0.0000	9.6357	58.2012
Nitrogen	0.0000	0.0122	0.0000	0.0017	0.0104
Oxygen	0.0122	0.0122	0.0000	0.0017	0.0104
Suspended Solid	0.0000	746.0750	0.0000	746.0750	0.0000
Water	0.0000	27740.6302	0.0000	3940.3307	23800.2995

```

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==
TOTAL (kg/h)         45.2428  29055.8503  213022.5139  5197.3287  236881.0355
TOTAL (m3/h)         33.0094   155.4964  179741.4867   44.9911  276190.2210
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=====
STREAM NAME           S-118
SOURCE                TH-101
DESTINATION           OUTPUT
=====

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STREAM PROPERTIES

ACTIVITY	U/ml	0.0
TEMP	°C	20.0
PRES	bar	1.0
DENSITY	g/l	998.7

COMPONENT FLOWRATES (kg/h averaged)

Air	0.0000
Biomass	4.4817
BOD	31.8323

Carb. Dioxide	0.1040
Copper	0.0000
Dead Biomass	0.0000
Debris	0.0000
Lead	0.0000
Mercury	0.0000
Methane	0.0000
Nitrogen	0.1040
Oxygen	0.2081
Suspended Solid	0.0000
Water	236215.8791

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=====
TOTAL (kg/h)      236252.6093
TOTAL (m3/h)      236.5546
=====
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OVERALL MATERIAL BALANCE (kg/h averaged)

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COMPONENT                IN                OUT                (OUT-IN)
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=
Air                      213022.513923    213022.513923    0.000000
Biomass                  107.500000       59.364492        -48.135508
BOD                      692.000000       484.386286       -207.613714
Carb. Dioxide           0.000000         75.490503        75.490503
Copper                   1.000000         1.000000         -0.000000
Dead Biomass             0.000000         8.605381         8.605381
Debris                   300.000000       300.000000       0.000000
Lead                     0.500000         0.500000        -0.000000
Mercury                  0.100000         0.100000         0.000000
Methane                  0.000000         75.374283        75.374283
Nitrogen                 0.000000         0.116220         0.116220
Oxygen                   0.000000         0.232439         0.232439
Suspended Solid         854.000000       853.852852       -0.147148
Water                    4739223.000000   4739319.077545   96.077545
=====
=
TOTAL                    4954200.613923   4954200.613923   -0.000000
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=
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TABLE 1
 SUMMARY OF WATER POLLUTION CONTROL OPERATIONS
 AVERAGE DAILY FLOW, M.G.D.
 FISCAL YEAR 1994

'93

'94

PLANT		Jul.	Aug.	Sep.	Oct.	Nov.	Dec.	Jan.	Feb.	Mar.	Apr.	May.	Jun.	YR. AVG
MANHATTAN:	WARDS ISLAND	285	290	278	257	251	279	278	280	297	264	263	268	274
	NORTH RIVER	189	189	197	186	190	185	182	182	194	158	163	165	182
BRONX:	HUNTS POINT	145	147	148	148	151	156	153	148	172	146	147	143	150
BROOKLYN:	26TH WARD	67	75	78	74	71	75	70	79	86	70	69	68	74
	CONEY ISLAND	103	104	109	108	100	105	106	103	113	106	106	103	106
	OWLS HEAD	127	131	142	135	125	131	133	130	137	122	126	127	131
	NEWTOWN CREEK	298	306	307	296	278	290	296	286	315	275	283	304	295
	RED HOOK	43	44	52	53	52	43	48	41	43	40	40	40	45
QUEENS:	JAMAICA	79	79	81	75	73	75	77	76	77	81	88	89	79
	TALLMAN ISLAND	57	58	61	62	58	60	61	57	63	57	56	55	59
	BOWERY BAY	124	127	133	125	114	121	129	127	134	119	119	117	124
	ROCKAWAY	22	22	22	21	22	24	23	24	25	23	24	24	23
STATEN ISLAND:	OAKWOOD BEACH	24	24	25	26	25	26	29	29	37	30	28	27	27
	PORT RICHMOND	34	36	40	39	38	40	41	43	53	44	42	42	41
TOTAL		1597	1632	1672	1606	1548	1611	1625	1605	1746	1535	1553	1573	1608

WARDS ISLAND
PROCESS EFFICIENCY SUMMARY
TABLE NO. 4

SPDES ID. NY0026131

FISCAL YEAR 1994

MONTH	<u>SUSPENDED SOLIDS</u>					<u>BIOCHEMICAL OXYGEN DEMAND</u>						
	<u>RAW</u>	<u>PRIMARY</u>	<u>REMOVAL</u>	<u>PLANT</u>	<u>REMOVAL</u>	<u>RAW SEWAGE</u>		<u>PRIMARY EFFLUENT</u>		<u>PLANT EFFLUENT</u>		
	<u>SEWAGE</u>	<u>EFFLUENT</u>	<u>%</u>	<u>EFFLUENT</u>	<u>%</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>TOTAL</u>	<u>REMOVAL</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>REMOVAL</u>
	<u>mg/L</u>	<u>mg/L</u>		<u>mg/L</u>		<u>mg/L</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>
JUL	81	67	17	10	88	64	21	46	28	7	6	89
AUG	82	60	27	9	89	77	28	51	34	9	8	88
SEP	84	59	30	8	90	81	33	49	40	9	8	89
OCT	88	65	26	7	92	90	40	57	37	8	10	91
NOV	93	72	23	8	91	90	48	60	33	9	11	90
DEC	83	79	5	12	86	76	29	50	34	7	6	91
JAN	87	87	0	12	86	91	35	70	23	11	8	88
FEB	84	91	0	12	86	89	44	71	20	13	10	85
MAR	85	86	0	13	85	89	41	73	18	14	13	84
APR	94	73	22	12	87	97	41	68	30	14	11	86
MAY	98	70	29	15	85	90	38	58	36	13	11	86
JUN	104	80	23	16	85	81	28	57	30	12	9	85
AVERAGE:	87	74	15	11	87	85	36	60	29	10	9	88

NOTE: Average as flow weighted.

Wards Island
Heavy Metals
Influent/Effluent (mg/L)
Fiscal Year 1994

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Be		Ag	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Ju1.	0.057	0.0230	0.0023	0.0012	0.0039	0.0026	0.053	0.025	0.0037	0.0012	0.00034	0.00020	0.00046	0.00010	0.00038	0.00029	0.00003	0.00003	0.00280	0.00048
Aug.	0.079	0.0370	0.0031	0.0013	0.0035	0.0026	0.078	0.034	0.0150	0.0052	0.00007	0.00003	0.00006	0.00006	0.00100	0.00110	0.00003	0.00003	0.00230	0.00083
Sep.	0.049	0.0190	0.0051	0.0009	0.0036	0.0030	0.055	0.020	0.0150	0.0019	0.00011	0.00003	0.00014	0.00006	0.00068	0.00054	0.00003	0.00003	0.00230	0.00041
Oct.	0.061	0.0130	0.0027	0.0005	0.0019	0.0018	0.063	0.022	0.0085	0.0012	0.00022	0.00010	0.00013	0.00006	0.00067	0.00068	0.00003	0.00003	0.00290	0.00040
Nov.	0.043	0.0086	0.0032	0.0014	0.0041	0.0032	0.058	0.018	0.0072	0.0052	0.00014	0.00003	0.00040	0.00010	0.00046	0.00038	0.00003	0.00003	0.00370	0.00044
Dec.	0.046	0.0190	0.0013	0.0038	0.0021	0.0009	0.058	0.022	0.0100	0.0035	0.00019	0.00003	0.00130	0.00009	0.00055	0.00039	0.00003	0.00003	0.00240	0.00042
Jan.	0.060	0.0300	0.0033	0.0011	0.0039	0.0020	0.065	0.032	0.0078	0.0017	0.00022	0.00003	0.00017	0.00018	0.00042	0.00027	0.00004	0.00003	0.00420	0.00051
Feb.	0.540	0.0130	0.0032	0.0015	0.0038	0.0038	0.062	0.023	0.0062	0.0012	0.00023	0.00003	0.00018	0.00013	0.00063	0.00045	0.00003	0.00003	0.00320	0.00051
Mar.	0.056	0.0130	0.0051	0.0017	0.0042	0.0030	0.080	0.057	0.0190	0.0026	0.00022	0.00008	0.00012	0.00011	0.00028	0.00010	0.00003	0.00003	0.00380	0.00063
Apr.	0.047	0.0097	0.0078	0.0019	0.0032	0.0015	0.056	0.023	0.0068	0.0012	0.00024	0.00005	0.00015	0.00008	0.00034	0.00027	0.00008	0.00008	0.00200	0.00045
May.	0.051	0.0093	0.0023	0.0012	0.0034	0.0073	0.059	0.020	0.0072	0.0011	0.00013	0.00005	0.00015	0.00006	0.00054	0.00052	0.00003	0.00003	0.00240	0.00080
Jun.	0.054	0.0350	0.0029	0.0015	0.0015	0.0019	0.041	0.016	0.0140	0.0026	0.00010	0.00003	0.00021	0.00006	0.00052	0.00043	0.00003	0.00006	0.00290	0.00100
AVG.	0.095	0.019	0.0035	0.0015	0.0033	0.0028	0.061	0.026	0.0100	0.0024	0.00018	0.00006	0.00029	0.00009	0.00054	0.00045	0.00004	0.00004	0.00291	0.00057

Wards Island
Heavy Metals
Sludge (mg/kg)
Fiscal Year 1994

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Be		V		Ag		SOL %
	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	
Jul.	36	1636	8.2	373	3.10	141	26	1182	7.2	327	0.260	11.8	0.064	3.0	0.0760	3.5	0.0068	0.310	1.30	59	1.40	64	2.2
Aug.	32	1600	5.4	270	1.80	90	22	1100	5.6	280	0.087	4.4	0.076	3.8	0.0560	2.8	0.0049	0.250	0.93	47	1.40	70	2.0
Sep.	27	1350	4.9	245	1.90	95	23	1150	6.5	325	0.150	7.5	0.061	3.0	0.0620	3.1	0.0053	0.270	0.93	47	1.40	70	2.0
Oct.	19	1056	1.6	89	0.66	37	19	1056	5.0	278	0.068	3.8	0.049	2.7	0.0670	3.7	0.0048	0.270	0.61	34	1.00	56	1.8
Nov.	21	1235	1.8	106	0.77	45	16	941	2.6	153	0.053	3.1	0.055	3.0	0.0650	3.8	0.0038	0.220	0.67	39	1.20	71	1.7
Dec.	19	905	2.2	105	0.62	30	18	857	6.4	305	0.076	3.6	0.053	2.5	0.0720	3.4	0.0063	0.300	1.00	48	1.20	57	2.1
Jan.	17	810	1.8	86	0.70	33	20	952	3.6	171	0.085	4.0	0.059	2.8	0.0700	3.3	0.0062	0.300	0.95	45	0.87	41	2.1
Feb.	20	952	1.9	90	0.62	30	19	905	4.8	229	0.099	4.7	0.063	3.0	0.0880	4.2	0.0061	0.290	1.10	52	1.20	57	2.1
Mar.	21	875	2.3	96	0.91	38	24	1000	5.4	225	0.140	5.8	0.077	3.2	0.0570	2.4	0.0044	0.180	1.40	58	1.40	58	2.4
Apr.	23	958	2.4	100	1.10	46	24	1000	7.1	296	0.140	5.8	0.097	4.0	0.0890	3.7	0.0084	0.350	1.10	46	1.40	58	2.4
May.	21	955	1.7	77	0.68	31	23	1045	6.3	286	0.084	3.8	0.095	4.3	0.0810	3.7	0.0074	0.340	0.82	37	1.40	64	2.2
Jun.	24	960	2.2	88	1.20	48	25	1000	6.1	244	0.092	3.7	0.100	4.0	0.0930	3.7	0.0070	0.280	1.20	48	1.40	56	2.5
AVG.	23	1108	3.0	144	1.17	55	22	1016	5.6	260	0.111	5.2	0.071	3.28	0.0730	3.4	0.0060	0.280	1.00	47	1.27	60	2.1

Wards Island
Nutrients (mg/L)
Fiscal Year 1994

DATE	NH3		ORG		TKN		NO3		NO2		PHOS.-TOTAL		PHOS.-ORTHO		CYANIDE	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	8.75	13.13	8.65	3.38	17.5	16.5	0.1505	0.2005	0.036	0.042	1.303	1.055	0.593	0.688	0.020	0.020
Aug.	9.51	11.63	12.20	8.23	21.7	19.9	0.1468	0.1990	0.046	0.100	2.043	1.421	0.728	0.990	0.020	0.020
Sep.	7.63	12.00	8.38	6.00	16.0	18.0	0.1493	0.1168	0.030	0.081	1.820	1.480	1.183	1.113	0.020	0.020
Oct.	11.11	13.59	10.25	5.93	21.3	19.5	0.1985	0.3190	0.072	0.099	2.081	1.436	1.383	1.167	0.020	0.020
Nov.	10.31	13.00	9.95	7.58	20.3	20.6	0.1043	0.1115	0.018	0.169	1.688	1.945	1.032	1.066	0.020	0.020
Dec.	13.10	11.94	9.55	7.33	22.6	19.3	0.0895	0.0715	0.058	0.061	1.863	1.250	0.999	1.032	0.020	0.020
Jan.	10.95	15.86	13.08	5.78	24.0	21.6	0.0820	0.1228	0.039	0.047	1.952	1.237	1.173	1.001	0.020	0.020
Feb.	9.68	13.58	10.40	7.95	20.1	21.5	0.1690	0.1548	0.036	0.038	1.985	1.498	1.294	1.014	0.020	0.020
Mar.	8.60	10.58	14.18	6.33	17.2	16.9	0.2160	0.1135	0.042	0.049	1.979	1.271	1.139	0.802	0.020	0.020
Apr.	8.54	10.69	11.48	4.83	20.0	15.5	0.2278	0.0730	0.054	0.068	2.125	1.127	1.040	0.926	0.020	0.020
May.	11.94	14.05	5.58	5.05	17.5	19.1	0.2893	0.1695	0.120	0.148	2.571	1.744	1.352	0.934	0.020	0.020
Jun.	11.28	11.19	8.43	8.80	19.7	20.0	0.1060	0.1550	0.053	0.143	1.841	1.469	1.138	1.062	0.020	0.020
AVG.	10.11	12.60	10.18	6.43	19.8	19.0	0.1607	0.1506	0.050	0.087	1.937	1.411	1.088	0.983	0.020	0.020

HUNTS POINT
 PROCESS EFFICIENCY SUMMARY
 TABLE NO. 4

SPDES ID. NY0026191

FISCAL YEAR 1994

MONTH	<u>S U S P E N D E D S O L I D S</u>					<u>B I O C H E M I C A L O X Y G E N D E M A N D</u>						
	<u>RAW</u>	<u>PRIMAY</u>		<u>PLANT</u>		<u>RAW SEWAGE</u>		<u>PRIMARY EFFLUENT</u>		<u>PLANT EFFLUENT</u>		
	<u>SEWAGE</u>	<u>EFFLUENT</u>	<u>REMOVAL</u>	<u>EFFLUENT</u>	<u>REMOVAL</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>TOTAL</u>	<u>REMOVAL</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>REMOVAL</u>
	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>
JUL	89	76	15	10	89	81	36	55	32	7	5	91
AUG	95	88	7	8	92	92	41	66	28	7	8	92
SEP	96	82	15	7	93	95	52	64	33	8	8	92
OCT	103	96	7	9	91	113	66	75	34	9	10	92
NOV	108	80	26	8	93	107	67	60	44	7	8	93
DEC	102	74	27	15	85	97	36	49	49	6	5	94
JAN	90	101	0	8	91	96	39	66	31	8	7	92
FEB	90	69	23	8	91	93	38	59	37	9	9	90
MAR	88	81	8	13	85	89	65	65	27	11	9	88
APR	99	80	19	9	91	101	61	69	32	8	7	92
MAY	101	77	24	11	89	104	41	61	41	9	7	91
JUN	104	86	17	7	93	95	34	71	25	7	6	93
AVERAGE:	97	83	14	10	90	97	49	63	35	8	8	92

NOTE: Average as flow weighted.

Hunts Point
Heavy Metals
Influent/Effluent (mg/L)
Fiscal Year 1994

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Be		Ag	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Ju1.	0.080	0.0150	0.0089	0.0008	0.0065	0.0036	0.072	0.022	0.0055	0.0007	0.00049	0.00018	0.00024	0.00006	0.00044	0.00027	0.00003	0.00003	0.00300	0.00028
Aug.	0.160	0.0290	0.0200	0.0028	0.0160	0.0029	0.180	0.043	0.0350	0.0030	0.00130	0.00160	0.00015	0.00006	0.00110	0.00052	0.00005	0.00003	0.00650	0.00088
Sep.	0.150	0.0100	0.0650	0.0031	0.0270	0.0055	0.190	0.010	0.0530	0.0012	0.00120	0.00004	0.00110	0.00006	0.00130	0.00040	0.00006	0.00003	0.01100	0.00018
Oct.	0.110	0.0099	0.0250	0.0035	0.0130	0.0097	0.180	0.022	0.0300	0.0012	0.00170	0.00014	0.00020	0.00006	0.00098	0.00069	0.00004	0.00003	0.00930	0.00023
Nov.	0.076	0.0081	0.0160	0.0006	0.0100	0.0045	0.098	0.019	0.0240	0.0040	0.00085	0.00005	0.00035	0.00006	0.00074	0.00058	0.00003	0.00003	0.00800	0.00040
Dec.	0.069	0.0095	0.2500	0.0034	0.0066	0.0042	0.095	0.032	0.0250	0.0041	0.00076	0.00011	0.00019	0.00009	0.00087	0.00069	0.00003	0.00003	0.00560	0.00044
Jan.	0.071	0.0100	0.0520	0.0140	0.0060	0.0055	0.100	0.046	0.0150	0.0020	0.00081	0.00017	0.00017	0.00007	0.00080	0.00063	0.00003	0.00003	0.00540	0.00018
Feb.	0.079	0.0100	0.0450	0.0018	0.0081	0.0050	0.110	0.032	0.0160	0.0008	0.00100	0.00017	0.00015	0.00006	0.00040	0.00036	0.00006	0.00003	0.00530	0.00033
Mar.	0.069	0.0190	0.0150	0.0058	0.0090	0.0053	0.120	0.045	0.0310	0.0056	0.00074	0.00015	0.00012	0.00008	0.00016	0.00005	0.00003	0.00003	0.00520	0.00018
Apr.	0.085	0.0077	0.0190	0.0015	0.0064	0.0082	0.110	0.025	0.0170	0.0012	0.00098	0.00022	0.00026	0.00009	0.00069	0.00045	0.00008	0.00008	0.00530	0.00018
May.	0.054	0.0120	0.0210	0.0016	0.0120	0.0077	0.072	0.035	0.0130	0.0014	0.00059	0.00018	0.00058	0.00006	0.00083	0.00061	0.00003	0.00003	0.00330	0.00100
Jun.	0.090	0.0045	0.0210	0.0011	0.0100	0.0053	0.110	0.036	0.0250	0.0008	0.00091	0.00014	0.00015	0.00008	0.00090	0.00068	0.00003	0.00003	0.00510	0.00036
AVG.	0.091	0.012	0.0465	0.0033	0.0109	0.0056	0.120	0.031	0.0241	0.0022	0.00094	0.00026	0.00031	0.00007	0.00077	0.00049	0.00004	0.00003	0.00608	0.00039

Hunts Point
 Heavy Metals
 Sludge (mg/kg)
 Fiscal Year 1994

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Be		V		Ag		SOL %
	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	
Jul.	34	1214	12.0	429	4.00	143	34	1214	9.2	329	0.440	16.0	0.057	2.0	0.1100	3.9	0.0110	0.400	2.30	82	1.50	54	2.8
Aug.	26	1529	7.9	465	2.20	129	25	1471	5.6	329	0.250	15.0	0.079	4.6	0.0590	3.5	0.0077	0.453	1.60	94	1.20	71	1.7
Sep.	30	1579	5.0	263	1.50	79	28	1474	7.2	379	0.310	16.0	0.062	3.3	0.0840	4.4	0.0074	0.390	1.50	79	1.50	79	1.9
Oct.	22	1048	5.0	238	2.00	95	27	1286	7.1	338	0.300	14.0	0.063	3.0	0.1000	4.8	0.0082	0.390	1.50	71	0.84	40	2.1
Nov.	24	1043	5.5	239	1.60	70	28	1217	5.1	222	0.320	14.0	0.061	2.7	0.1300	5.7	0.0078	0.340	1.40	61	1.80	78	2.3
Dec.	21	913	4.5	196	1.20	52	24	1043	5.4	235	0.250	11.0	0.061	2.7	0.0820	3.6	0.0068	0.300	1.30	57	1.50	65	2.3
Jan.	19	905	3.5	167	1.10	52	27	1286	4.8	229	0.260	12.0	0.063	3.0	0.0650	3.1	0.0062	0.300	1.00	48	0.95	45	2.1
Feb.	24	1043	4.7	204	1.30	57	29	1261	6.4	278	0.200	8.7	0.059	2.6	0.1000	4.3	0.0080	0.300	1.40	61	1.60	70	2.3
Mar.	20	909	4.4	200	1.30	59	27	1227	6.5	295	0.280	12.7	0.064	2.9	0.1100	5.0	0.0056	0.300	1.10	50	1.50	68	2.2
Apr.	25	1000	5.5	220	1.90	76	31	1240	7.7	308	0.320	13.0	0.064	2.6	0.1000	4.0	0.0110	0.440	1.90	76	1.80	72	2.5
May.	23	958	4.6	192	1.40	58	27	1125	7.6	317	0.360	15.0	0.070	2.9	0.0700	2.9	0.0100	0.420	1.20	50	1.70	71	2.4
Jun.	18	818	3.0	136	1.00	45	21	955	5.1	232	0.210	9.5	0.071	3.2	0.0930	4.2	0.0065	0.300	1.10	50	0.98	45	2.2
AVG.	24	1080	5.5	246	1.71	76	27	1233	6.5	291	0.292	13.1	0.065	2.96	0.0919	4.1	0.0080	0.361	1.44	65	1.41	63	2.2

Hunts Point
Nutrients (mg/L)
Fiscal Year 1994

DATE	NH3		ORG		TKN		NO3		NO2		PHOS.-TOTAL		PHOS.-ORTHO		CYANIDE	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	9.23	13.45	7.63	5.08	16.7	18.5	0.1168	1.1693	0.015	0.531	1.843	1.405	0.915	1.213	0.020	0.020
Aug.	11.50	13.82	7.35	10.25	18.8	24.1	0.1568	0.9245	0.031	0.483	4.882	2.081	1.402	1.638	0.020	0.020
Sep.	8.38	10.70	13.75	7.68	22.1	18.4	0.2965	2.1800	0.030	0.895	2.080	2.158	0.983	1.373	0.020	0.020
Oct.	11.95	9.55	10.38	7.73	22.3	17.3	0.1890	1.5700	0.055	0.199	2.215	1.763	1.356	1.528	0.020	0.020
Nov.	14.13	18.50	11.55	8.95	25.7	27.4	0.1593	0.6085	0.045	1.105	2.838	2.383	1.557	1.595	0.020	0.020
Dec.	10.59	9.61	8.80	4.53	19.4	14.1	0.4543	1.1655	0.077	0.665	1.701	1.393	0.918	1.132	0.020	0.020
Jan.	13.95	11.23	12.70	7.80	26.6	19.0	0.0860	4.2363	0.082	0.641	2.029	1.332	1.074	0.965	0.020	0.020
Feb.	12.78	16.38	9.13	9.23	21.9	25.6	0.3038	0.8500	0.102	0.160	1.871	1.473	1.373	1.198	0.020	0.020
Mar.	11.43	14.40	13.98	9.00	25.4	23.4	0.3310	0.5350	0.071	0.425	2.706	1.761	1.701	1.408	0.020	0.020
Apr.	13.54	15.31	8.85	3.95	22.4	19.3	0.3338	1.1820	0.052	0.716	2.101	1.791	1.118	1.774	0.020	0.020
May.	12.31	10.74	11.75	6.93	24.1	17.7	0.3083	2.1693	0.072	0.434	2.043	1.953	0.969	1.123	0.020	0.020
Jun.	14.80	11.25	10.30	9.50	25.1	20.8	0.1668	0.6845	0.088	0.239	3.103	1.394	1.194	1.313	0.020	0.020
AVG.	12.05	12.91	10.51	7.55	22.5	20.5	0.2418	1.4396	0.060	0.541	2.451	1.740	1.213	1.355	0.020	0.020

26TH WARD
PROCESS EFFICIENCY SUMMARY
TABLE NO. 4

SPDES ID. NY0026212

FISCAL YEAR 1994

MONTH	<u>S U S P E N D E D S O L I D S</u>					<u>B I O C H E M I C A L O X Y G E N D E M A N D</u>						
	<u>RAW</u>	<u>PRIMARY</u>		<u>PLANT</u>		<u>RAW SEWAGE</u>		<u>PRIMARY EFFLUENT</u>		<u>PLANT EFFLUENT</u>		
	<u>SEWAGE</u>	<u>EFFLUENT</u>	<u>REMOVAL</u>	<u>EFFLUENT</u>	<u>REMOVAL</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>TOTAL</u>	<u>REMOVAL</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>REMOVAL</u>
	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>
JUL	84	54	36	19	77	99	52	77	22	13	7	87
AUG	93	60	35	23	75	106	50	77	27	14	6	87
SEP	84	53	37	6	93	107	46	76	29	6	4	94
OCT	84	66	21	9	89	112	54	93	17	9	7	92
NOV	79	74	6	12	85	104	56	91	13	11	5	89
DEC	88	75	15	18	80	109	52	92	16	15	7	86
JAN	104	72	31	15	86	122	58	91	25	12	7	90
FEB	75	64	15	15	80	105	52	80	24	15	9	86
MAR	86	67	22	20	77	103	53	76	26	13	7	87
APR	83	68	18	24	71	115	70	92	20	14	8	88
MAY	94	69	27	22	77	115	57	99	14	17	9	85
JUN	99	62	37	11	89	118	61	76	36	9	5	92
AVERAGE:	88	65	26	16	82	110	55	85	22	12	7	89

NOTE:

26th Ward
Heavy Metals
Influent/Effluent (mg/L)
Fiscal Year 1994

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Ba		Ag	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Ju1.	0.140	0.0480	0.0030	0.0014	0.0043	0.0027	0.054	0.046	0.0110	0.0088	0.00037	0.00036	0.00012	0.00008	0.00041	0.00032	0.00003	0.00003	0.00049	0.00052
Aug.	0.084	0.0200	0.0180	0.0017	0.0021	0.0011	0.063	0.020	0.0100	0.0029	0.00015	0.00006	0.00006	0.00006	0.00044	0.00023	0.00003	0.00003	0.00280	0.00041
Sep.	0.029	0.0100	0.0036	0.0027	0.0047	0.0049	0.068	0.038	0.0180	0.0058	0.00003	0.00003	0.00018	0.00006	0.00058	0.00049	0.00003	0.00003	0.00140	0.00018
Oct.	0.025	0.0200	0.0020	0.0015	0.0023	0.0028	0.047	0.029	0.0160	0.0059	0.00026	0.00019	0.00006	0.00006	0.00087	0.00080	0.00003	0.00003	0.00056	0.00035
Nov.	0.033	0.0062	0.0250	0.0120	0.0040	0.0018	0.046	0.019	0.0075	0.0029	0.00016	0.00005	0.00007	0.00006	0.00041	0.00042	0.00003	0.00003	0.00150	0.00018
Dec.	0.030	0.0091	0.0036	0.0022	0.0044	0.0015	0.049	0.030	0.0089	0.0059	0.00014	0.00007	0.00006	0.00006	0.00076	0.00089	0.00005	0.00003	0.00074	0.00018
Jan.	0.050	0.0100	0.0031	0.0014	0.0048	0.0025	0.080	0.029	0.0140	0.0022	0.00074	0.00018	0.00006	0.00006	0.00040	0.00032	0.00003	0.00003	0.00130	0.00018
Feb.	0.032	0.0091	0.0031	0.0027	0.0026	0.0025	0.048	0.023	0.0061	0.0019	0.00003	0.00003	0.00015	0.00008	0.00041	0.00030	0.00003	0.00003	0.00110	0.00018
Mar.	0.051	0.0220	0.0100	0.0048	0.0045	0.0036	0.170	0.069	0.0520	0.0140	0.00160	0.00019	0.00011	0.00011	0.00007	0.00006	0.00004	0.00003	0.00046	0.00055
Apr.	0.054	0.0078	0.0051	0.0021	0.0033	0.0026	0.120	0.030	0.0220	0.0024	0.00270	0.00019	0.00011	0.00008	0.00054	0.00036	0.00008	0.00008	0.00280	0.00120
May.	0.059	0.0190	0.0030	0.0054	0.0026	0.0036	0.110	0.032	0.0078	0.0054	0.00064	0.00013	0.00006	0.00006	0.00026	0.00028	0.00003	0.00003	0.00250	0.00096
Jun.	0.053	0.0056	0.0022	0.0005	0.0046	0.0039	0.076	0.020	0.0130	0.0018	0.01100	0.00003	0.00006	0.00006	0.00071	0.00038	0.00003	0.00003	0.00420	0.00032
AVG.	0.053	0.016	0.0068	0.0032	0.0037	0.0028	0.078	0.032	0.0155	0.0050	0.00149	0.00013	0.00009	0.00007	0.00049	0.00040	0.00004	0.00003	0.00165	0.00043

26th Ward
 Heavy Metals
 Sludge (mg/kg)
 Fiscal Year 1994

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Ba		V		Ag		SOL %
	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	
Ju1.	15	789	4.8	253	1.60	84	22	1158	7.8	411	0.100	5.3	0.051	2.7	0.0840	4.4	0.0052	0.300	1.00	53	0.33	17	1.9
Aug.	13	929	6.4	457	2.20	157	17	1214	5.2	371	0.084	6.0	0.038	2.7	0.0560	4.0	0.0048	0.340	0.69	49	0.27	19	1.4
Sep.	15	750	2.8	140	0.87	44	31	1550	7.0	350	0.180	9.0	0.053	2.7	0.0750	3.8	0.0056	0.280	1.10	55	0.39	20	2.0
Oct.	11	611	1.7	94	0.77	43	18	1000	5.4	300	0.120	6.7	0.038	2.1	0.0870	4.8	0.0041	0.230	0.63	35	0.37	21	1.8
Nov.	13	722	1.8	100	0.59	33	20	1111	6.3	350	0.160	8.9	0.042	2.3	0.0930	5.2	0.0047	0.260	0.65	36	0.42	23	1.8
Dec.	11	550	1.7	85	0.72	36	17	850	4.8	240	0.120	6.0	0.042	2.1	0.0870	4.4	0.0065	0.330	0.85	43	0.33	17	2.0
Jan.	10	526	1.6	84	0.61	32	16	842	3.0	158	0.091	4.8	0.042	2.2	0.0690	3.6	0.0048	0.250	0.86	45	0.29	15	1.9
Feb.	11	550	2.1	105	0.62	31	17	850	5.7	285	0.120	6.0	0.034	1.7	0.1000	5.0	0.0054	0.300	0.92	46	0.29	14	2.0
Mar.	12	522	2.6	113	0.78	34	20	870	6.7	291	0.110	4.8	0.047	2.0	0.1100	4.8	0.0039	0.170	1.50	65	0.50	22	2.3
Apr.	14	667	3.2	152	0.79	38	20	952	7.3	348	0.150	7.1	0.038	1.8	0.1200	5.7	0.0092	0.440	1.30	62	0.45	21	2.1
May.	13	591	3.4	155	1.00	45	21	955	7.9	359	0.220	10.0	0.044	2.0	0.0740	3.4	0.0084	0.380	1.10	50	0.54	25	2.2
Jun.	14	583	2.9	121	0.71	30	23	958	6.9	288	0.120	5.0	0.054	2.3	0.1200	5.0	0.0069	0.290	1.20	50	0.55	23	2.4
AVG.	13	649	2.9	155	0.94	51	20	1026	6.2	313	0.131	6.6	0.044	2.22	0.0896	4.5	0.0058	0.298	0.98	49	0.39	20	2.0

26th Ward
 Nutrients (mg/L)
 Fiscal Year 1994

DATE	NH3		ORG		TKN		NO3		NO2		PHOS.-TOTAL		PHOS.-ORTHO		CYANIDE	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	8.26	10.35	10.03	6.15	18.3	16.5	0.2675	0.2650	0.047	0.267	1.669	1.414	0.597	0.689	0.020	0.020
Aug.	7.59	6.98	6.43	5.53	14.0	12.5	0.3200	0.7575	0.052	0.568	2.030	1.813	0.533	0.736	0.020	0.020
Sep.	8.33	13.00	7.70	7.13	16.0	20.1	0.5800	0.9925	0.097	1.046	1.980	1.578	0.905	1.137	0.020	0.020
Oct.	9.00	11.60	9.75	7.90	18.8	19.5	0.4050	0.7575	0.076	0.668	2.235	1.405	1.315	0.959	0.020	0.020
Nov.	7.98	12.02	10.28	6.00	18.3	18.0	0.3768	0.7475	0.061	0.622	2.275	1.420	1.088	1.093	0.020	0.020
Dec.	7.69	12.06	13.35	8.57	21.0	18.0	0.2475	0.5900	0.094	0.293	2.320	1.740	1.013	0.750	0.020	0.020
Jan.	10.34	12.76	10.68	7.00	21.0	19.8	0.3750	0.3100	0.071	0.162	2.793	1.213	1.093	0.820	0.020	0.020
Feb.	8.69	9.31	9.58	8.45	18.3	17.8	0.3175	0.3150	0.165	0.236	1.928	0.863	0.880	0.563	0.020	0.020
Mar.	7.73	13.30	13.53	13.45	21.3	26.8	0.4975	0.7000	0.144	0.209	2.545	1.640	1.138	0.723	0.020	0.020
Apr.	8.10	13.48	11.43	8.53	19.5	22.0	0.3500	0.2025	0.070	0.267	2.618	1.825	0.935	1.503	0.020	0.020
May.	8.18	16.93	12.08	10.58	20.3	27.5	0.3375	0.1575	0.037	0.048	2.415	1.603	1.078	0.943	0.020	0.020
Jun.	7.63	15.10	17.40	9.90	25.0	25.0	0.1675	0.2625	0.071	0.495	2.513	1.298	1.043	0.975	0.020	0.020
AVG.	8.29	12.24	11.02	8.26	19.3	20.3	0.3535	0.5048	0.082	0.407	2.277	1.484	0.968	0.907	0.020	0.020

TALLMAN ISLAND
PROCESS EFFICIENCY SUMMARY
TABLE NO. 4

SPDES ID. NY0026239

FISCAL YEAR 1994

MONTH	<u>SUSPENDED SOLIDS</u>					<u>BIOCHEMICAL OXYGEN DEMAND</u>						
	<u>RAW</u>	<u>PRIMARY</u>	<u>REMOVAL</u>	<u>PLANT</u>	<u>REMOVAL</u>	<u>RAW SEWAGE</u>		<u>PRIMARY EFFLUENT</u>		<u>PLANT EFFLUENT</u>		
	<u>SEWAGE</u>	<u>EFFLUENT</u>	<u>%</u>	<u>EFFLUENT</u>	<u>%</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>TOTAL</u>	<u>REMOVAL</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>REMOVAL</u>
	<u>mg/L</u>	<u>mg/L</u>		<u>mg/L</u>		<u>mg/L</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>
JUL	98	59	40	4	96	113	64	62	45	4	3	96
AUG	92	57	38	5	95	104	60	56	46	3	3	97
SEP	93	45	52	4	96	102	61	49	52	3	3	97
OCT	99	50	49	8	92	110	61	59	46	5	4	95
NOV	99	56	43	6	94	121	65	66	45	5	5	96
DEC	98	54	45	8	92	126	65	64	49	5	3	96
JAN	98	58	41	9	91	113	59	67	41	8	4	93
FEB	86	62	28	6	93	114	64	75	34	7	5	94
MAR	88	60	32	8	91	104	63	64	38	7	4	93
APR	95	60	37	6	94	113	68	66	42	6	4	95
MAY	102	63	39	5	95	127	72	78	39	5	3	96
JUN	108	59	45	6	94	132	69	66	50	4	3	97
AVERAGE:	95	56	41	6	94	113	64	64	43	5	4	96

NOTE: Average as flow weighted.

Tallman Island
Heavy Metals
Influent/Effluent (mg/L)
Fiscal Year 1994

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Be		Ag	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	0.130	0.0120	0.0120	0.0017	0.0260	0.0100	0.110	0.039	0.0190	0.0009	0.00080	0.00036	0.00024	0.00006	0.00046	0.00017	0.00003	0.00003	0.00670	0.00043
Aug.	0.150	0.0280	0.0096	0.0022	0.0100	0.0060	0.093	0.039	0.0130	0.0015	0.00210	0.00180	0.00013	0.00006	0.00032	0.00018	0.00003	0.00003	0.01400	0.00039
Sep.	0.093	0.0090	0.0087	0.0024	0.0150	0.0068	0.120	0.055	0.0190	0.0008	0.00065	0.00021	0.00017	0.00006	0.00058	0.00034	0.00003	0.00003	0.00920	0.00030
Oct.	0.050	0.0130	0.0220	0.0013	0.0078	0.0020	0.070	0.025	0.0068	0.0008	0.00130	0.00063	0.00008	0.00006	0.00066	0.00056	0.00003	0.00003	0.01200	0.00033
Nov.	0.067	0.0090	0.0060	0.0020	0.0092	0.0087	0.120	0.040	0.0170	0.0020	0.00220	0.00160	0.00021	0.00006	0.00085	0.00050	0.00003	0.00003	0.00460	0.00068
Dec.	0.047	0.0096	0.0087	0.0029	0.0084	0.0094	0.073	0.033	0.0089	0.0014	0.00320	0.00046	0.00013	0.00006	0.00062	0.00036	0.00003	0.00003	0.00800	0.00050
Jan.	0.041	0.0140	0.0120	0.0020	0.0340	0.0120	0.120	0.052	0.0100	0.0019	0.00180	0.00062	0.00015	0.00012	0.00044	0.00033	0.00003	0.00003	0.00480	0.00053
Feb.	0.049	0.0130	0.0067	0.0027	0.0085	0.0082	0.093	0.039	0.0092	0.0004	0.00049	0.00025	0.00023	0.00006	0.00039	0.00028	0.00003	0.00003	0.00600	0.00840
Mar.	0.044	0.0140	0.0100	0.0036	0.0031	0.0040	0.100	0.045	0.0091	0.0039	0.00034	0.00014	0.00014	0.00009	0.00050	0.00050	0.00003	0.00003	0.00560	0.00088
Apr.	0.056	0.0110	0.0092	0.0023	0.0030	0.0030	0.120	0.027	0.0140	0.0008	0.00021	0.00003	0.00020	0.00006	0.00045	0.00030	0.00008	0.00008	0.00580	0.00071
May.	0.052	0.0120	0.0110	0.0064	0.0170	0.0110	0.100	0.028	0.0076	0.0007	0.00088	0.00012	0.00006	0.00006	0.00051	0.00025	0.00003	0.00003	0.00530	0.00120
Jun.	0.054	0.0480	0.0080	0.0018	0.0210	0.0180	0.092	0.036	0.0076	0.0012	0.00039	0.00013	0.00009	0.00006	0.00053	0.00044	0.00003	0.00003	0.00760	0.00100
AVG.	0.069	0.016	0.0103	0.0026	0.0136	0.0083	0.101	0.038	0.0118	0.0014	0.00120	0.00053	0.00015	0.00007	0.00053	0.00035	0.00003	0.00003	0.00747	0.00128

Tallman Island
 Heavy Metals
 Sludge (mg/kg)
 Fiscal Year 1994

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Be		V		Ag		SOL %
	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	
Jul.	14	933	6.6	440	4.00	267	18	1200	4.2	280	0.260	17.0	0.027	1.8	0.0570	3.8	0.0043	0.300	0.85	57	1.60	107	1.5
Aug.	9	573	6.7	447	2.50	167	17	1133	4.6	307	0.087	5.8	0.077	5.1	0.0560	3.7	0.0040	0.270	0.65	43	0.28	19	1.5
Sep.	16	1143	3.0	214	1.30	93	15	1071	4.0	286	0.280	20.0	0.065	4.6	0.0590	4.2	0.0057	0.410	0.72	51	1.00	71	1.4
Oct.	11	917	2.3	192	0.94	78	12	1000	2.8	233	0.210	18.0	0.045	3.8	0.0590	4.9	0.0043	0.360	0.52	43	0.80	67	1.2
Nov.	10	769	2.4	185	1.00	77	12	923	2.8	215	0.370	28.0	0.044	3.4	0.0560	4.3	0.0040	0.310	0.41	32	1.10	85	1.3
Dec.	9	708	1.6	133	0.67	56	11	917	2.3	192	0.350	29.0	0.041	3.4	0.0460	3.8	0.0037	0.310	0.33	28	0.88	73	1.2
Jan.	11	733	1.8	120	0.82	55	15	1000	3.1	207	0.240	16.0	0.049	3.3	0.0610	4.1	0.0043	0.290	0.49	33	1.10	73	1.5
Feb.	11	917	2.5	208	1.00	83	19	1583	4.0	333	0.170	14.0	0.048	4.0	0.0660	5.5	0.0053	0.440	0.84	70	1.10	71	1.2
Mar.	11	647	2.3	135	0.92	54	17	1000	3.6	212	0.170	10.0	0.044	2.6	0.0530	3.1	0.0590	3.500	0.89	52	1.20	71	1.7
Apr.	13	684	2.8	147	0.92	48	20	1053	4.5	237	0.130	6.8	0.052	2.7	0.1200	6.3	0.0084	0.440	0.97	51	1.30	68	1.9
May.	12	667	3.1	172	0.98	54	20	1111	4.7	261	0.180	10.0	0.047	2.6	0.0580	3.2	0.0062	0.340	1.40	78	1.10	61	1.8
Jun.	12	600	2.9	145	0.87	44	19	950	3.8	190	0.160	8.0	0.072	3.6	0.1000	5.0	0.0077	0.390	1.20	60	1.50	75	2.0
AVG.	12	774	3.2	212	1.33	90	16	1078	3.7	246	0.217	15.2	0.051	3.41	0.0659	4.3	0.0097	0.613	0.77	50	1.08	72	1.5

Tallman Island
Nutrients (mg/L)
Fiscal Year 1994

DATE	NH3		ORG		TKN		NO3		NO2		PHOS.-TOTAL		PHOS.-ORTHO		CYANIDE	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	14.65	4.68	10.28	3.33	25.0	8.0	0.2883	2.6400	0.015	1.015	2.445	1.178	1.265	1.048	0.020	0.020
Aug.	12.92	3.60	11.86	5.88	24.6	9.5	0.1190	5.2678	0.046	0.245	2.774	1.816	1.448	1.466	0.020	0.020
Sep.	13.00	5.63	11.08	3.63	24.1	9.3	0.0818	4.1150	0.024	0.182	2.705	1.833	1.643	1.590	0.020	0.020
Oct.	13.35	6.10	14.65	4.65	28.0	10.8	0.0833	3.8200	0.030	0.307	2.875	1.723	1.633	1.438	0.020	0.020
Nov.	15.13	9.10	9.63	4.40	24.8	13.5	0.0503	5.1775	0.026	0.680	3.273	2.545	1.918	1.898	0.020	0.020
Dec.	12.88	7.20	14.73	4.88	27.6	12.1	0.1153	3.8175	0.048	0.752	2.780	1.870	1.590	1.470	0.020	0.020
Jan.	13.33	10.28	8.93	4.48	22.3	14.8	0.2168	2.7650	0.062	0.596	2.710	1.680	1.715	0.997	0.030	0.020
Feb.	14.18	10.50	12.93	4.78	27.1	15.3	0.2210	2.5200	0.095	0.934	2.945	1.700	1.348	0.973	0.020	0.020
Mar.	11.18	6.26	19.43	4.88	30.6	11.1	0.5605	2.5325	0.069	0.722	2.850	1.398	1.460	1.008	0.020	0.020
Apr.	14.03	5.15	9.73	4.35	23.8	9.5	0.4850	3.6175	0.095	0.462	3.160	1.625	1.690	1.123	0.020	0.020
May.	15.93	5.96	12.15	2.13	28.1	8.1	0.5750	3.0425	0.100	0.585	3.035	1.508	1.793	1.213	0.020	0.020
Jun.	13.73	9.03	10.48	3.55	24.2	12.6	0.3475	3.9900	0.035	0.437	2.623	1.480	1.603	1.320	0.020	0.020
AVG.	13.69	6.96	12.15	4.24	25.8	11.2	0.2620	3.6088	0.054	0.576	2.848	1.696	1.592	1.295	0.021	0.020

OAKWOOD BEACH
 PROCESS EFFICIENCY SUMMARY
 TABLE NO. 4

SPDES ID. NY0026174

FISCAL YEAR 1994

MONTH	SUSPENDED SOLIDS					BIOCHEMICAL OXYGEN DEMAND						
	RAW SEWAGE	PRIMARY EFFLUENT	REMOVAL	PLANT EFFLUENT	REMOVAL	RAW SEWAGE		PRIMARY EFFLUENT		PLANT EFFLUENT		
	mg/L	mg/L	%	mg/L	%	TOTAL mg/L	FILTRATE mg/L	TOTAL mg/L	REMOVAL %	TOTAL mg/L	FILTRATE mg/L	REMOVAL %
JUL	151	66	56	6	96	107	27	50	53	6	3	94
AUG	144	73	49	4	97	118	29	55	53	4	3	97
SEP	136	70	49	7	95	114	27	44	61	6	4	95
OCT	126	60	52	5	96	110	24	44	60	5	3	95
NOV	153	73	52	5	97	117	26	56	52	4	2	97
DEC	118	69	42	9	92	96	32	74	23	8	4	92
JAN	99	54	45	5	95	98	27	55	44	6	3	94
FEB	101	57	44	10	90	86	29	50	42	10	3	88
MAR	99	44	56	10	90	80	24	43	46	15	7	81
APR	125	55	56	9	93	114	32	52	54	12	7	89
MAY	172	86	50	14	92	144	34	64	56	14	7	90
JUN	176	75	57	8	95	156	38	71	54	12	6	92
AVERAGE:	132	65	51	6	95	108	27	54	50	6	3	94

NOTE: Average as flow weighted.

Oakwood Beach
Heavy Metals
Influent/Effluent (mg/L)
Fiscal Year 1994

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Be		Ag	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Ju1.	0.140	0.0120	0.0047	0.0014	0.0120	0.0059	0.170	0.036	0.0140	0.0026	0.00075	0.00029	0.00030	0.00008	0.00076	0.00020	0.00005	0.00003	0.00560	0.00032
Aug.	0.095	0.0210	0.0270	0.0011	0.0100	0.0061	0.084	0.021	0.0120	0.0012	0.00014	0.00003	0.00014	0.00006	0.00066	0.00043	0.00003	0.00003	0.00590	0.00020
Sep.	0.052	0.0050	0.0030	0.0006	0.0120	0.0055	0.085	0.027	0.0075	0.0004	0.00030	0.00005	0.00015	0.00006	0.00075	0.00044	0.00004	0.00005	0.00570	0.00026
Oct.	0.052	0.0094	0.0019	0.0007	0.0078	0.0057	0.071	0.018	0.0094	0.0010	0.00028	0.00004	0.00006	0.00006	0.00081	0.00067	0.00003	0.00003	0.00900	0.00067
Nov.	0.037	0.0089	0.0022	0.0007	0.0130	0.0091	0.066	0.019	0.0099	0.0022	0.00160	0.00003	0.00022	0.00006	0.00076	0.00048	0.00003	0.00003	0.00510	0.00031
Dec.	0.047	0.0056	0.0027	0.0004	0.0200	0.0090	0.074	0.028	0.0063	0.0036	0.00020	0.00004	0.00100	0.00006	0.00081	0.00059	0.00003	0.00003	0.00930	0.00030
Jan.	0.034	0.0098	0.0031	0.0013	0.0140	0.0110	0.052	0.030	0.0047	0.0005	0.00061	0.00040	0.00008	0.00006	0.00058	0.00030	0.00003	0.00003	0.00430	0.00032
Feb.	0.032	0.0082	0.0110	0.0110	0.0160	0.0110	0.057	0.040	0.0038	0.0007	0.00025	0.00011	0.00008	0.00006	0.00063	0.00050	0.00003	0.00003	0.00390	0.00045
Mar.	0.033	0.0038	0.0024	0.0008	0.0220	0.0160	0.081	0.024	0.0092	0.0004	0.00016	0.00030	0.00013	0.00012	0.00090	0.00058	0.00003	0.00003	0.00300	0.00026
Apr.	0.039	0.0082	0.0042	0.0008	0.0076	0.0059	0.076	0.051	0.0066	0.0005	0.00040	0.00026	0.00016	0.00008	0.00042	0.00042	0.00008	0.00008	0.00270	0.00018
May.	0.043	0.0097	0.0073	0.0012	0.0690	0.0098	0.084	0.021	0.0076	0.0008	0.00040	0.00010	0.00006	0.00006	0.00049	0.00026	0.00003	0.00003	0.00480	0.00110
Jun.	0.110	0.0240	0.0061	0.0006	0.0220	0.0100	0.150	0.018	0.0230	0.0004	0.00038	0.00006	0.00019	0.00006	0.00110	0.00048	0.00003	0.00003	0.01800	0.00039
AVG.	0.060	0.010	0.0063	0.0017	0.0188	0.0088	0.088	0.028	0.0095	0.0012	0.00046	0.00014	0.00021	0.00007	0.00072	0.00045	0.00004	0.00004	0.00644	0.00040

Oakwood Beach
Heavy Metals
Sludge (mg/kg)
Fiscal Year 1994

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Be		V		Ag		SOL %
	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	
Jul.	9	775	1.7	142	1.30	108	10	817	1.5	125	0.024	2.0	0.079	6.6	0.0420	3.5	0.0021	0.200	0.11	9	0.64	53	1.2
Aug.	14	933	2.5	167	0.85	57	11	733	2.6	173	0.044	2.9	0.032	2.1	0.0560	3.7	0.0034	0.230	0.27	18	0.78	52	1.5
Sep.	7	600	1.0	90	0.96	87	8	727	1.5	136	0.110	10.0	0.036	3.3	0.0330	3.0	0.0022	0.200	0.30	27	0.52	47	1.1
Oct.	6	527	0.4	37	1.00	91	8	691	1.0	90	0.150	13.6	0.031	2.8	0.0410	3.7	0.0023	0.210	0.13	12	0.65	59	1.1
Nov.	6	545	0.6	57	0.79	72	8	736	1.2	109	0.027	2.5	0.044	4.0	0.0490	4.5	0.0022	0.200	0.33	30	0.71	65	1.1
Dec.	10	588	1.7	100	0.89	52	12	706	3.1	182	0.055	3.2	0.130	7.6	0.0630	3.7	0.0043	0.250	0.19	11	0.89	52	1.7
Jan.	9	538	1.0	63	0.89	56	15	938	2.0	125	0.066	4.1	0.100	6.3	0.0770	4.8	0.0044	0.280	0.17	11	0.62	39	1.6
Feb.	13	765	1.4	82	1.40	82	22	1294	4.6	271	0.130	7.6	0.063	3.7	0.1100	6.5	0.0068	0.400	0.41	24	0.85	50	1.7
Mar.	9	425	1.1	55	0.79	40	15	750	3.5	175	0.067	3.4	0.075	3.8	0.1000	5.0	0.0041	0.210	0.53	27	0.80	40	2.0
Apr.	10	485	1.1	55	1.70	85	15	750	3.3	165	0.075	3.8	0.064	3.2	0.1300	6.5	0.0085	0.430	0.36	18	0.78	39	2.0
May.	9	524	0.9	55	12.00	71	13	765	2.6	153	0.490	2.9	0.037	2.2	0.0780	4.6	0.0062	0.360	0.34	20	0.78	46	1.7
Jun.	11	524	1.2	57	1.30	62	15	714	3.2	152	0.063	3.0	0.074	3.5	0.1100	5.2	0.0069	0.330	0.31	15	0.93	44	2.1
AVG.	9	602	1.2	80	1.99	72	13	802	2.5	155	0.108	4.9	0.064	4.09	0.0741	4.6	0.0045	0.275	0.29	19	0.75	49	1.6

Oakwood Beach
Nutrients (mg/L)
Fiscal Year 1994

DATE	NH3		ORG		TKN		NO3		NO2		PHOS.-TOTAL		PHOS.-ORTHO		CYANIDE	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	18.18	3.85	13.20	3.90	31.4	7.8	0.0683	2.6815	0.027	0.375	5.130	2.600	2.448	2.088	0.020	0.020
Aug.	17.96	4.93	14.73	2.83	32.7	7.8	0.1968	2.5775	0.131	0.348	5.013	2.547	2.611	2.024	0.020	0.020
Sep.	17.55	4.41	12.08	1.83	29.6	6.3	0.0933	2.8808	0.034	0.291	4.627	2.550	2.653	2.273	0.020	0.020
Oct.	15.96	2.87	13.53	1.63	29.5	4.5	0.1128	2.3440	0.070	0.434	4.702	2.464	2.489	1.929	0.020	0.020
Nov.	11.83	3.26	17.90	1.65	29.7	4.9	0.7255	2.2345	0.078	0.724	5.022	2.231	2.585	2.030	0.020	0.020
Dec.	14.74	7.19	18.50	3.98	33.2	11.2	0.0753	1.2983	0.050	0.666	4.024	2.091	1.818	1.718	0.020	0.020
Jan.	13.61	3.69	10.20	2.70	23.8	6.4	0.0803	1.1020	0.139	1.086	3.496	1.542	1.581	1.307	0.020	0.020
Feb.	11.48	2.03	10.50	3.70	22.0	5.8	0.5238	1.9313	0.220	0.503	3.313	1.578	1.431	0.879	0.020	0.020
Mar.	10.15	3.38	11.50	7.63	21.6	11.0	1.0195	3.0360	0.305	0.410	3.648	1.710	1.448	0.623	0.020	0.020
Apr.	11.64	5.20	15.85	7.43	27.5	12.6	0.3825	2.9223	0.393	0.303	3.975	2.875	1.823	1.415	0.020	0.020
May.	16.98	6.34	18.80	5.43	35.8	11.8	0.6625	2.7355	0.112	0.302	6.466	2.746	2.317	1.483	0.020	0.020
Jun.	14.99	10.14	15.17	3.13	30.1	13.3	0.2450	2.0500	0.051	0.313	5.973	2.465	2.428	2.143	0.020	0.020
AVG.	14.59	4.77	14.33	3.82	28.9	8.6	0.3488	2.3161	0.134	0.479	4.615	2.283	2.136	1.659	0.020	0.020

TABLE 1
SUMMARY OF WATER POLLUTION CONTROL OPERATIONS
AVERAGE DAILY FLOW, M.G.D.
FISCAL YEAR 1995

PLANT		'94 '95												
		Jul.	Aug.	Sep.	Oct.	Nov.	Dec.	Jan.	Feb.	Mar.	Apr.	May.	Jun.	YR. AVG
MANHATTAN:	WARDS ISLAND	283	273	261	252	261	245	241	241	229	220	218		248
	NORTH RIVER	170	167	166	158	167	155	157	156	149	146	147		158
BRONX:	HUNTS POINT	148	143	138	136	137	133	132	133	125	125	121		134
BROOKLYN:	26TH WARD	76	76	78	76	70	80	74	74	72	68	72		74
	CONEY ISLAND	104	107	106	103	105	100	102	99	95	95	99		101
	OWLS HEAD	129	132	127	123	126	126	120	125	119	123	122		125
	NEWTOWN CREEK	316	316	39	274	279	270	256	270	257	269	281		257
	RED HOOK	43	42	40	42	43	42	39	38	38	40	38		40
QUEENS:	JAMAICA	90	90	84	71	85	76	85	84	83	84	82		83
	TALLMAN ISLAND	56	59	58	55	55	56	54	54	52	53	55		55
	BOWERY BAY	119	125	121	118	119	119	114	115	106	108	112		116
	ROCKAWAY	24	25	25	24	24	25	24	21	21	21	22		23
STATEN ISLAND:	OAKWOOD BEACH	27	28	28	26	28	31	31	24	24	18	23		26
	PORT RICHMOND	41	41	38	37	38	38	39	40	39	37	37		39
TOTAL		1626	1623	1309	1495	1537	1496	1468	1473	1409	1408	1429		1479

WARDS ISLAND
PROCESS EFFICIENCY SUMMARY
TABLE NO. 4

PDES ID. NY0026131

FISCAL YEAR 1995

MONTH	<u>S U S P E N D E D S O L I D S</u>					<u>B I O C H E M I C A L O X Y G E N D E M A N D</u>						
	<u>RAW</u>	<u>PRIMARY</u>	<u>REMOVAL</u>	<u>PLANT</u>	<u>REMOVAL</u>	<u>RAW SEWAGE</u>		<u>PRIMARY EFFLUENT</u>		<u>PLANT EFFLUENT</u>		
	<u>SEWAGE</u>	<u>EFFLUENT</u>	<u>%</u>	<u>EFFLUENT</u>	<u>%</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>TOTAL</u>	<u>REMOVAL</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>REMOVAL</u>
	<u>mg/L</u>	<u>mg/L</u>		<u>mg/L</u>		<u>mg/L</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>
JUL	84	60	29	9	89	69	25	49	29	9	9	87
AUG	83	63	24	6	93	77	27	48	38	7	7	91
SEP	92	64	30	7	92	80	35	54	33	8	10	90
OCT	91	85	7	12	87	94	45	62	34	9	7	90
NOV	95	70	26	11	88	96	45	60	38	9	8	91
DEC	91	61	33	7	92	86	43	56	35	9	9	90
JAN	101	63	38	8	92	97	44	60	38	10	9	90
<u>AVERAGE:</u>	<u>90</u>	<u>67</u>	<u>26</u>	<u>9</u>	<u>90</u>	<u>83</u>	<u>36</u>	<u>55</u>	<u>34</u>	<u>8</u>	<u>9</u>	<u>90</u>

NOTE: Average as flow weighted.

Wards Island
Heavy Metals
Influent/Effluent (mg/L)
Fiscal Year 1995

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Ba		Ag	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	0.039	0.0180	0.0071	0.0027	0.0040	0.0026	0.065	0.045	0.0088	0.0022	0.00019	0.00005	0.00007	0.00007	0.00073	0.00061	0.00008	0.00008	0.00120	0.00022
Aug.	0.044	0.0100	0.0120	0.0018	0.0043	0.0031	0.051	0.018	0.0087	0.0014	0.00019	0.00006	0.00018	0.00006	0.00039	0.00038	0.00008	0.00008	0.00300	0.00025
Sep.	0.044	0.0056	0.0063	0.0013	0.0068	0.0030	0.054	0.017	0.0069	0.0016	0.00029	0.00003	0.00019	0.00006	0.00058	0.00043	0.00003	0.00004	0.00520	0.00034
Oct.	0.038	0.0100	0.0025	0.0009	0.0036	0.0007	0.046	0.028	0.0100	0.0026	0.00050	0.00042	0.00016	0.00006	0.00064	0.00041	0.00005	0.00005	0.00460	0.00110
Nov.	0.035	0.0091	0.0041	0.0004	0.0010	0.0010	0.044	0.025	0.0071	0.0018	0.00003	0.00003	0.00009	0.00006	0.00057	0.00048	0.00003	0.00003	0.00097	0.00055
Dec.	0.038	0.0062	0.0018	0.0007	0.0025	0.0010	0.047	0.023	0.0056	0.0014	0.00011	0.00004	0.00006	0.00006	0.00072	0.00051	0.00003	0.00003	0.00230	0.00045
Jan.	0.055	0.0080	0.0047	0.0005	0.0057	0.0034	0.082	0.017	0.0190	0.0013	0.00057	0.00006	0.00030	0.00006	0.00036	0.00026	0.00003	0.00003	0.00260	0.00070
Feb.	0.035	0.0062	0.0041	0.0018	0.0022	0.0026	0.050	0.050	0.0055	0.0023	0.00018	0.00005	0.00013	0.00006	0.00061	0.00054	0.00003	0.00003	0.00190	0.00055
Mar.	0.045	0.0120	0.0024	0.0027	0.0120	0.0093	0.100	0.059	0.0290	0.0120	0.00580	0.00003	0.00006	0.00006	0.00084	0.00072	0.00005	0.00003	0.00350	0.00180
Apr.	0.031	0.0068	0.0029	0.0007	0.0029	0.0020	0.037	0.015	0.0063	0.0010	0.00009	0.00003	0.00011	0.00006	0.00047	0.00045	0.00003	0.00003	0.00260	0.00180
May.	0.037	0.0086	0.0016	0.0002	0.0029	0.0022	0.052	0.019	0.0081	0.0023	0.00011	0.00012	0.00011	0.00006	0.00037	0.00024	0.00003	0.00003	0.00250	0.00029
Jun.	0.047	0.0098	0.0020	0.0016	0.0023	0.0035	0.049	0.017	0.0079	0.0010	0.00016	0.00003	0.00010	0.00006	0.00056	0.00035	0.00003	0.00003	0.00086	0.00200
AVG.	0.041	0.009	0.0043	0.0013	0.0042	0.0029	0.056	0.028	0.0102	0.0026	0.00069	0.00008	0.00013	0.00006	0.00057	0.00045	0.00004	0.00004	0.00260	0.00084

Wards Island
Nutrients (mg/L)
Fiscal Year 1995

DATE	NH3		ORG		TKN		NO3		NO2		PHOS.-TOTAL		PHOS.-ORTHO		CYANIDE	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	7.36	11.91	9.18	2.93	16.5	16.4	0.2155	0.1618	0.057	0.108	1.925	1.439	1.088	1.163	0.020	0.020
Aug.	7.51	11.84	6.25	6.40	13.8	18.2	0.3850	0.2700	0.063	0.095	1.756	1.877	1.335	1.485	0.020	0.020
Sep.	6.25	9.38	10.28	8.38	16.5	17.8	0.1343	0.0730	0.033	0.067	1.765	1.458	0.969	1.074	0.020	0.020
Oct.	12.15	14.05	9.75	6.43	21.9	20.5	0.1120	0.2412	0.046	0.079	1.962	2.124	1.592	0.972	0.020	0.020
Nov.	6.73	13.65	15.97	9.54	22.7	23.2	0.2567	0.1910	0.039	0.068	1.817	1.165	1.213	1.319	0.020	0.020
Dec.	8.58	11.20	8.95	7.20	17.5	18.4	0.1085	0.1286	0.021	0.084	2.105	1.298	1.125	1.085	0.020	0.020
Jan.	8.58	11.72	12.05	10.62	20.6	22.3	0.2870	0.2744	0.043	0.073	1.994	3.432	1.400	1.185	0.020	0.020
Feb.	7.65	11.70	9.50	8.86	17.1	20.5	0.2050	0.1289	0.030	0.055	2.711	1.390	1.072	1.090	0.020	0.020
Mar.	8.50	10.60	9.00	8.27	17.5	18.9	0.1130	0.0975	0.022	0.047	2.195	1.968	1.105	1.078	0.020	0.020
Apr.	12.75	13.17	11.30	6.83	24.0	20.0	0.1590	0.1082	0.086	0.074	2.183	1.553	1.612	1.332	0.020	0.020
May.	10.95	12.60	14.10	5.97	25.1	18.6	0.1475	0.1005	0.038	0.052	2.512	1.807	1.873	1.374	0.020	0.020
Jun.	8.10	11.74	8.45	4.79	16.5	16.3	0.0830	0.1321	0.020	0.074	2.165	1.164	1.125	1.082	0.020	0.020
AVG.	8.76	11.96	10.40	7.18	19.1	19.3	0.1839	0.1589	0.041	0.073	2.091	1.723	1.292	1.186	0.020	0.020

HUNTS POINT
 PROCESS EFFICIENCY SUMMARY
 TABLE NO. 4

SPDES ID. NY0026191

FISCAL YEAR 1995

MONTH	<u>SUSPENDED SOLIDS</u>					<u>BIOCHEMICAL OXYGEN DEMAND</u>						
	<u>RAW</u>	<u>PRIMARY</u>	<u>REMOVAL</u>	<u>PLANT</u>	<u>REMOVAL</u>	<u>RAW SEWAGE</u>		<u>PRIMARY EFFLUENT</u>		<u>PLANT EFFLUENT</u>		
	<u>SEWAGE</u>	<u>EFFLUENT</u>	<u>%</u>	<u>EFFLUENT</u>	<u>%</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>TOTAL</u>	<u>REMOVAL</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>REMOVAL</u>
	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>
JUL	99	72	27	7	93	84	31	59	30	6	5	93
AUG	101	72	29	6	94	89	35	60	33	5	4	94
SEP	104	90	13	6	94	96	39	68	29	5	5	95
OCT	101	95	6	10	90	105	43	76	28	7	7	93
NOV	102	83	19	10	90	97	44	67	31	8	7	92
DEC	93	80	14	8	91	98	85	83	15	10	11	90
JAN	82	84	0	6	93	106	49	84	21	9	8	92
<u>AVERAGE:</u>	<u>98</u>	<u>83</u>	<u>18</u>	<u>8</u>	<u>92</u>	<u>96</u>	<u>46</u>	<u>70</u>	<u>28</u>	<u>7</u>	<u>7</u>	<u>93</u>

NOTE: Average as flow weighted.

Hunts Point
Heavy Metals
Influent/Effluent (mg/L)
Fiscal Year 1995

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Be		Ag	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Ju1.	0.042	0.0047	0.0120	0.0016	0.0031	0.0040	0.100	0.029	0.0094	0.0004	0.00270	0.00038	0.00021	0.00007	0.00086	0.00057	0.00008	0.00008	0.00190	0.00022
Aug.	0.073	0.0068	0.0100	0.0013	0.0095	0.0047	0.150	0.021	0.0270	0.0006	0.00140	0.00021	0.00022	0.00007	0.00098	0.00049	0.00008	0.00008	0.00410	0.00032
Sep.	0.074	0.0053	0.0014	0.0014	0.0077	0.0028	0.100	0.019	0.0180	0.0017	0.00094	0.00034	0.00035	0.00016	0.00073	0.00046	0.00003	0.00003	0.00680	0.00020
Oct.	0.120	0.0210	0.0220	0.0019	0.0120	0.0110	0.180	0.050	0.0310	0.0034	0.00210	0.00017	0.00026	0.00006	0.00088	0.00063	0.00006	0.00005	0.00600	0.00074
Nov.	0.059	0.0085	0.0770	0.0037	0.0120	0.0073	0.078	0.034	0.0130	0.0016	0.00200	0.00110	0.00023	0.00530	0.00086	0.00067	0.00003	0.00003	0.00380	0.00062
Dec.	0.096	0.0120	0.0230	0.0018	0.0071	0.0041	0.130	0.023	0.0130	0.0019	0.00170	0.00019	0.00019	0.00006	0.00084	0.00016	0.00003	0.00003	0.00600	0.00060
Jan.	0.088	0.0042	0.0150	0.0034	0.0064	0.0062	0.110	0.043	0.0190	0.0029	0.00160	0.00069	0.00006	0.00006	0.00050	0.00043	0.00004	0.00003	0.00740	0.00150
Feb.	0.094	0.0074	0.0150	0.0018	0.0110	0.0140	0.130	0.036	0.0120	0.0023	0.00140	0.00044	0.00012	0.00006	0.00076	0.00049	0.00004	0.00003	0.00630	0.00057
Mar.	0.038	0.0084	0.0073	0.0009	0.0099	0.0077	0.051	0.037	0.0072	0.0010	0.00034	0.00008	0.00006	0.00006	0.00043	0.00029	0.00003	0.00003	0.00330	0.00020
Apr.	0.079	0.0077	0.0130	0.0015	0.0230	0.0160	0.110	0.028	0.0160	0.0012	0.00150	0.00022	0.00006	0.00006	0.00079	0.00059	0.00003	0.00003	0.00560	0.00020
May.	0.140	0.0092	0.0160	0.0006	0.0120	0.0089	0.180	0.028	0.0260	0.0010	0.00150	0.00003	0.00021	0.00006	0.00075	0.00033	0.00003	0.00003	0.00740	0.00031
Jun.	0.180	0.0140	0.0260	0.0014	0.0700	0.0110	0.240	0.031	0.0420	0.0024	0.00230	0.00014	0.00038	0.00006	0.00100	0.00050	0.00006	0.00003	0.01300	0.00180
AVG.	0.090	0.009	0.0198	0.0018	0.0153	0.0081	0.130	0.032	0.0195	0.0017	0.00162	0.00033	0.00020	0.00051	0.00078	0.00047	0.00005	0.00004	0.00594	0.00061

Hunts Point
Heavy Metals
Sludge (mg/kg)
Fiscal Year 1995

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Be		V		Ag		SOL %
	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	WET	DRY	
Jul.	20	952	3.8	181	0.97	46	27	1286	8.1	386	0.300	14.0	0.082	3.9	0.1100	5.2	0.0071	0.340	1.40	67	0.96	46	2.1
Aug.	18	900	3.1	155	1.20	60	25	1250	6.6	330	0.500	25.0	0.079	4.0	0.1100	5.5	0.0076	0.380	1.10	55	1.30	65	2.0
Sep.	21	1105	4.2	221	2.20	116	24	1263	6.5	342	0.240	13.0	0.084	4.4	0.0880	4.6	0.0054	0.280	0.91	48	1.20	63	1.9
Oct.	22	1000	4.3	195	1.30	59	26	1182	5.6	255	0.290	13.0	0.068	3.1	0.0970	4.4	0.0047	0.200	1.60	73	1.80	82	2.2
Nov.	26	1130	4.6	200	1.50	65	29	1261	6.8	296	0.420	18.0	0.087	3.8	0.1200	5.2	0.0069	0.300	1.20	52	2.00	87	2.3
Dec.	24	1143	4.8	229	1.40	67	30	1429	6.7	319	0.440	21.0	0.084	4.0	0.1000	4.8	0.0083	0.400	1.70	81	2.00	95	2.1
Jan.	25	1087	5.4	235	1.50	65	31	1348	6.8	296	0.410	18.0	0.100	4.3	0.0590	2.6	0.0070	0.300	1.70	74	1.60	70	2.3
Feb.	23	1211	4.2	221	2.10	111	25	1316	5.0	263	0.260	14.0	0.072	3.8	0.1100	5.8	0.0074	0.390	1.20	63	1.70	89	1.9
Mar.	20	1111	3.7	206	1.30	72	24	1333	4.2	233	0.270	15.0	0.064	3.6	0.1200	6.7	0.0050	0.280	0.96	53	1.50	83	1.8
Apr.	19	1056	3.2	178	0.96	53	23	1278	4.0	222	0.280	16.0	0.060	3.3	0.0830	4.6	0.0058	0.320	0.75	42	1.40	78	1.8
May.																							
Jun.																							
AVG.	22	1070	4.1	202	1.44	71	26	1295	6.0	294	0.341	16.7	0.078	3.82	0.0997	4.9	0.0065	0.319	1.25	61	1.55	76	2.0

Hunts Point
Nutrients (mg/L)
Fiscal Year 1995

DATE	NH3		ORG		TKN		NO3		NO2		PHOS.-TOTAL		PHOS.-ORTHO		CYANIDE	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	10.40	9.58	11.16	8.12	21.6	17.7	0.2060	1.1300	0.056	0.401	1.899	1.187	1.168	1.037	0.020	0.020
Aug.	10.86	13.84	12.53	14.15	23.4	28.0	0.4113	0.6313	0.077	0.256	2.311	1.817	1.387	1.500	0.020	0.020
Sep.	8.41	13.70	10.60	5.68	19.0	19.4	0.1598	0.4993	0.030	0.264	2.358	2.021	1.333	1.688	0.020	0.020
Oct.	12.32	13.11	15.70	7.41	28.0	20.5	0.1350	3.3347	0.011	0.769	1.854	0.978	1.218	0.897	0.020	0.020
Nov.	10.60	15.35	17.90	9.04	28.5	24.4	0.2525	3.8892	0.043	0.987	2.162	1.934	1.135	1.724	0.020	0.020
Dec.	10.05	12.61	10.95	8.52	21.0	21.1	0.0870	4.6800	0.028	0.391	1.929	1.789	1.201	1.597	0.020	0.020
Jan.	12.87	11.94	6.65	9.74	19.5	21.7	0.3360	3.6233	0.097	0.345	2.767	1.794	1.455	1.370	0.020	0.020
Feb.	11.85	10.39	13.80	8.89	25.7	19.3	0.2670	3.3018	0.053	0.279	2.580	2.310	1.510	1.910	0.020	0.020
Mar.	9.93	10.84	9.75	7.92	19.7	18.7	0.1225	5.6922	0.043	0.512	2.157	2.119	0.981	1.821	0.020	0.020
Apr.	12.60	12.06	10.90	7.17	23.5	19.2	0.0885	4.3963	0.042	0.702	2.242	1.979	1.425	1.319	0.020	0.020
May.	11.98	15.88	13.55	8.36	25.5	24.2	0.0695	2.8538	0.021	0.731	2.487	2.264	1.281	1.772	0.020	0.020
Jun.	13.33	16.09	6.45	6.46	19.8	22.5	0.0950	4.0172	0.030	1.019	1.988	1.758	1.425	1.545	0.020	0.020
AVG.	11.26	12.95	11.66	8.45	22.9	21.4	0.1858	3.1708	0.044	0.555	2.228	1.829	1.293	1.515	0.020	0.020

26th WARD
 PROCESS EFFICIENCY SUMMARY
 TABLE NO. 4

SPDES ID. NY0026212

FISCAL YEAR 1995

MONTH	<u>SUSPENDED SOLIDS</u>					<u>BIOCHEMICAL OXYGEN DEMAND</u>						
	<u>RAW</u>	<u>PRIMAY</u>	<u>REMOVAL</u>	<u>PLANT</u>	<u>REMOVAL</u>	<u>RAW SEWAGE</u>		<u>PRIMARY EFFLUENT</u>		<u>PLANT EFFLUENT</u>		
	<u>SEWAGE</u>	<u>EFFLUENT</u>	<u>%</u>	<u>EFFLUENT</u>	<u>%</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>TOTAL</u>	<u>REMOVAL</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>REMOVAL</u>
	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>
JUL	91	50	45	7	92	102	67	73	28	8	6	92
AUG	88	45	49	8	91	115	55	82	29	10	6	91
SEP	90	55	39	9	90	98	51	76	22	9	5	91
OCT	90	57	37	8	91	120	60	92	23	11	6	91
NOV	90	53	41	22	76	118	61	90	24	18	7	85
DEC	80	60	25	13	84	106	60	91	14	16	9	85
JAN	79	67	15	12	85	117	62	92	21	15	8	87
AVERAGE:	87	55	39	11	88	111	59	85	24	12	7	89

NOTE: Average as flow weighted.

26th Ward
Heavy Metals
Influent/Effluent (mg/L)
Fiscal Year 1995

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Be		Ag	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Ju1.	0.066	0.0180	0.0046	0.0046	0.0031	0.0020	0.150	0.110	0.0130	0.0110	0.00540	0.00040	0.00007	0.00006	0.00120	0.00068	0.00008	0.00008	0.00093	0.00022
Aug.	0.210	0.0075	0.0048	0.0011	0.0150	0.0007	0.150	0.014	0.0200	0.0034	0.00042	0.00003	0.00012	0.00008	0.00060	0.00064	0.00008	0.00008	0.00330	0.00020
Sep.	0.050	0.0048	0.0039	0.0014	0.0076	0.0042	0.080	0.016	0.0190	0.0020	0.00009	0.00003	0.00026	0.00021	0.00054	0.00050	0.00003	0.00003	0.00100	0.00020
Oct.	0.110	0.0053	0.0270	0.0020	0.0085	0.0031	0.260	0.016	0.1100	0.0035	0.00170	0.00032	0.00050	0.00006	0.00150	0.00057	0.00009	0.00005	0.00280	0.00029
Nov.	0.067	0.0450	0.0038	0.0034	0.0032	0.0016	0.082	0.067	0.0095	0.0099	0.00120	0.00018	0.00009	0.00006	0.00038	0.00037	0.00013	0.00003	0.00150	0.00150
Dec.	0.042	0.0078	0.0036	0.0009	0.0047	0.0032	0.063	0.019	0.0100	0.0018	0.00051	0.00018	0.00006	0.00006	0.00054	0.00050	0.00003	0.00003	0.00140	0.00018
Jan.	0.032	0.0057	0.0034	0.0036	0.0027	0.0018	0.076	0.021	0.0130	0.0022	0.00035	0.00004	0.00008	0.00006	0.00052	0.00033	0.00006	0.00003	0.00093	0.00033
Feb.	0.052	0.0086	0.0028	0.0022	0.0120	0.0031	0.064	0.025	0.0082	0.0032	0.00065	0.00016	0.00017	0.00006	0.00038	0.00029	0.00003	0.00003	0.00210	0.00024
Mar.	0.029	0.0072	0.0240	0.0063	0.0035	0.0029	0.050	0.029	0.0100	0.0024	0.00086	0.00003	0.00006	0.00006	0.00026	0.00026	0.00003	0.00003	0.00150	0.00020
Apr.	0.036	0.0063	0.0023	0.0009	0.0021	0.0013	0.054	0.012	0.0072	0.0021	0.00018	0.00017	0.00006	0.00006	0.00064	0.00043	0.00004	0.00004	0.00130	0.00020
May.	0.065	0.0088	0.0019	0.0012	0.0038	0.0026	0.170	0.019	0.0066	0.0044	0.00017	0.00003	0.00024	0.00006	0.00031	0.00028	0.00003	0.00003	0.00170	0.00021
Jun.	0.076	0.0070	0.0051	0.0012	0.0051	0.0025	0.150	0.026	0.0420	0.0053	0.00037	0.00003	0.00006	0.00006	0.00087	0.00054	0.00003	0.00003	0.00160	0.00020
AVG.	0.070	0.011	0.0073	0.0024	0.0059	0.0024	0.112	0.031	0.0224	0.0043	0.00099	0.00013	0.00015	0.00007	0.00065	0.00045	0.00006	0.00004	0.00167	0.00033

26th Ward
Nutrients (mg/L)
Fiscal Year 1995

DATE	NH3		ORG		TKN		NO3		NO2		PHOS.-TOTAL		PHOS.-ORTHO		CYANIDE	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	6.07	8.96	8.95	7.55	15.0	16.5	0.1850	1.0000	0.043	0.939	2.130	1.428	1.203	1.225	0.020	0.020
Aug.	6.40	8.80	13.13	8.48	19.5	17.3	0.2050	1.3250	0.059	0.990	2.033	1.660	1.140	1.413	0.020	0.020
Sep.	6.64	10.05	11.13	9.95	17.8	20.0	0.3100	0.9250	0.089	1.227	2.068	1.283	1.043	1.088	0.020	0.020
Oct.	7.95	11.54	6.55	12.17	14.5	23.7	0.0500	1.3032	0.078	0.819	2.770	2.637	1.390	1.210	0.020	0.020
Nov.	6.40	8.16	17.15	7.49	23.5	15.6	0.1750	2.7367	0.074	0.817	2.515	2.255	1.587	1.655	0.020	0.020
Dec.	8.40	10.57	14.10	8.86	22.5	19.4	0.5100	1.4967	0.101	0.698	2.330	1.535	1.420	0.980	0.020	0.020
Jan.	7.30	13.58	13.20	10.19	20.5	23.8	0.2500	0.7474	0.123	0.735	2.425	1.185	1.150	0.555	0.020	0.020
Feb.	6.50	13.24	20.50	11.53	27.0	24.7	0.6100	0.7643	0.138	0.527	3.170	2.610	0.985	0.990	0.020	0.020
Mar.	7.00	12.35	14.50	10.68	21.5	23.0	0.2650	0.5171	0.060	0.409	1.925	1.105	1.020	0.880	0.020	0.020
Apr.	9.28	16.52	13.75	10.02	23.0	26.5	0.2150	0.3553	0.061	0.359	2.295	1.625	1.515	1.350	0.020	0.020
May.	12.30	16.90	11.20	9.23	23.5	26.1	0.0400	0.3468	0.041	0.315	2.420	1.920	1.370	1.155	0.020	0.020
Jun.	8.85	16.85	13.65	8.22	22.5	25.1	3.7900	0.5253	0.078	0.807	2.255	1.330	1.215	1.096	0.020	0.020
AVG.	7.76	12.29	13.15	9.53	20.9	21.8	0.5504	1.0036	0.079	0.720	2.361	1.714	1.253	1.133	0.020	0.020

TALLMAN ISLAND
 PROCESS EFFICIENCY SUMMARY
 TABLE NO. 4

PDES ID. NY0026239

FISCAL YEAR 1995

MONTH	<u>SUSPENDED SOLIDS</u>					<u>BIOCHEMICAL OXYGEN DEMAND</u>						
	<u>RAW</u>	<u>PRIMARY</u>	<u>REMOVAL</u>	<u>PLANT</u>	<u>REMOVAL</u>	<u>RAW SEWAGE</u>		<u>PRIMARY EFFLUENT</u>		<u>PLANT EFFLUENT</u>		
	<u>SEWAGE</u>	<u>EFFLUENT</u>	<u>%</u>	<u>EFFLUENT</u>	<u>%</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>TOTAL</u>	<u>REMOVAL</u>	<u>TOTAL</u>	<u>FILTRATE</u>	<u>REMOVAL</u>
	<u>mg/L</u>	<u>mg/L</u>		<u>mg/L</u>		<u>mg/L</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>	<u>mg/L</u>	<u>mg/L</u>	<u>%</u>
JUL	96	56	42	6	94	117	65	64	45	4	3	97
AUG	93	51	45	6	94	110	57	55	50	4	4	96
SEP	106	55	49	5	95	123	76	65	47	4	4	97
OCT	107	53	50	6	94	116	67	67	42	4	3	97
NOV	106	47	56	4	96	127	67	64	50	3	3	98
DEC	100	63	38	4	96	111	63	64	42	4	3	96
JAN	98	64	35	6	94	118	63	71	40	5	3	96
<u>AVERAGE:</u>	<u>101</u>	<u>55</u>	<u>47</u>	<u>5</u>	<u>95</u>	<u>118</u>	<u>66</u>	<u>65</u>	<u>46</u>	<u>4</u>	<u>3</u>	<u>97</u>

NOTE: Average as flow weighted.

Tallman Island
Heavy Metals
Influent/Effluent (mg/L)
Fiscal Year 1995

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Ba		Ag	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	0.047	0.0130	0.0089	0.0023	0.0084	0.0047	0.100	0.043	0.0080	0.0019	0.00029	0.00009	0.00009	0.00006	0.00035	0.00028	0.00008	0.00008	0.00430	0.00075
Aug.	0.057	0.0170	0.0052	0.0015	0.0140	0.0094	0.110	0.032	0.0066	0.0006	0.00110	0.00030	0.00016	0.00006	0.00045	0.00031	0.00008	0.00008	0.00680	0.00095
Sep.	0.039	0.0072	0.0059	0.0021	0.0130	0.0070	0.072	0.038	0.0110	0.0022	0.00025	0.00012	0.00012	0.00006	0.00022	0.00011	0.00003	0.00003	0.00450	0.00110
Oct.	0.070	0.0150	0.0110	0.0018	0.0170	0.0056	0.098	0.029	0.0086	0.0011	0.00038	0.00012	0.00021	0.00013	0.00060	0.00034	0.00006	0.00005	0.00680	0.00610
Nov.	0.057	0.0100	0.0092	0.0015	0.0069	0.0050	0.079	0.032	0.0140	0.0010	0.00028	0.00017	0.00035	0.00006	0.00035	0.00023	0.00003	0.00003	0.00680	0.00049
Dec.	0.040	0.0077	0.0110	0.0011	0.0066	0.0049	0.078	0.030	0.0100	0.0008	0.00028	0.00010	0.00013	0.00006	0.00076	0.00051	0.00004	0.00003	0.00430	0.00034
Jan.	0.056	0.0059	0.0110	0.0031	0.0110	0.0066	0.130	0.030	0.0120	0.0024	0.00048	0.00035	0.00012	0.00006	0.00045	0.00031	0.00004	0.00004	0.00700	0.00064
Feb.	0.054	0.0090	0.0061	0.0022	0.0090	0.0066	0.093	0.042	0.0120	0.0019	0.00110	0.00034	0.00020	0.00006	0.00064	0.00038	0.00003	0.00003	0.00550	0.00051
Mar.	0.044	0.0110	0.0058	0.0020	0.0230	0.0100	0.082	0.032	0.0049	0.0010	0.00027	0.00013	0.00006	0.00006	0.00037	0.00039	0.00003	0.00003	0.00500	0.00085
Apr.	0.065	0.0110	0.0120	0.0038	0.0084	0.0064	0.110	0.021	0.0120	0.0011	0.00039	0.00019	0.00010	0.00006	0.00056	0.00040	0.00003	0.00003	0.00770	0.00110
May.	0.057	0.0084	0.0044	0.0014	0.0057	0.0081	0.081	0.036	0.0093	0.0024	0.00031	0.00012	0.00006	0.00006	0.00035	0.00021	0.00003	0.00003	0.00570	0.00160
Jun.	0.110	0.0120	0.0130	0.0012	0.0150	0.0075	0.310	0.048	0.0120	0.0037	0.00049	0.00033	0.00020	0.00006	0.00052	0.00037	0.00003	0.00003	0.00800	0.00062
AVG.	0.058	0.011	0.0086	0.0020	0.0115	0.0068	0.112	0.034	0.0100	0.0017	0.00047	0.00020	0.00015	0.00007	0.00047	0.00032	0.00004	0.00004	0.00603	0.00125

Tallman Island
Nutrients (mg/L)
Fiscal Year 1995

DATE	NH3		ORG		TKN		NO3		NO2		PHOS.-TOTAL		PHOS.-ORTHO		CYANIDE	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	13.40	5.46	7.63	2.25	21.0	7.7	0.3435	7.4250	0.015	0.330	2.510	1.625	1.475	1.373	0.020	0.020
Aug.	11.83	4.35	7.05	2.18	18.9	6.5	0.3125	6.9575	0.035	0.221	2.245	1.365	1.408	1.140	0.020	0.020
Sep.	14.20	6.02	8.25	2.35	22.5	8.4	0.0535	4.8275	0.017	0.276	3.010	2.053	1.553	1.393	0.020	0.020
Oct.	13.45	4.87	8.15	2.45	21.6	7.3	0.1670	4.0910	0.012	0.273	2.630	1.790	1.560	1.170	0.020	0.020
Nov.	12.55	4.64	8.05	1.01	20.6	5.6	0.3395	4.5543	0.058	0.276	2.630	1.415	1.380	1.160	0.020	0.020
Dec.	8.90	5.24	12.95	1.29	21.9	6.5	0.2070	4.7074	0.057	0.287	2.945	1.900	1.370	1.040	0.020	0.020
Jan.	11.55	7.63	7.90	1.42	19.5	9.0	0.2415	3.3535	0.025	0.506	2.880	1.900	1.265	1.170	0.020	0.020
Feb.	11.36	7.93	12.75	1.70	24.1	9.6	0.1360	3.5393	0.044	0.899	2.375	1.280	1.150	0.817	0.020	0.020
Mar.	15.45	10.85	8.15	2.35	23.6	13.2	0.1670	2.5839	0.042	0.632	2.975	1.700	1.415	1.195	0.020	0.020
Apr.	18.90	12.55	10.75	2.42	29.7	15.0	0.2645	2.6587	0.066	0.296	3.315	2.240	1.870	1.510	0.020	0.020
May.	14.50	15.26	9.05	3.35	23.6	18.6	0.3670	0.8264	0.043	0.278	3.105	2.020	1.650	1.450	0.020	0.020
Jun.	18.15	15.55	7.35	3.13	25.5	18.7	0.3550	0.2595	0.045	0.262	3.580	2.415	2.160	1.230	0.020	0.020
AVG.	13.69	8.36	9.00	2.16	22.7	10.5	0.2462	3.8153	0.038	0.378	2.850	1.809	1.521	1.221	0.020	0.020

OAKWOOD BEACH
 PROCESS EFFICIENCY SUMMARY
 TABLE NO. 4

SPDES ID. NY0026174

FISCAL YEAR 1995

MONTH	SUSPENDED SOLIDS					BIOCHEMICAL OXYGEN DEMAND						
	RAW SEWAGE	PRIMARY EFFLUENT	REMOVAL	PLANT EFFLUENT	REMOVAL	RAW SEWAGE		PRIMARY EFFLUENT		PLANT EFFLUENT		
	mg/L	mg/L	%	mg/L	%	TOTAL mg/L	FILTRATE mg/L	TOTAL mg/L	REMOVAL %	TOTAL mg/L	FILTRATE mg/L	REMOVAL %
JUL	180	73	59	5	97	146	27	60	59	13	6	91
AUG	192	54	72	5	97	147	26	52	65	7	4	95
SEP	173	61	65	5	97	150	33	75	50	6	3	96
OCT	170	72	58	5	97	152	33	64	58	6	3	96
NOV	177	59	67	5	97	168	36	49	71	7	3	96
DEC	151	54	64	6	96	126	38	54	57	6	3	95
JAN	147	60	59	8	95	130	32	58	55	7	3	95
AVERAGE:	173	62	64	6	97	148	32	59	60	7	3	95

NOTE: Average as flow weighted.

Oakwood Beach
Heavy Metals
Influent/Effluent (mg/L)
Fiscal Year 1995

DATE	Cu		Cr		Ni		Zn		Pb		Cd		Hg		As		Ba		Ag	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	0.200	0.0190	0.0086	0.0011	0.0190	0.0066	0.290	0.028	0.0390	0.0006	0.00060	0.00003	0.00082	0.00006	0.00180	0.00065	0.00008	0.00008	0.01900	0.00022
Aug.	0.200	0.0054	0.0110	0.0013	0.0250	0.0038	0.270	0.017	0.0059	0.0009	0.00110	0.00005	0.00050	0.00006	0.00130	0.00041	0.00008	0.00008	0.02700	0.00330
Sep.	0.120	0.0074	0.0033	0.0005	0.0160	0.0036	0.130	0.022	0.0160	0.0019	0.00052	0.00010	0.00035	0.00006	0.00052	0.00023	0.00005	0.00003	0.00640	0.00072
Oct.	0.049	0.0084	0.0021	0.0010	0.0110	0.0080	0.070	0.030	0.0080	0.0020	0.00035	0.00018	0.00011	0.00006	0.00060	0.00043	0.00005	0.00005	0.00360	0.00038
Nov.	0.150	0.0089	0.0052	0.0006	0.0160	0.0045	0.200	0.017	0.0260	0.0017	0.00078	0.00003	0.00160	0.00006	0.00120	0.00021	0.00003	0.00003	0.01900	0.00052
Dec.	0.100	0.0058	0.0066	0.0006	0.0210	0.0079	0.140	0.025	0.0160	0.0016	0.00066	0.00004	0.00006	0.00006	0.00090	0.00056	0.00004	0.00003	0.01500	0.00049
Jan.	0.069	0.0043	0.0037	0.0008	0.0140	0.0063	0.098	0.033	0.0110	0.0019	0.00008	0.00004	0.00010	0.00006	0.00052	0.00024	0.00007	0.00003	0.00520	0.00057
Feb.	0.180	0.0057	0.0310	0.0010	0.0340	0.0072	0.270	0.026	0.0920	0.0018	0.00064	0.00004	0.00082	0.00006	0.00077	0.00044	0.00008	0.00003	0.01300	0.00390
Mar.	0.033	0.0070	0.0039	0.0004	0.0170	0.0120	0.048	0.029	0.0054	0.0010	0.00007	0.00003	0.00008	0.00006	0.00066	0.00047	0.00004	0.00003	0.00320	0.00038
Apr.	0.120	0.0087	0.0050	0.0005	0.0180	0.0077	0.140	0.010	0.0200	0.0010	0.00034	0.00004	0.00071	0.00006	0.00080	0.00057	0.00003	0.00003	0.00700	0.00077
May.	0.071	0.0093	0.0026	0.0013	0.0140	0.0087	0.100	0.016	0.0120	0.0013	0.00022	0.00003	0.00035	0.00006	0.00078	0.00052	0.00003	0.00003	0.00580	0.00044
Jun.	0.300	0.0190	0.0096	0.0005	0.0280	0.0014	0.340	0.011	0.0070	0.0020	0.00091	0.00017	0.00200	0.00006	0.00180	0.00034	0.00007	0.00003	0.02600	0.00200
AVG.	0.133	0.009	0.0077	0.0008	0.0194	0.0065	0.175	0.022	0.0215	0.0015	0.00052	0.00007	0.00063	0.00006	0.00097	0.00042	0.00005	0.00004	0.01252	0.00114

Oakwood Beach
Nutrients (mg/L)
Fiscal Year 1995

DATE	NH3		ORG		TKN		NO3		NO2		PHOS.-TOTAL		PHOS.-ORTHO		CYANIDE	
	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.	INF.	EFF.
Jul.	16.91	10.19	22.75	3.08	39.7	13.3	0.5788	3.1525	0.021	0.610	6.393	2.645	2.277	2.324	0.020	0.020
Aug.	15.32	5.48	21.58	2.80	36.9	8.3	0.3933	4.2158	0.032	0.461	6.492	3.486	2.463	2.244	0.020	0.020
Sep.	17.32	4.29	12.23	1.48	29.6	5.8	0.4053	5.0495	0.025	0.363	4.836	2.987	2.355	2.409	0.020	0.020
Oct.	18.64	5.65	21.05	1.63	39.7	7.3	0.3013	5.5205	0.060	0.344	6.163	2.898	2.790	2.636	0.020	0.020
Nov.	16.39	5.56	36.60	1.60	53.0	7.2	0.4468	6.0798	0.053	0.400	10.289	3.180	3.138	3.065	0.020	0.020
Dec.	17.32	6.74	15.45	2.53	32.8	9.3	0.5690	5.3878	0.081	0.429	5.100	3.390	2.720	2.750	0.020	0.020
Jan.	15.93	6.70	14.85	1.83	30.8	8.5	0.4853	4.0005	0.065	0.345	4.463	2.395	2.424	2.065	0.020	0.020
Feb.	19.29	9.24	17.68	2.78	37.0	12.0	0.5900	3.3450	0.160	0.561	5.337	1.414	2.800	0.908	0.020	0.020
Mar.	26.07	13.08	38.35	2.90	64.4	16.0	0.2650	1.3490	0.035	0.401	11.837	2.982	4.499	1.555	0.020	0.020
Apr.	20.20	15.29	19.10	12.75	39.3	28.0	0.2335	2.9490	0.017	0.426	4.962	3.629	2.899	2.644	0.020	0.020
May.	18.86	14.58	24.65	1.45	43.5	16.0	0.2200	2.7680	0.030	0.420	8.596	2.455	2.948	2.104	0.020	0.020
Jun.	28.04	22.23	26.45	5.80	54.5	28.0	0.3150	0.8080	0.035	0.143	7.595	4.272	4.382	3.941	0.020	0.020
AVG.	19.19	9.92	22.56	3.38	41.7	13.3	0.4003	3.7188	0.051	0.408	6.838	2.978	2.975	2.387	0.020	0.020

MONTHLY FLOW RATE

comparison of all plants

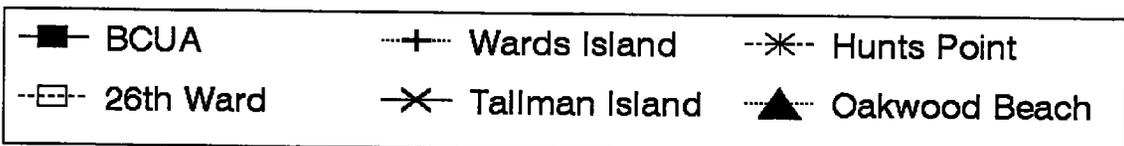
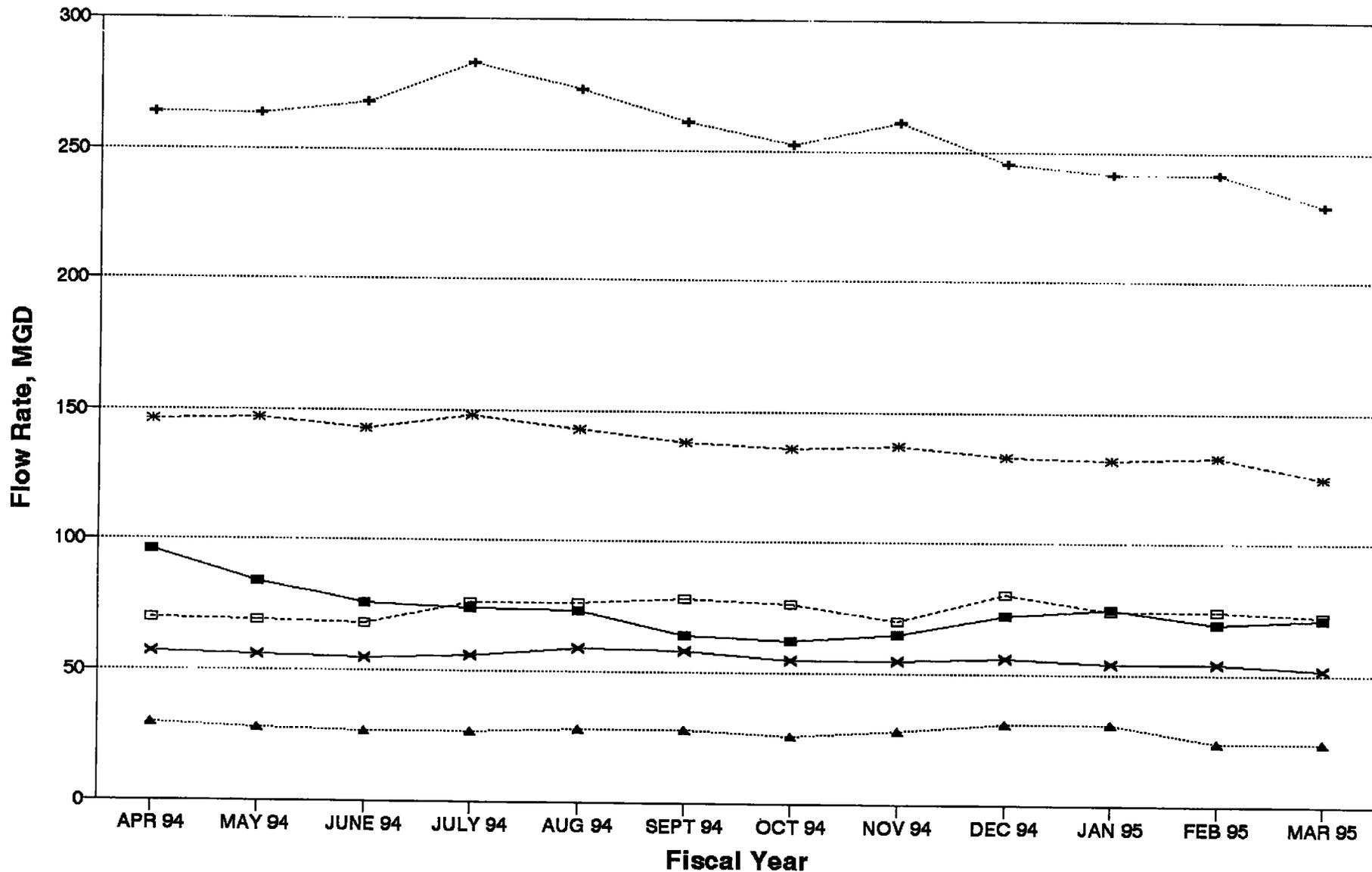
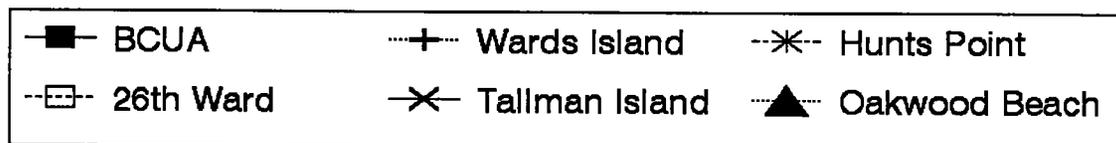
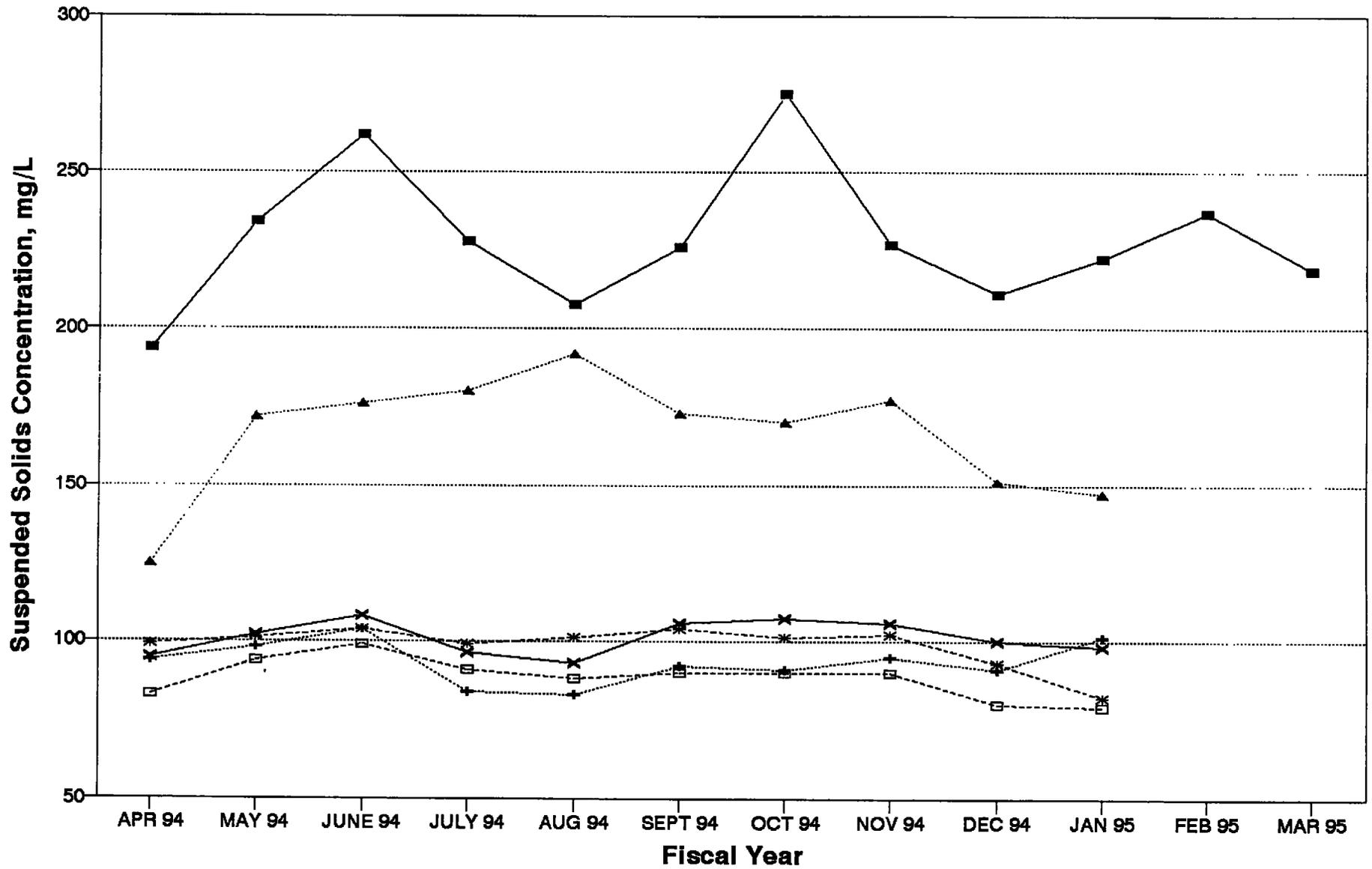


Figure 1

SUSPENDED SOLIDS, INFLUENT

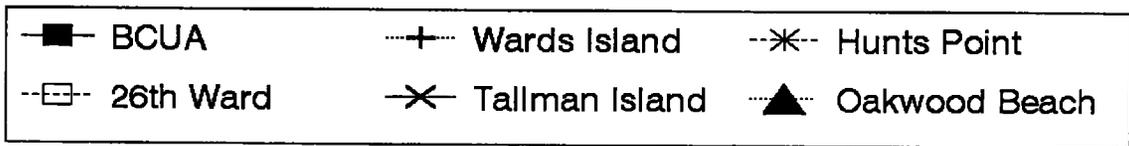
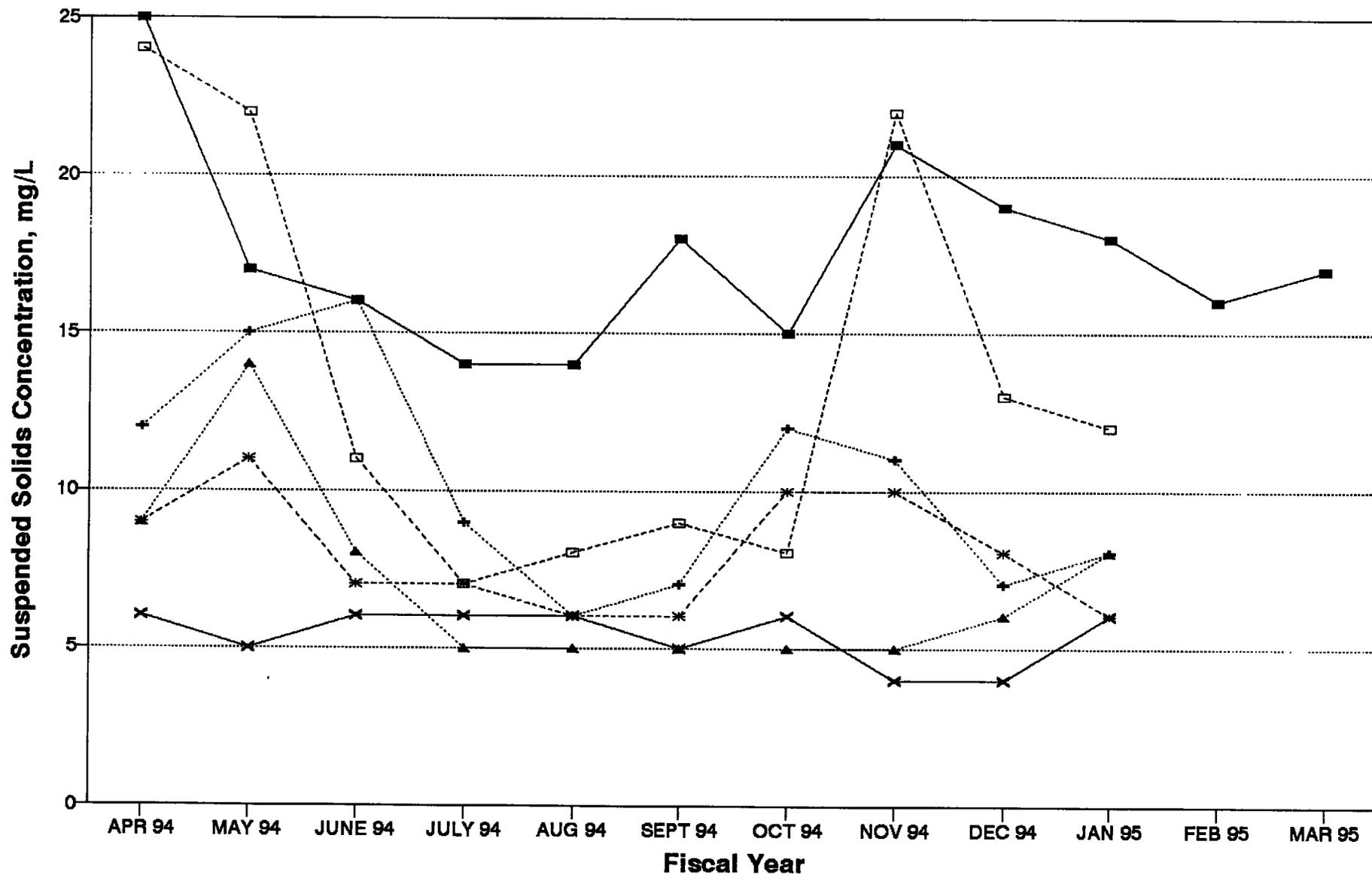
comparison of all plants



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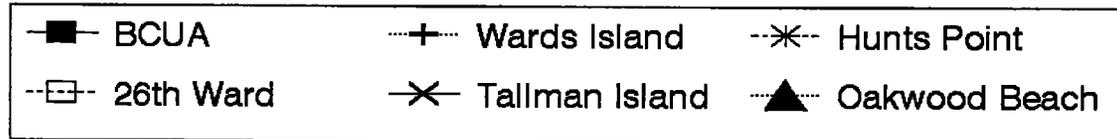
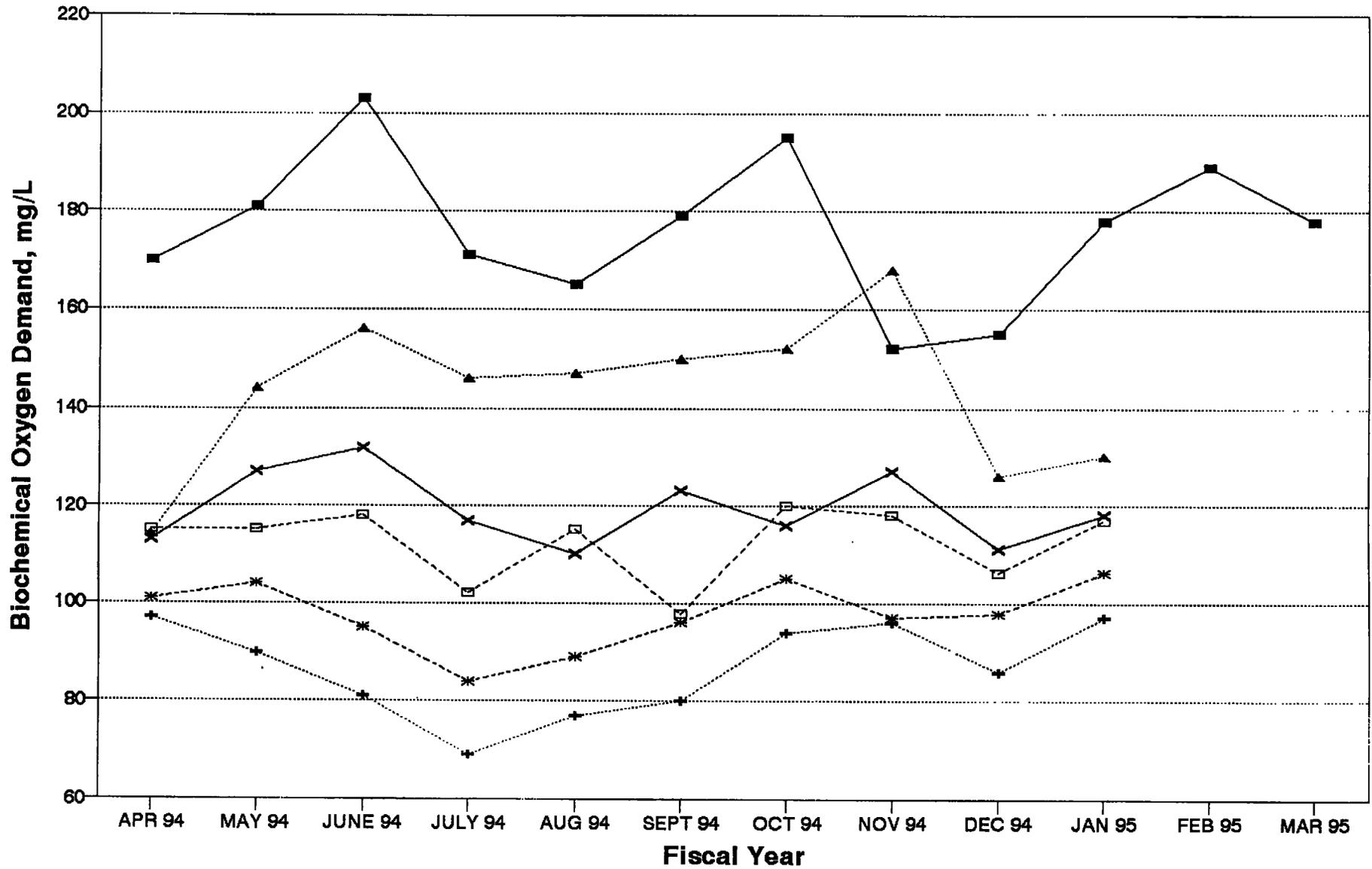
SUSPENDED SOLIDS, EFFLUENT

comparison of all plants



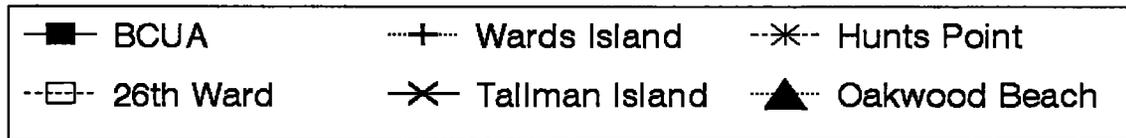
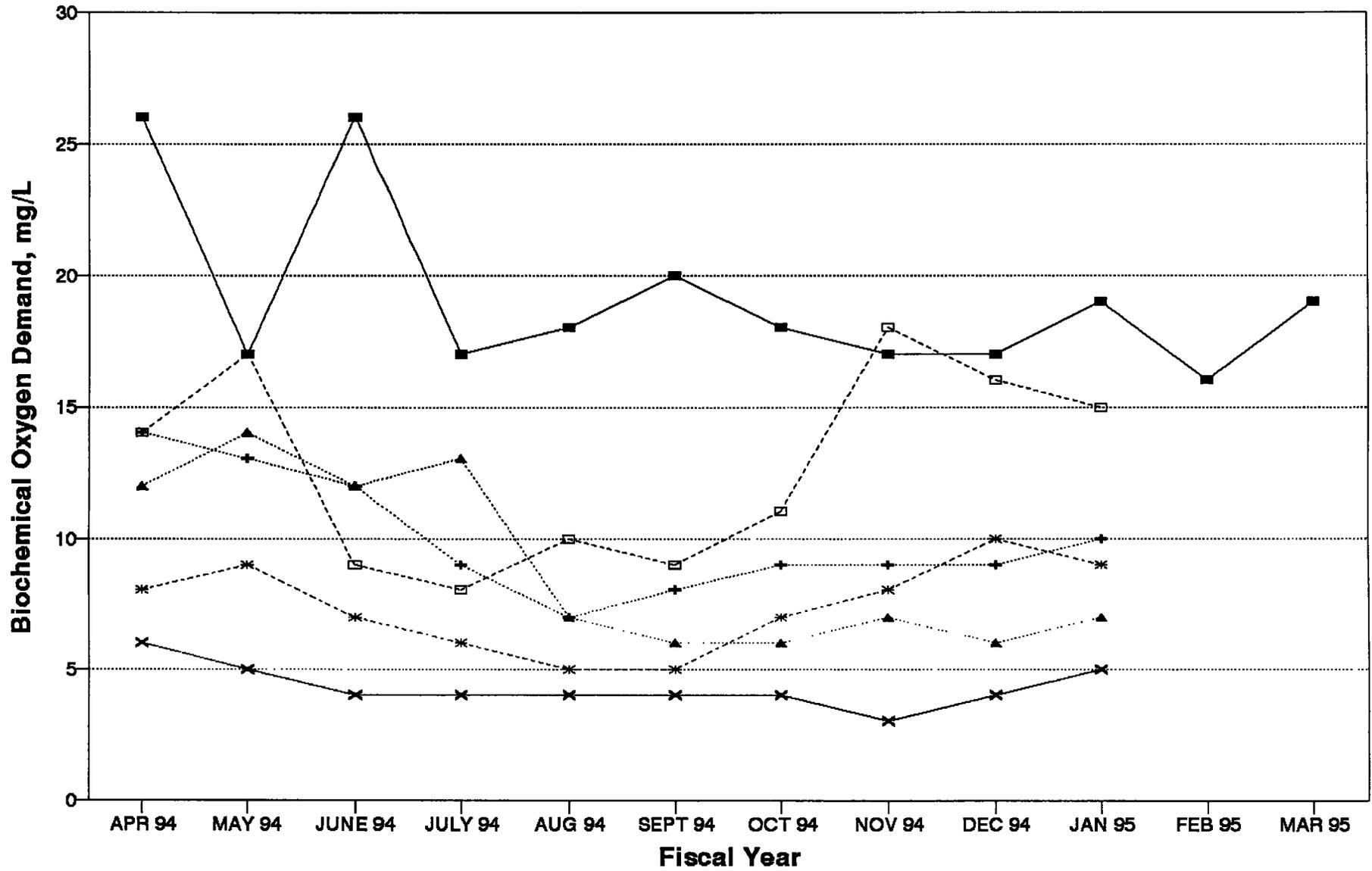
BOD, INFLUENT

comparison of all plants



BOD, EFFLUENT

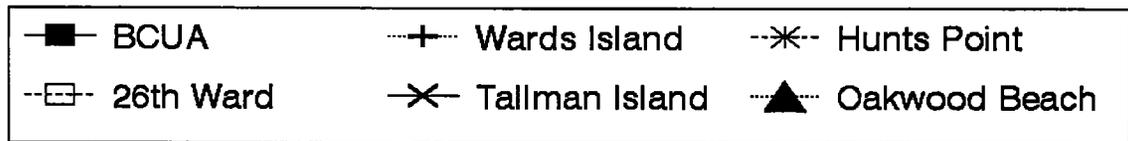
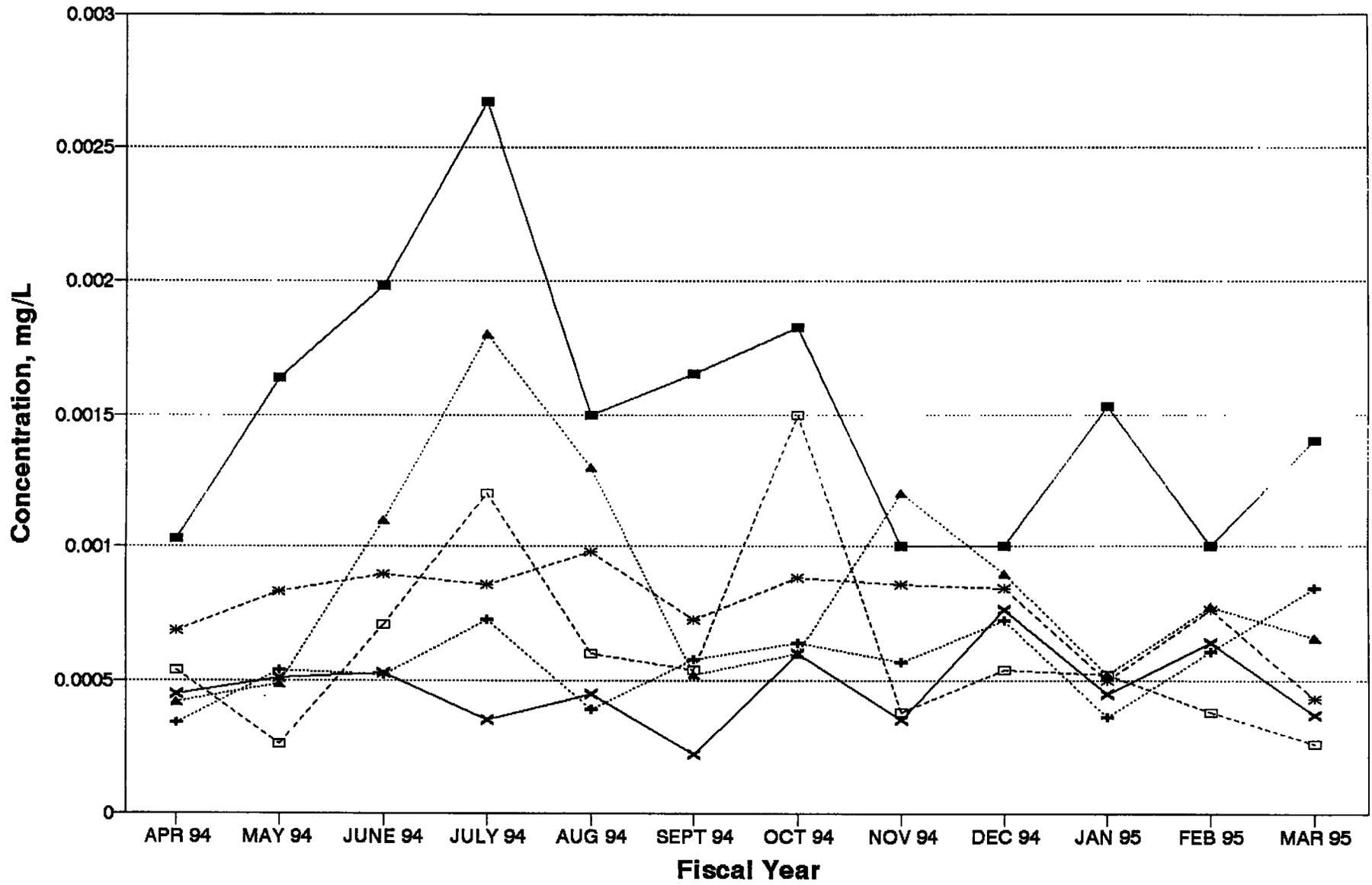
comparison of all plants



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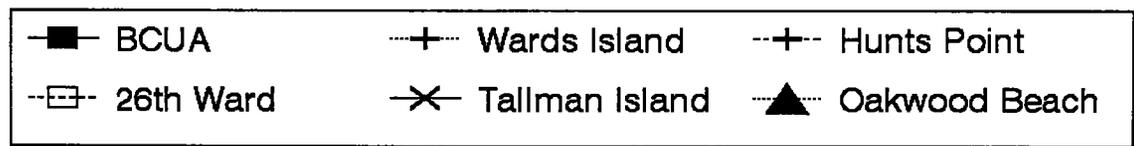
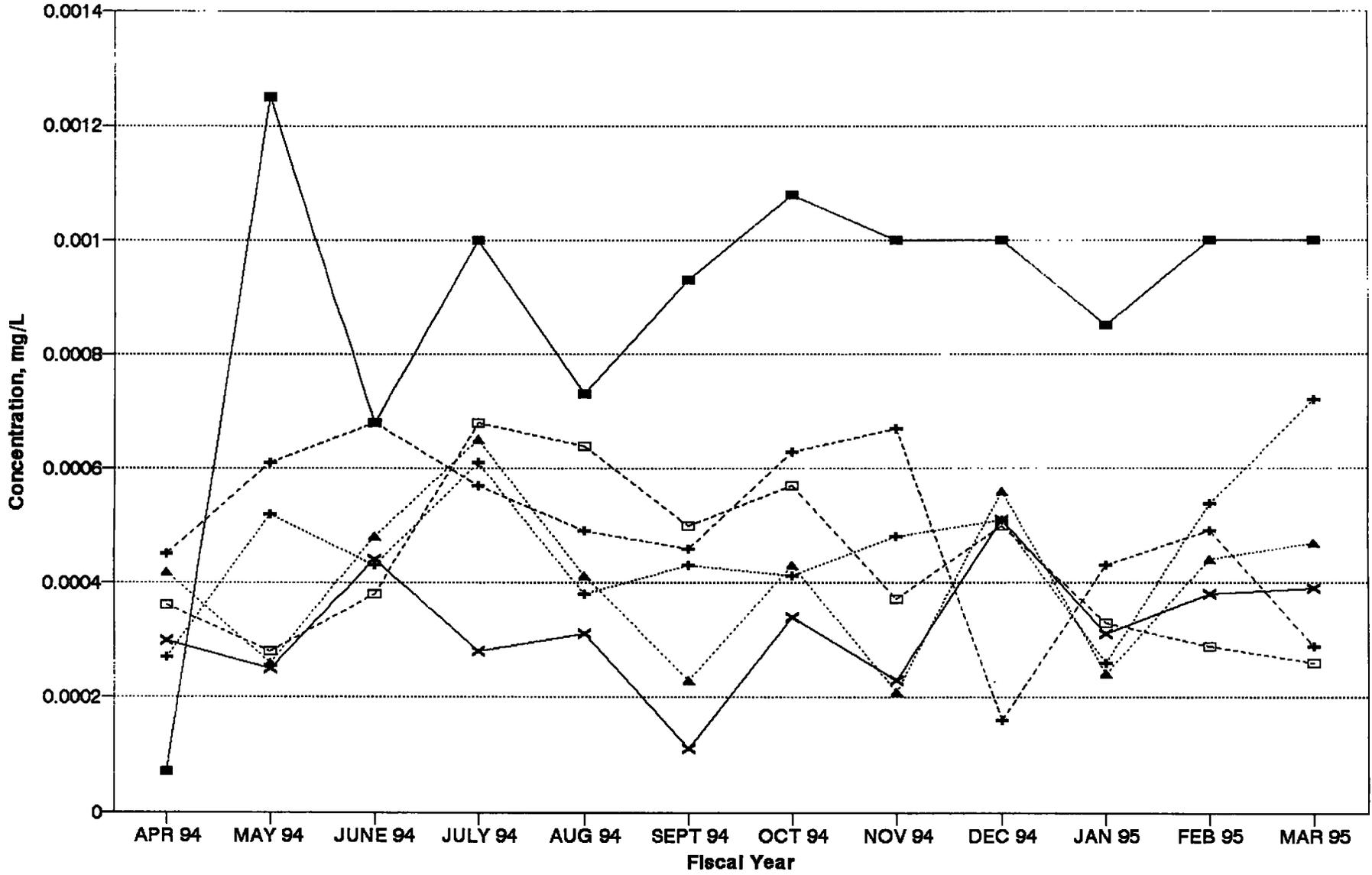
ARSENIC INFLUENT CONCENTRATION

comparison of all plants



ARSENIC EFFLUENT CONCENTRATION

comparison of all plants



CADMIUM INFLUENT CONCENTRATION

comparison of all plants

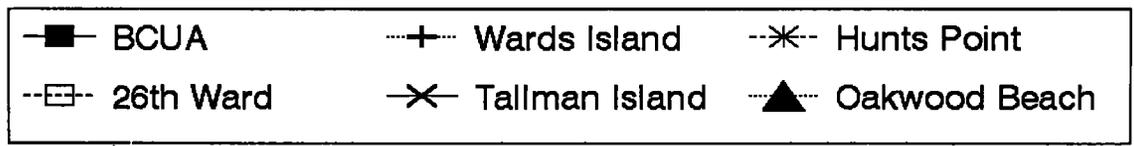
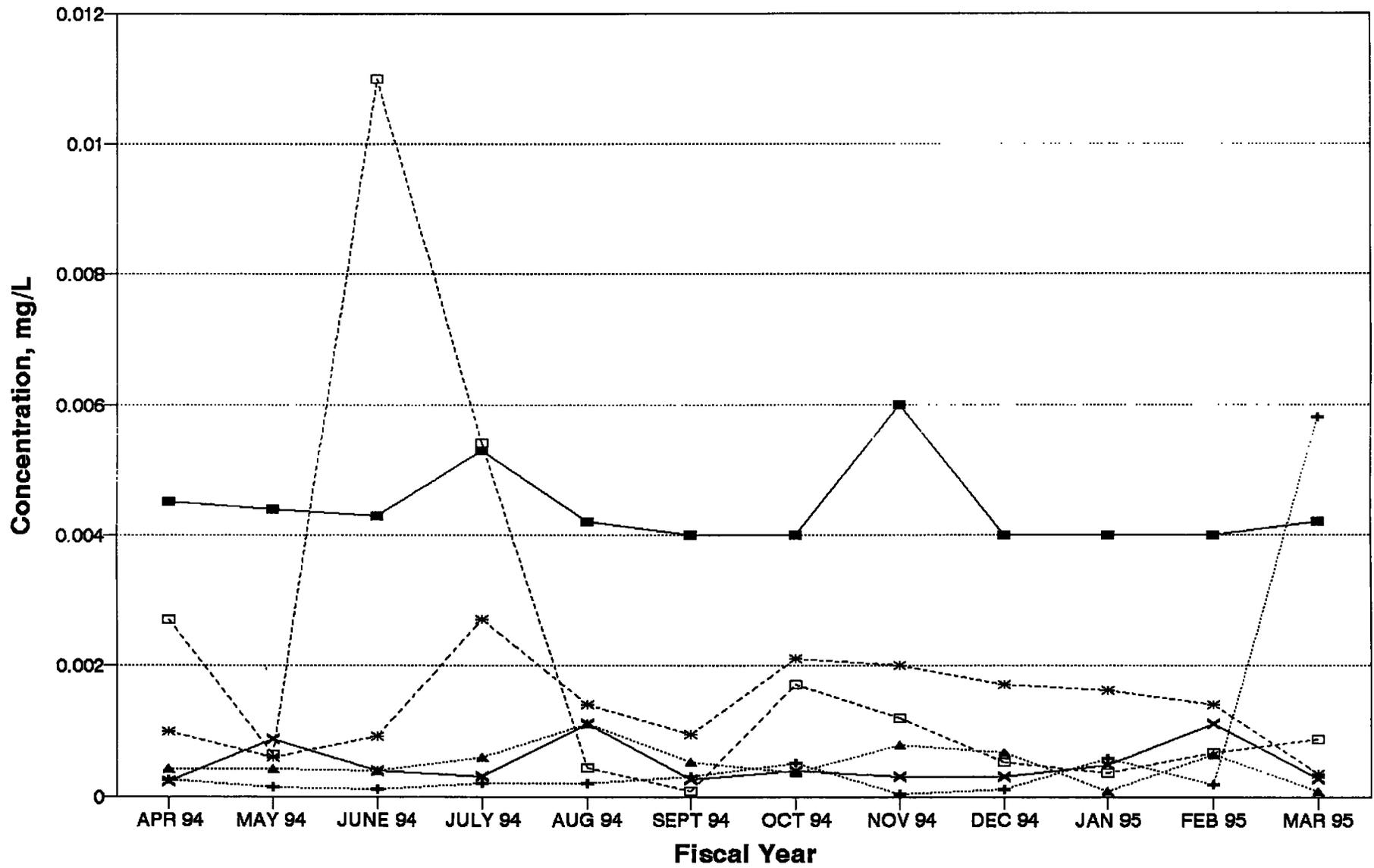
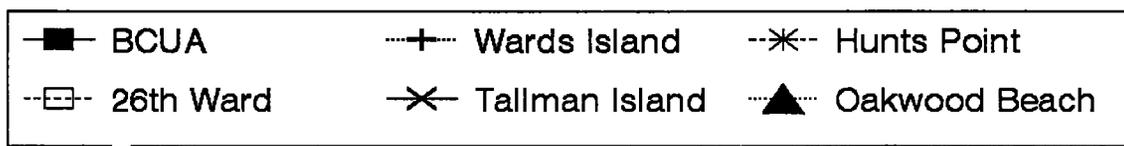
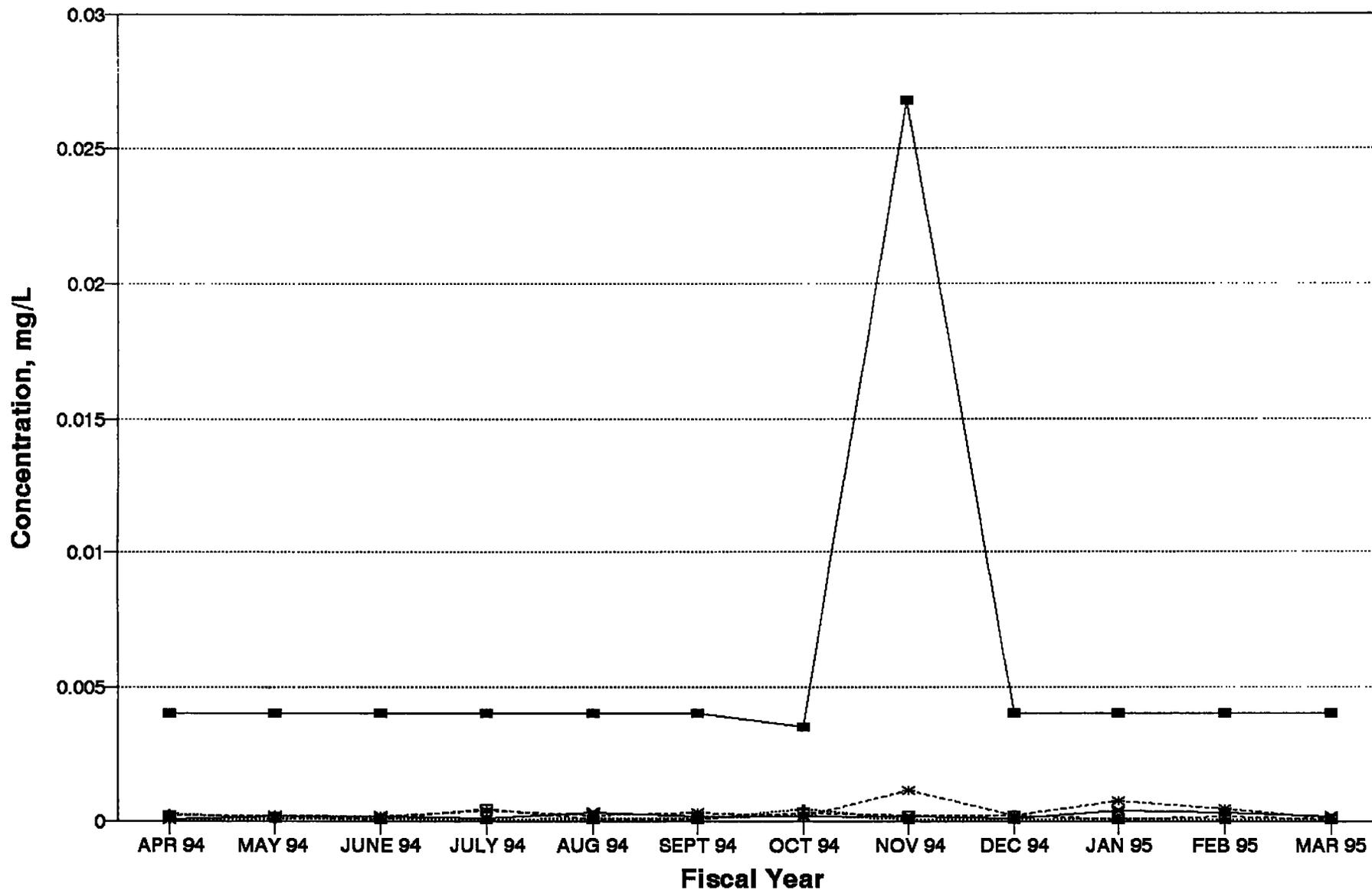


Figure 1

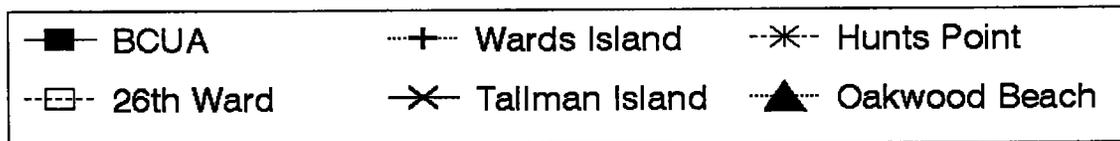
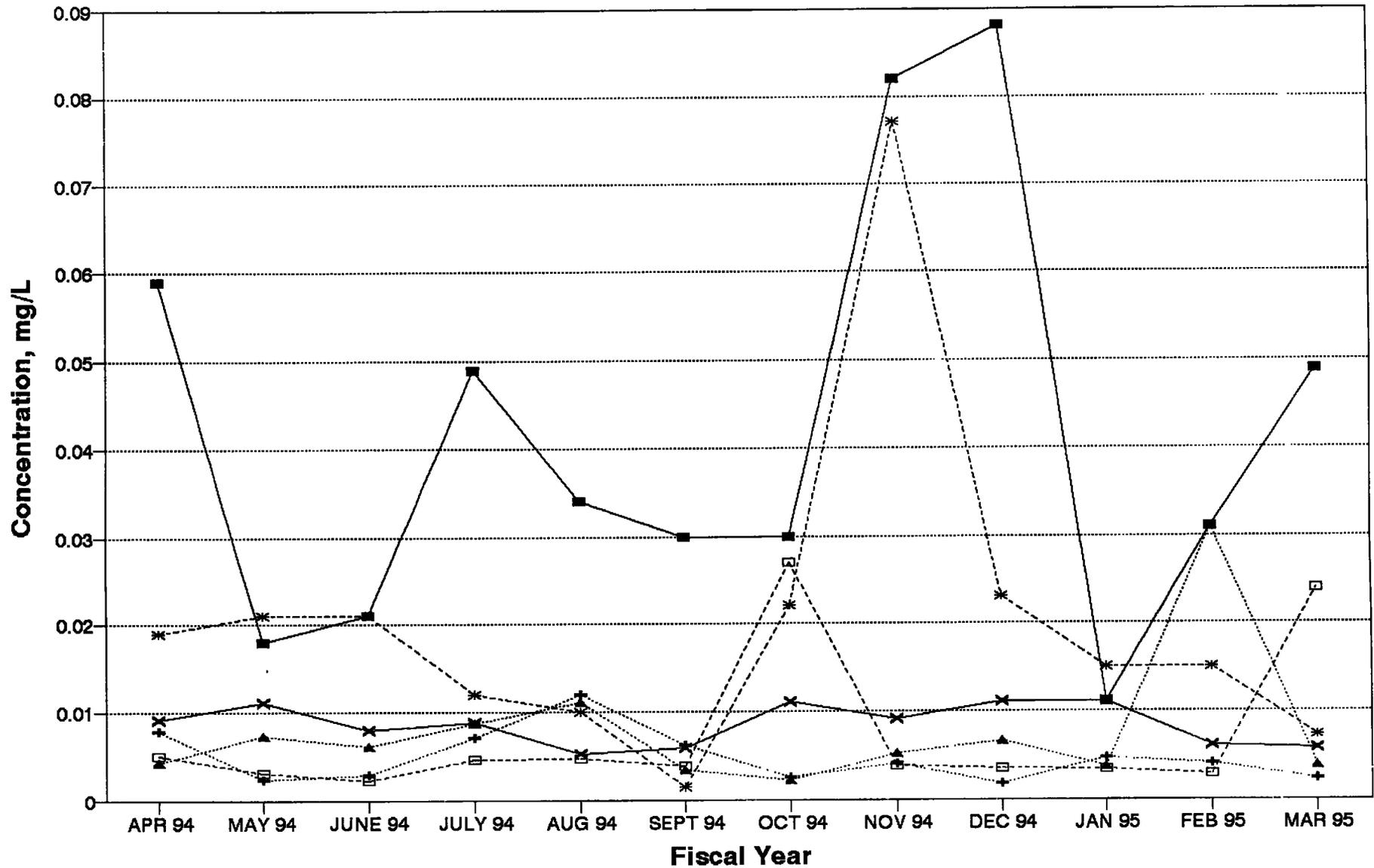
CADMIUM EFFLUENT CONCENTRATION

comparison of all plants



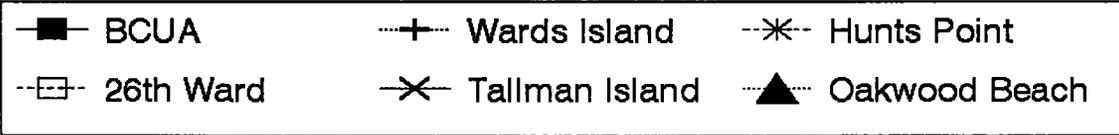
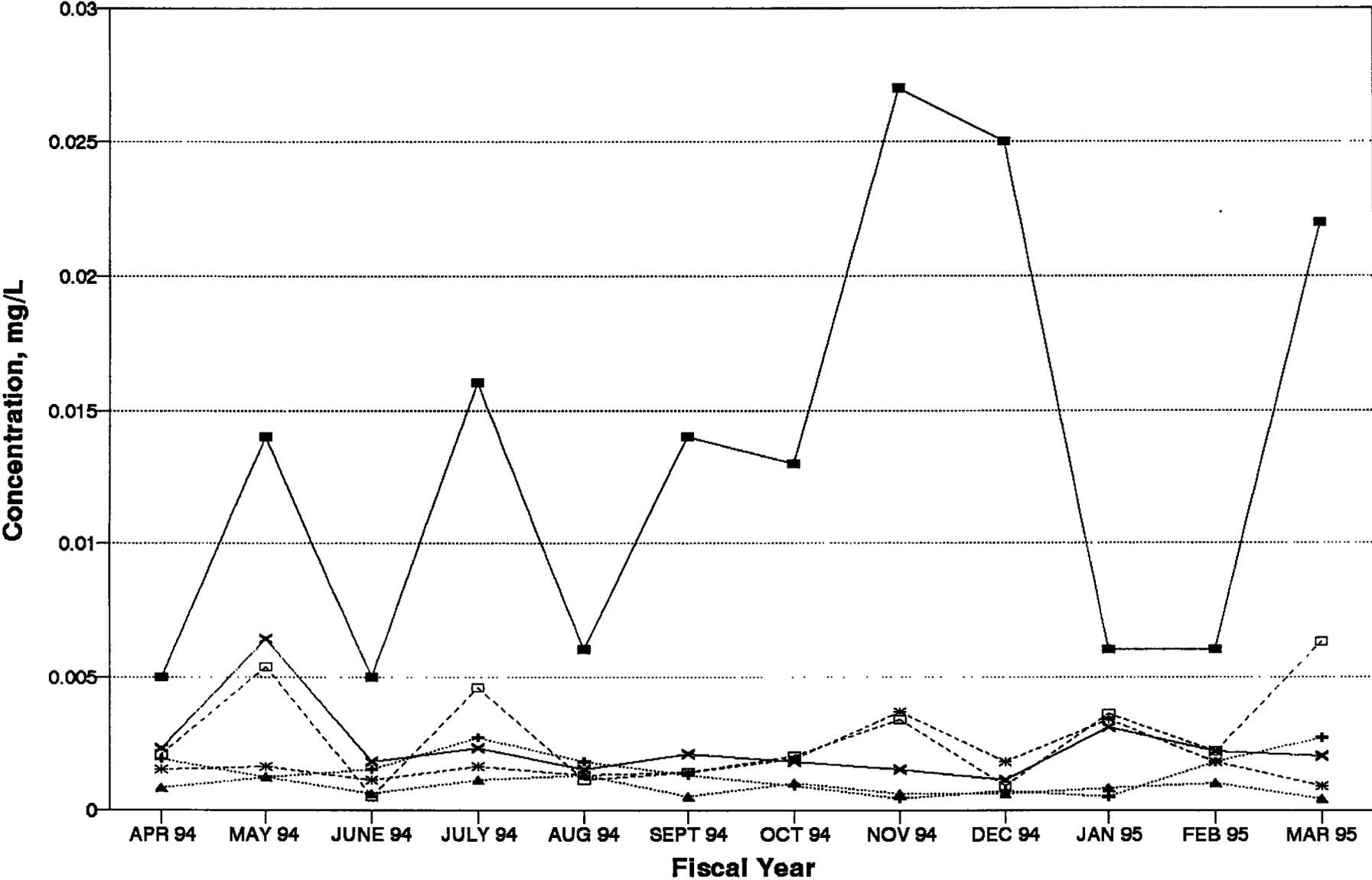
CHROMIUM INFLUENT CONCENTRATION

comparison of all plants



CHROMIUM EFFLUENT CONCENTRATION

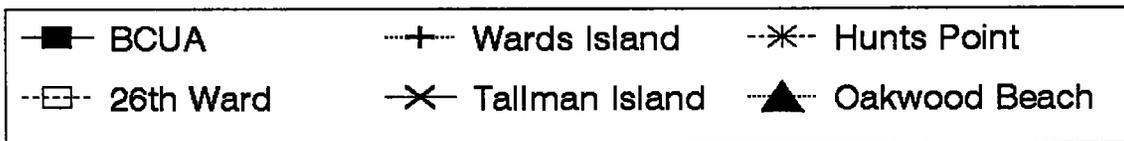
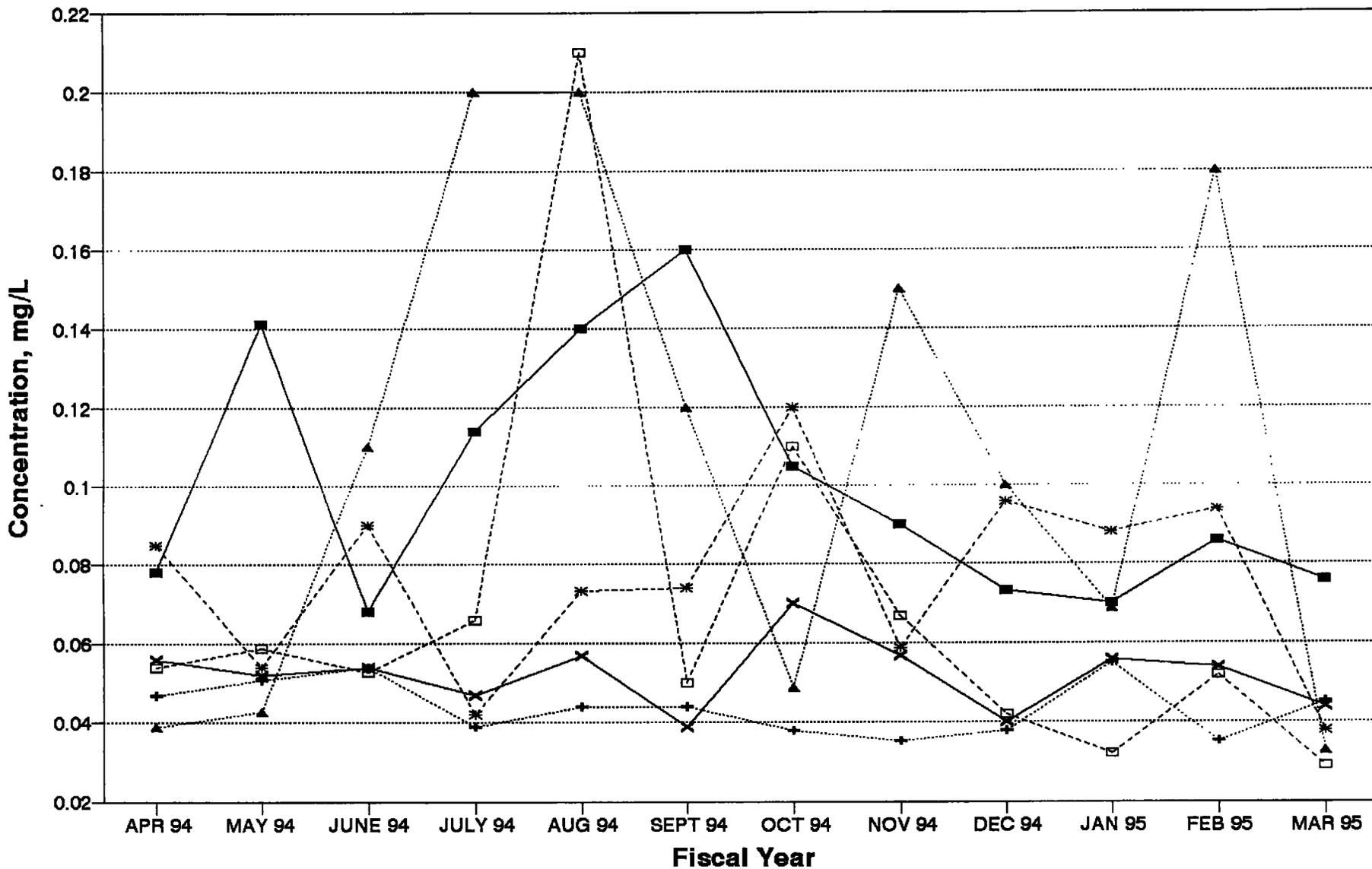
comparison of all plants



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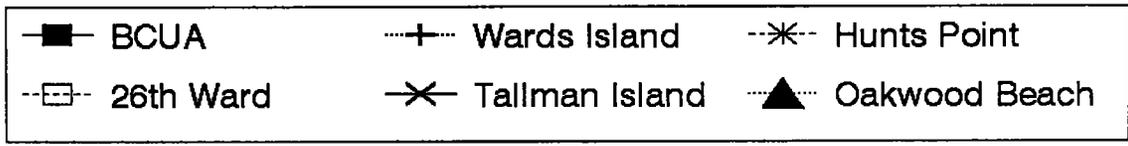
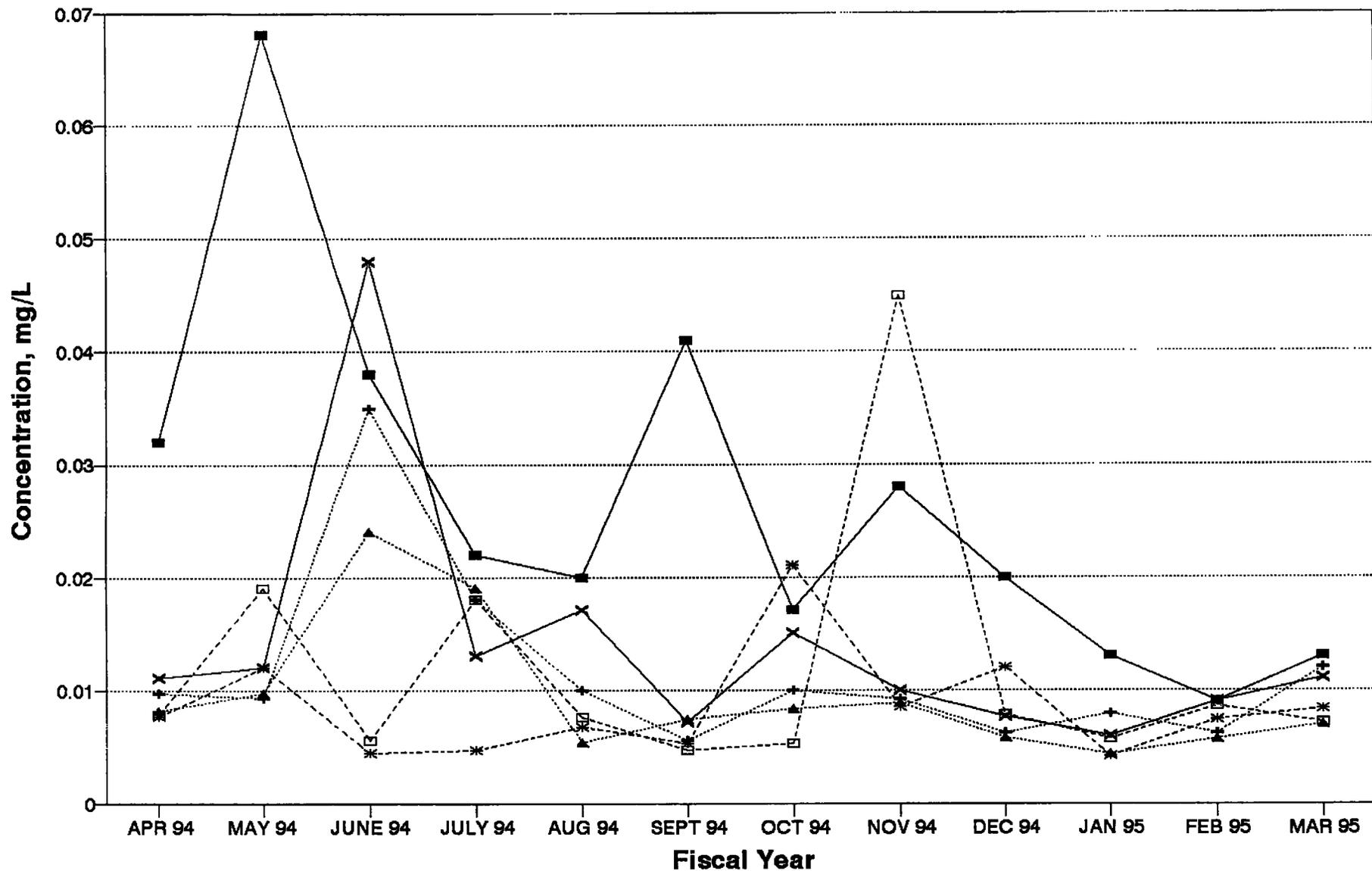
COPPER INFLUENT CONCENTRATION

comparison of all plants



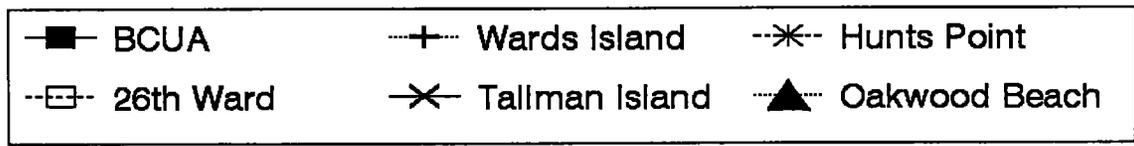
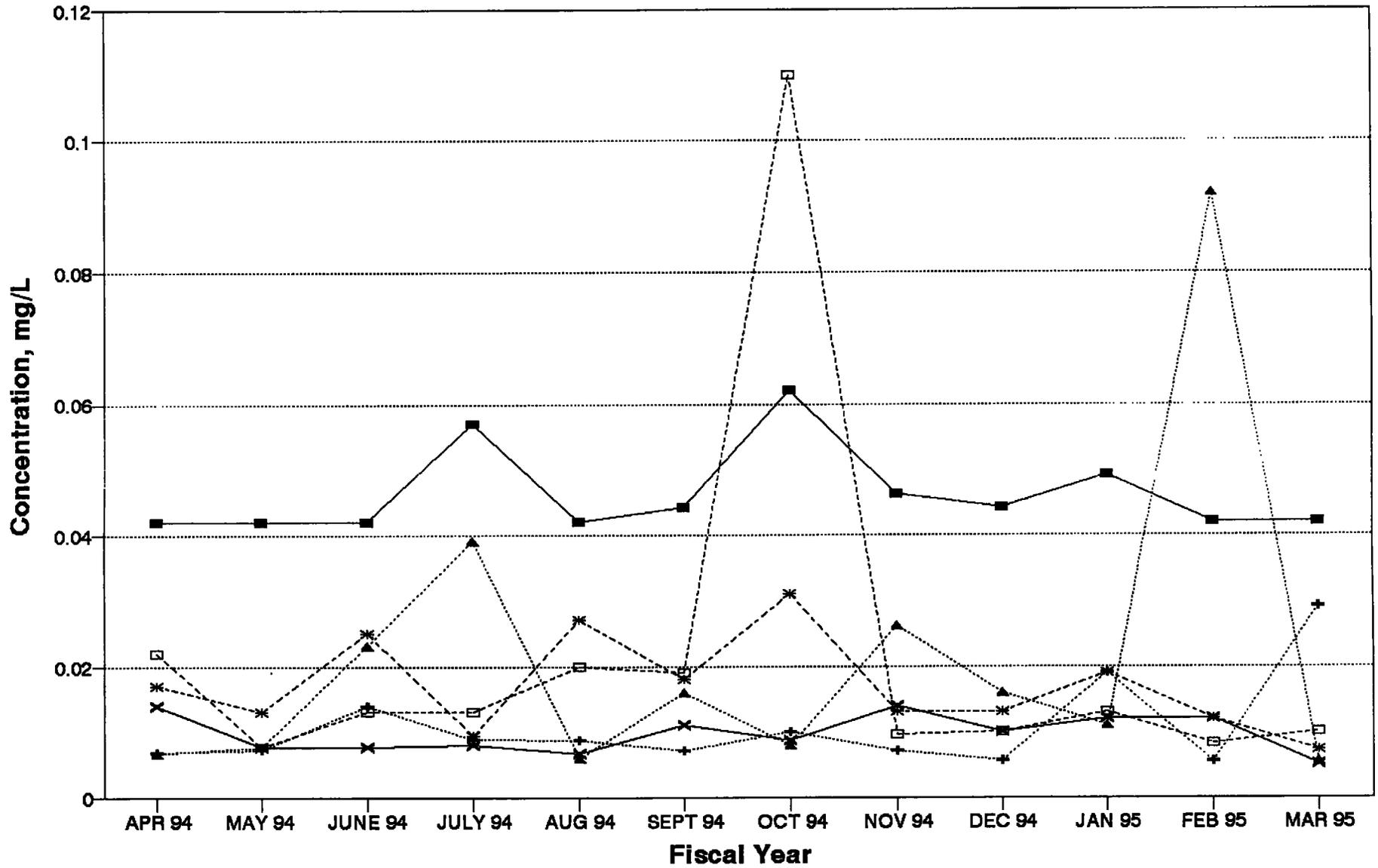
COPPER EFFLUENT CONCENTRATION

comparison of all plants



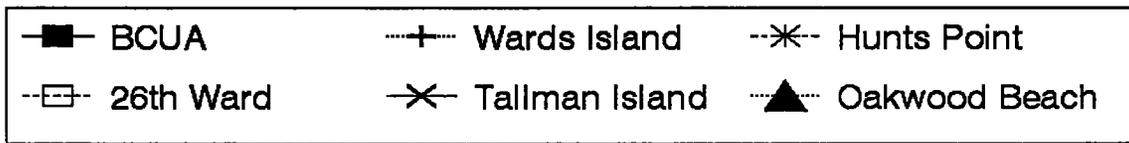
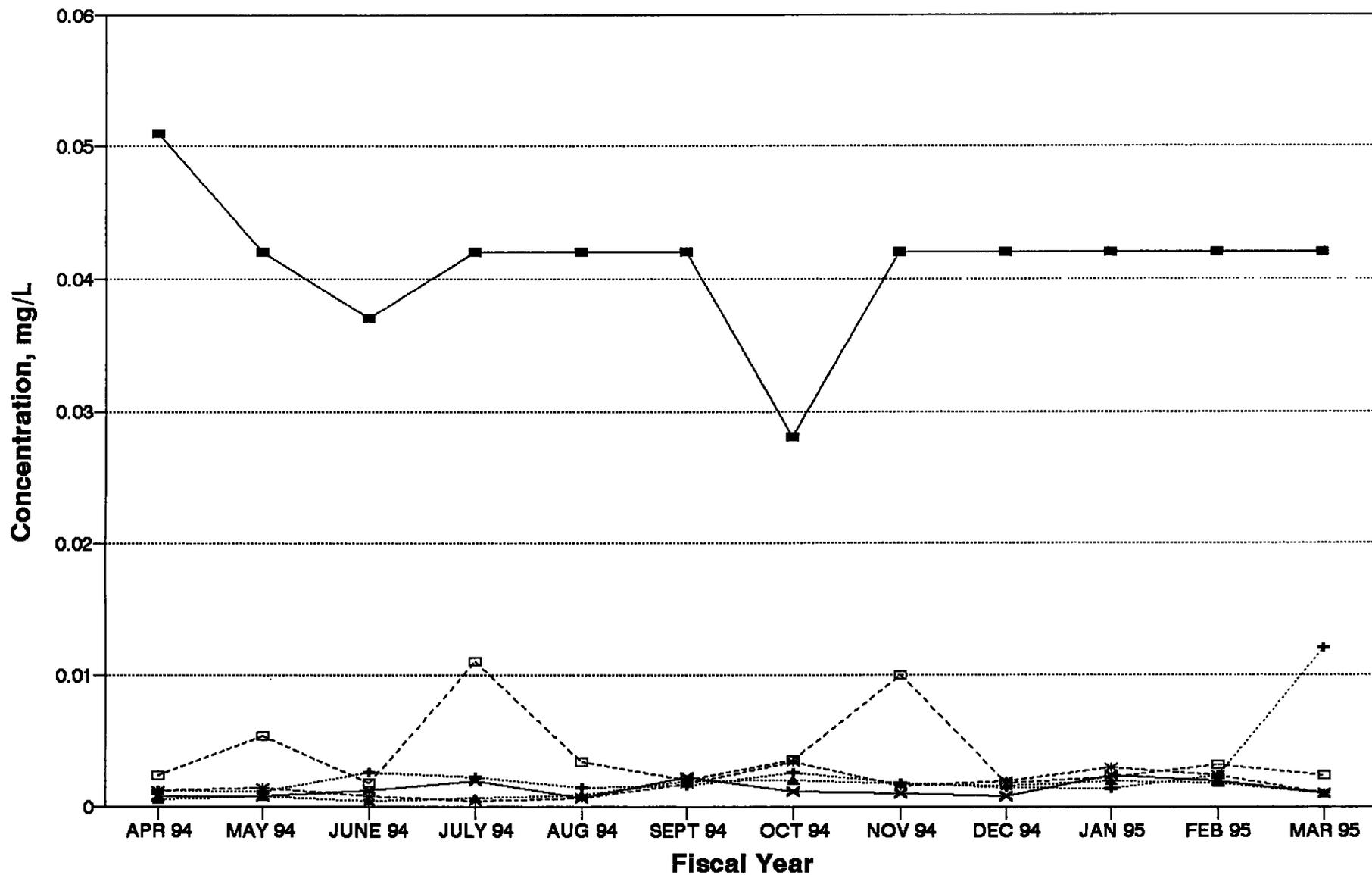
LEAD INFLUENT CONCENTRATION

comparison of all plants



LEAD EFFLUENT CONCENTRATION

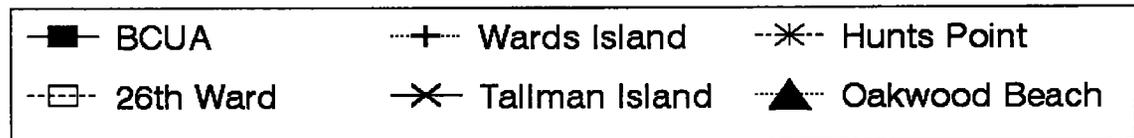
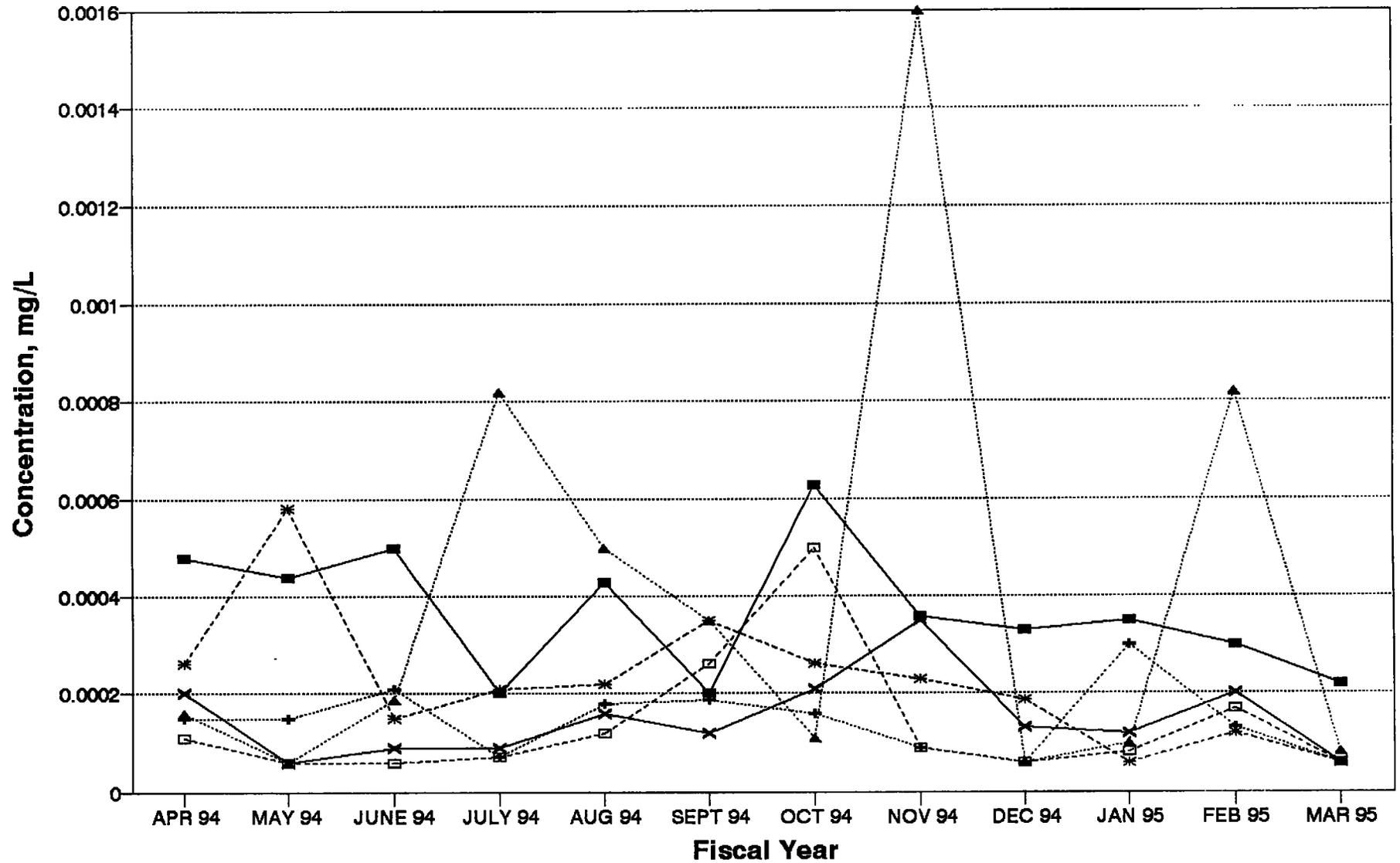
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7.2.1

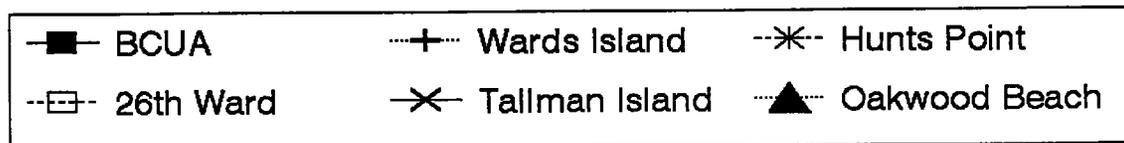
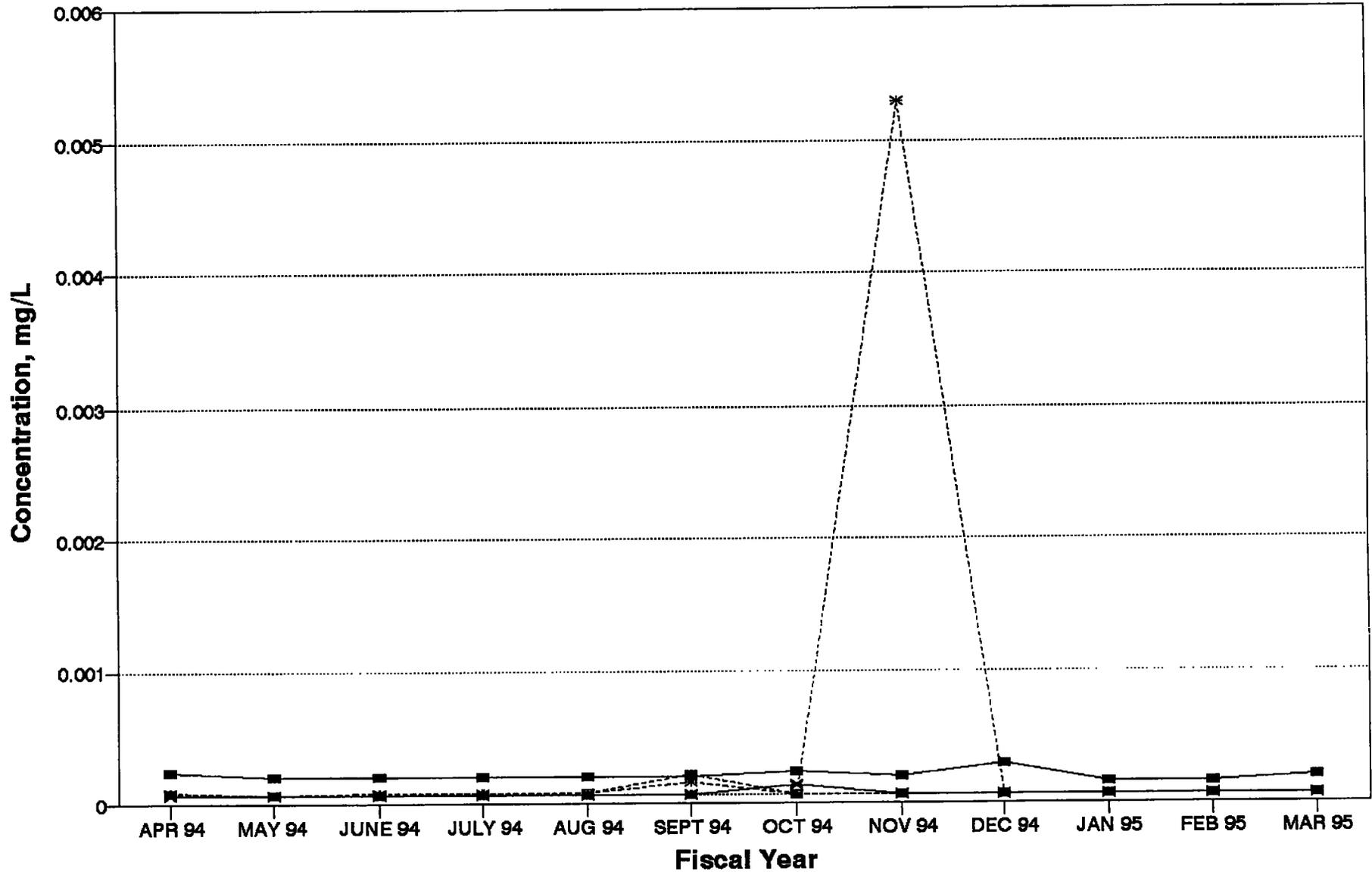
MERCURY INFLUENT CONCENTRATION

comparison of all plants



MERCURY EFFLUENT CONCENTRATION

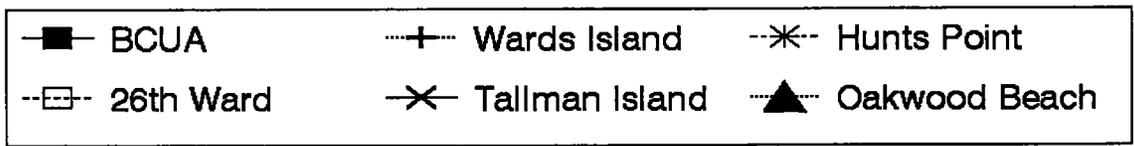
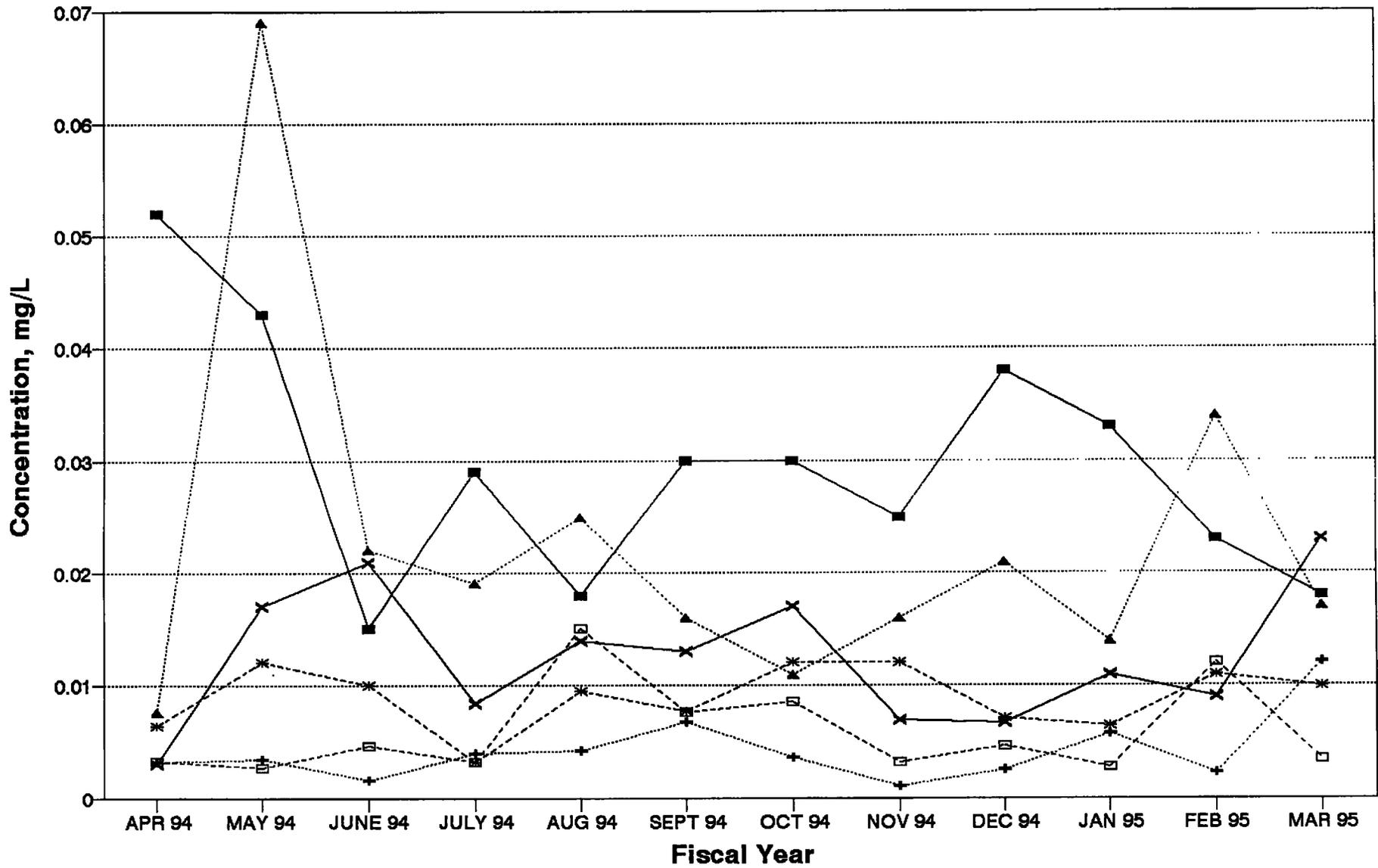
comparison of all plants



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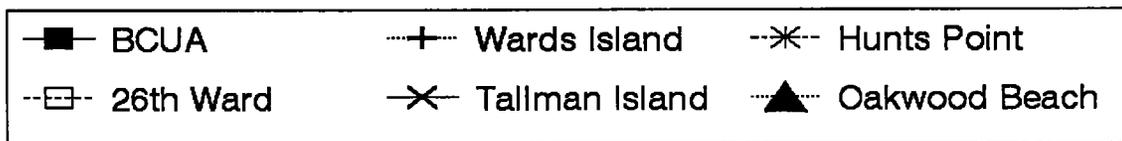
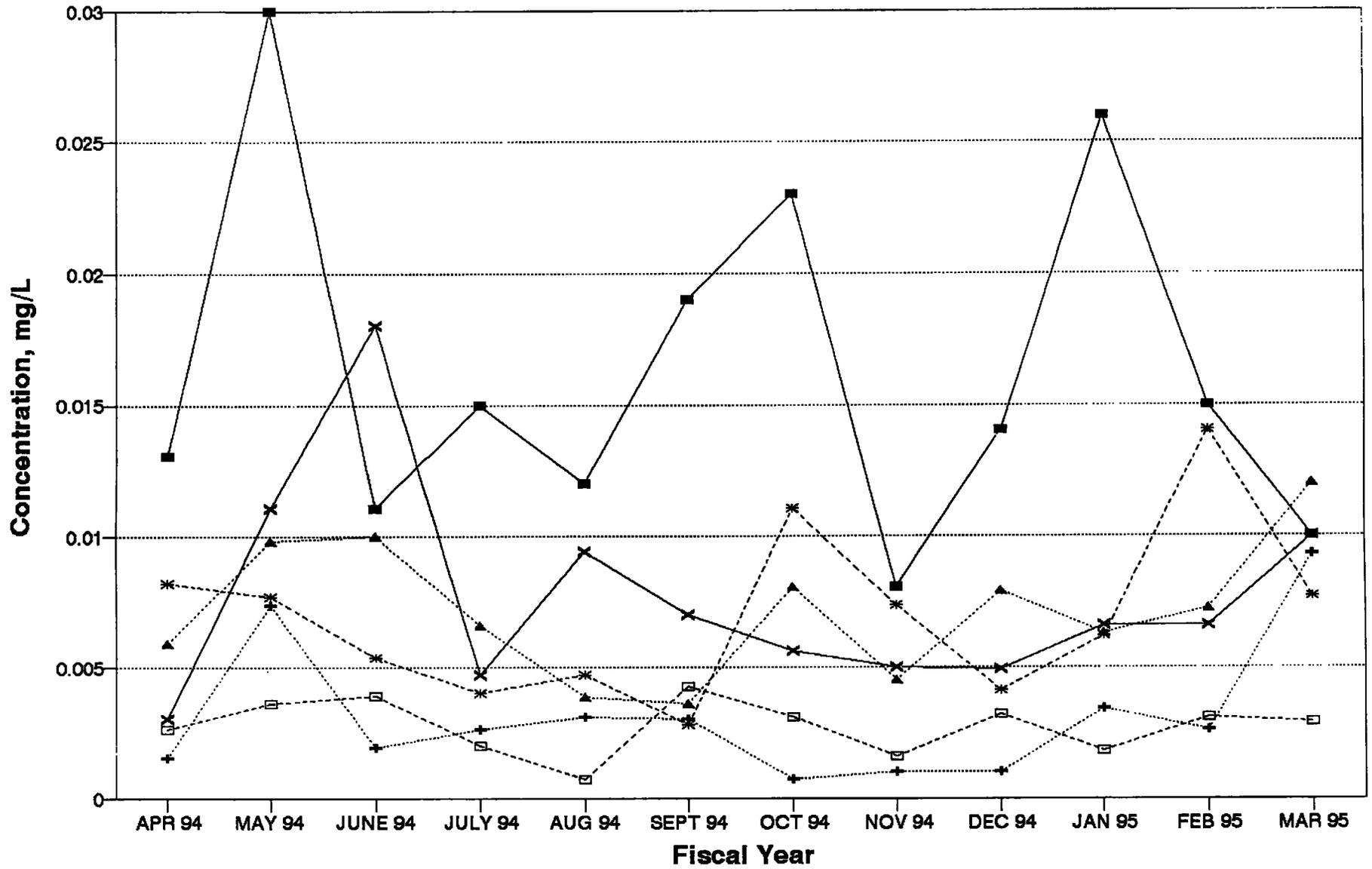
NICKEL INFLUENT CONCENTRATION

comparison of all plants



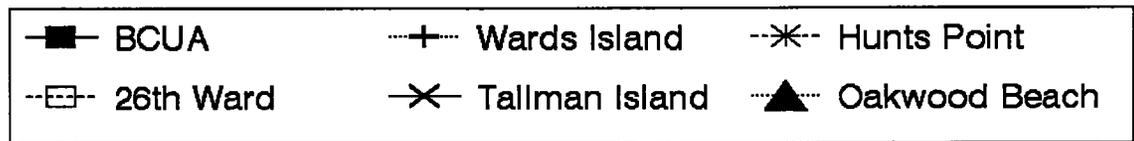
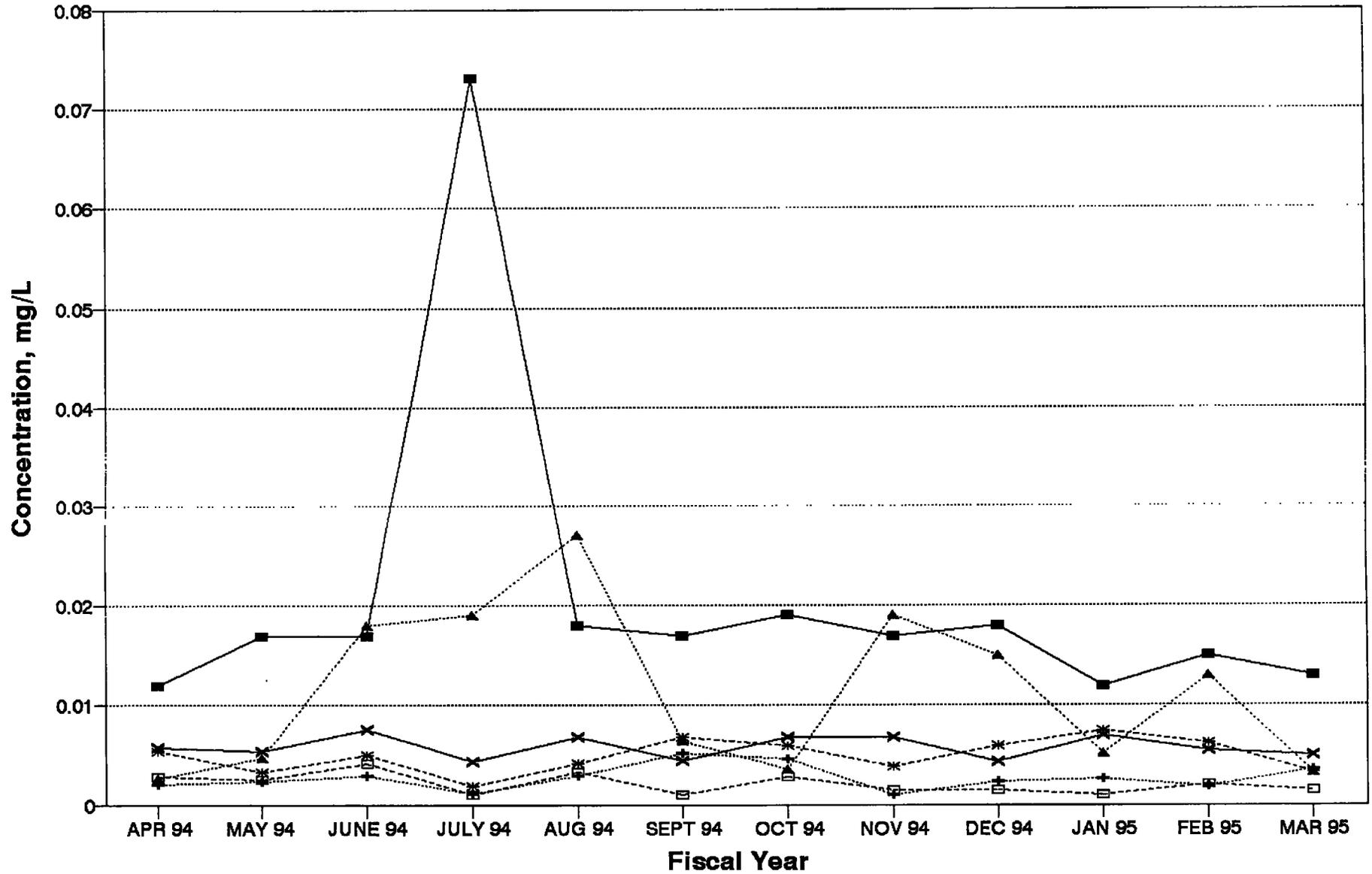
NICKEL EFFLUENT CONCENTRATION

comparison of all plants



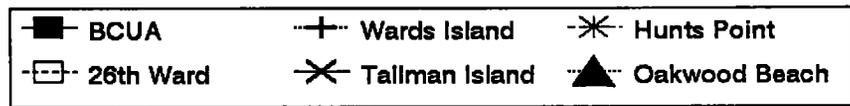
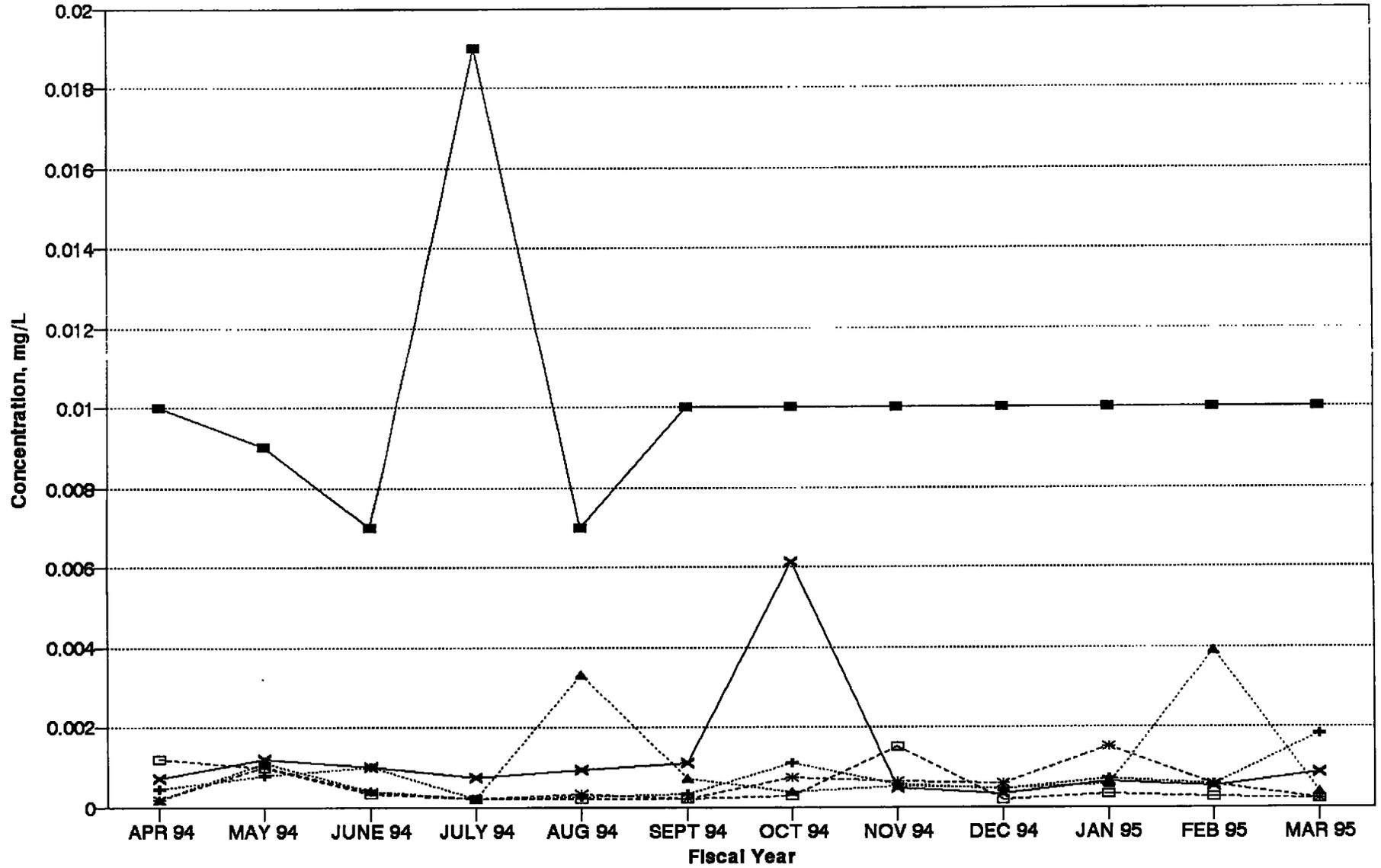
SILVER INFLUENT CONCENTRATION

comparison of all plants



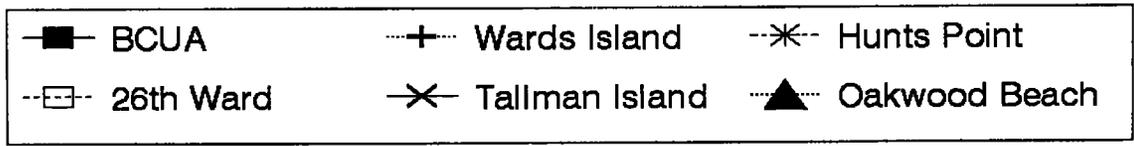
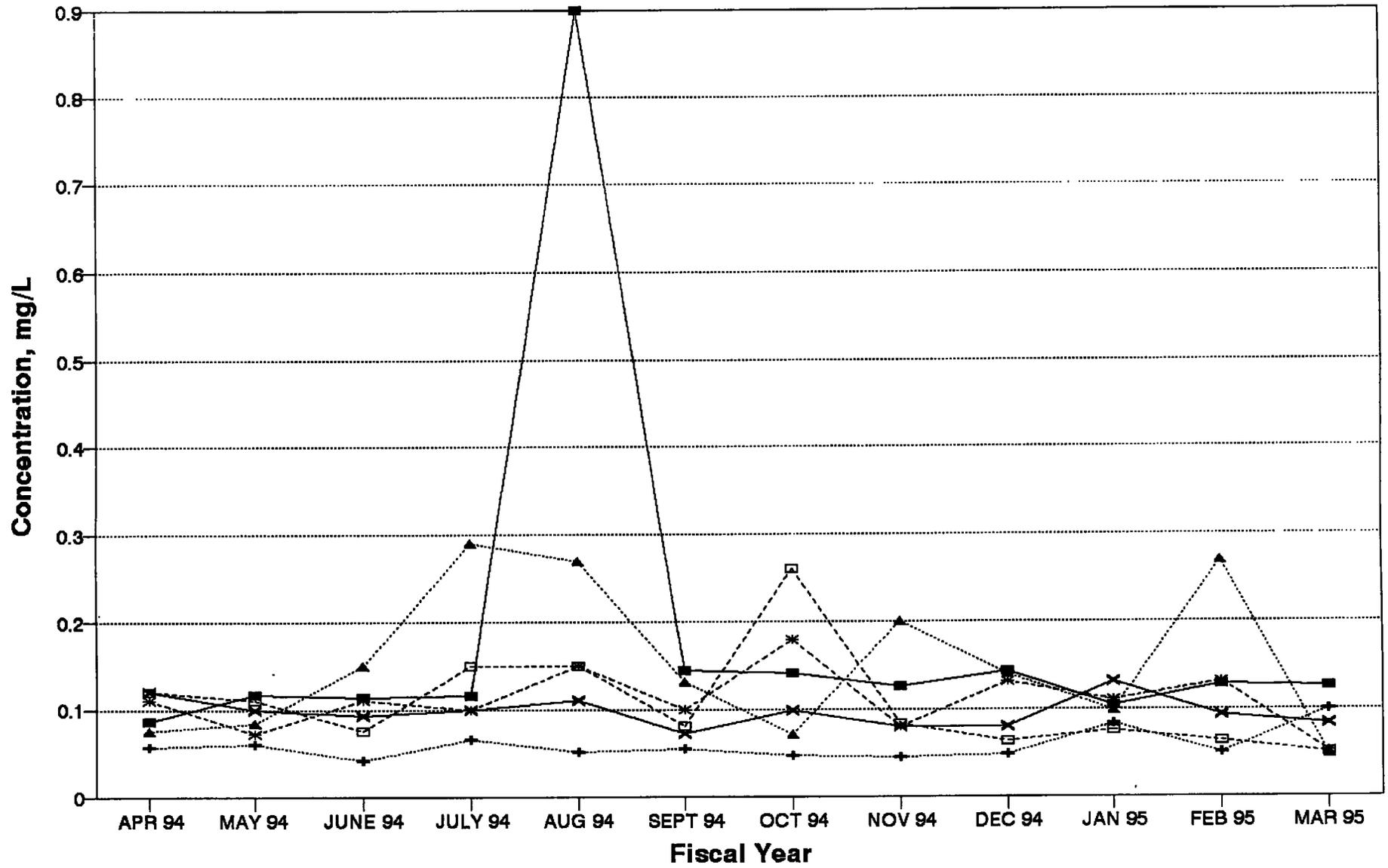
SILVER EFFLUENT CONCENTRATION

comparison of all plants



ZINC INFLUENT CONCENTRATION

comparison of all plants



ZINC EFFLUENT CONCENTRATION

comparison of all plants

